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Received August 20, 2025 WV DEP/Div of Air Quality

9627 Tuscarora Pike Martinsburg, WV 25403

125 Granville Square, Suite 400 Morgantown, WV 26501

501 Avery Street Parkersburg, WV 26101

Southpointe Town Center 1800 Main Street, Suite 200 Canonsburg, PA 15317

480 West Jubal Early Drive, Suite 130 Winchester, VA 22601

August 20, 2025

E-MAIL

bowlesrice.com

Edward S. Andrews West Virginia Department of Environmental Protection Division of Air Quality 601 57th Street, SE Charleston, West Virginia 25304 edward.s.andrews@wv.gov

> Re: Clean Seas West Virginia Inc.

Application for NSR Permit And

Title V Permit Revision

Dear Mr. Andrews:

Attached for filing on behalf of Clean Seas West Virginia Inc., please find the Application for NSR Permit and Title V Permit Revision.

If you have any questions regarding this filing, please contact me.

Very truly yours,

Marc Mignault

MM:tlp Attachments

Samantha N. Blair (via e-mail) cc:

# **Division of Air Quality Permit Application Submittal**

PI	lease find attached a permit application for : Clean-	Seas West Virginia Inc, Belle
	[Con	mpany Name; Facility Location]
•	DAQ Facility ID (for existing facilities only):	
٠	Current 45CSR13 and 45CSR30 (Title V) permits	
	associated with this process (for existing facilitie	s only):
n n	Type of NSR Application (check all that apply):  Construction  Modification  Class I Administrative Update  Class II Administrative Update  Relocation  Temporary  Permit Determination	<ul> <li>Type of 45CSR30 (TITLE V) Revision (if any)**:</li></ul>
•	Payment Type:  ☐ Credit Card (Instructions to pay by credit car ☐ Check (Make checks payable to: WVDEP – Di Mail checks to:  WVDEP – DAQ – Permitting  Attn: NSR Permitting Secretary  601 57 <sup>th</sup> Street, SE  Charleston, WV 25304	emails you the Facility ID Number and Permit Application Number. Please add these identifiers to your check or cover letter
•	If the permit writer has any questions, please con Responsible Official/Authorized Representat  • Name: Dan Bates	ntact (all that apply): ive
	Email: dan@clean-seas.com	
	• Phone Number: 310-387-7636	9
	✓ Company Contact	
	Name: John Yonce	
	Email: john.yonce@clean-seas.com	
	• Phone Number: 617-922-0076	
	☑ Consultant	
	Name: Roger Hanshaw	
	Email: rhanshaw@bowlesrice.com	
	<ul> <li>Phone Number: 304-347-1100</li> </ul>	

☐ CLASS I ADMINISTRATIVE UPDATE

☐ CLASS II ADMINISTRATIVE UPDATE

#### WEST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION**

#### **DIVISION OF AIR QUALITY**

601 57th Street, SE Charleston, WV 25304 (304) 926-0475

www.dep.wv.gov/daq

#### APPLICATION FOR NSR PERMIT **AND** TITLE V PERMIT REVISION

(OPTIONAL) PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNOWN): PLEASE CHECK TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY): **☐** CONSTRUCTION ☐ MODIFICATION ☐ RELOCATION ☐ ADMINISTRATIVE AMENDMENT **☐ MINOR MODIFICATION** ☐ SIGNIFICANT MODIFICATION ☐ TEMPORARY IF ANY BOX ABOVE IS CHECKED. INCLUDE TITLE V REVISION ☐ AFTER-THE-FACT INFORMATION AS ATTACHMENT S TO THIS APPLICATION

FOR TITLE V FACILITIES ONLY: Please refer to "Title V (Appendix A, "Title V Permit Revision Flowchart") and					
Sec	tion I. General				
Name of applicant (as registered with the WV Secreta Clean-Seas West Virginia Inc.	ry of State's Office):	2. Federal Employer ID No. <i>(FEIN):</i> 92-3247592			
3. Name of facility (if different from above):		4. The applicant is the:  ☐ OWNER ☐ OPERATOR ☒ BOTH			
5A. Applicant's mailing address: 2700 E Dupont Ave, Ste 3B Belle WV 25015	5B. Facility's prese 2700 E Dupont Ave S Belle WV 25015		ddress:		
<ul> <li>6. West Virginia Business Registration. Is the applicant</li> <li>If YES, provide a copy of the Certificate of Incorpor change amendments or other Business Registration</li> <li>If NO, provide a copy of the Certificate of Authority/amendments or other Business Certificate as Attach</li> </ul>	ation/Organization/Limit Certificate as Attachmen /Authority of L.L.C./Regi	ted Partners t A.	hip (one page) includ		
7. If applicant is a subsidiary corporation, please provide	the name of parent corpo	ration: Clean-	Seas Inc.		
8. Does the applicant own, lease, have an option to buy of	or otherwise have control	of the <i>propos</i>	ed site? 🛚 YES	□NO	
- If <b>YES</b> , please explain: 20 year lease, commen	ncing March 1 2025				
If <b>NO</b> , you are not eligible for a permit for this source					
<ol> <li>Type of plant or facility (stationary source) to be consadministratively updated or temporarily permitted crusher, etc.): Plastics Pyrolysis Plant</li> </ol>			10. North American Classification S (NAICS) code	System	
Г			325199		
11A. DAQ Plant ID No. (for existing facilities only):  -	11B. List all current 45CS associated with this		CSR30 (Title V) permexisting facilities only		
All of the required forms and additional information can be	found under the Permitting	Section of DA	AQ's website, or reque	ested by phone.	

12A.		
- For Modifications, Administrative Updates or Tel		please provide directions to the
<ul> <li>present location of the facility from the nearest state</li> <li>For Construction or Relocation permits, please p</li> </ul>		ite location from the nearest state
road. Include a MAP as Attachment B.	Torrac amount to the proposed from a	no reculer from the fredrest state
From US Rte 60, turn SOUTH onto Warrior Way.		
Turn EAST on E Dupont Ave.		
In approx 400 feet, turn NORTH into existing parking lot	t at 2700 E Dupont Ave	
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:
2700 E Dupont Ave	Belle	Kanawha
12.E. UTM Northing (KM): 1822380.411	12F. UTM Easting (KM): 440427.769	12G. UTM Zone: 17n
13. Briefly describe the proposed change(s) at the facility A plastics conversion plant will be constructed at the site	=	aludaa a daliyany daak
preprocessing, pyrolysis of plastic, pyrolysis oil loading ir		
baghouse for recovery of airborne plastic and parking.  14A. Provide the date of anticipated installation or change	ne: Oct 1 2025	
<ul> <li>If this is an After-The-Fact permit application, provi</li> </ul>		14B. Date of anticipated Start-Up if a permit is granted:
change did happen: / /		Nov 1 2025
14C. Provide a <b>Schedule</b> of the planned <b>Installation</b> of/one application as <b>Attachment C</b> (if more than one unit	<del>-</del>	units proposed in this permit
15. Provide maximum projected <b>Operating Schedule</b> of Hours Per Day 24 Days Per Week 7	f activity/activities outlined in this applica Weeks Per Year 52	ation:
16. Is demolition or physical renovation at an existing fac	cility involved? XYES NO	
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will become	e subject due to proposed
changes (for applicability help see www.epa.gov/cepp	oo), submit your <b>Risk Management Pla</b>	n (RMP) to U. S. EPA Region III.
18. Regulatory Discussion. List all Federal and State a	air pollution control regulations that you l	pelieve are applicable to the
proposed process (if known). A list of possible applica	able requirements is also included in Atta	achment S of this application
(Title V Permit Revision Information). Discuss application	bility and proposed demonstration(s) of	compliance (if known). Provide this
information as <b>Attachment D.</b>		
Section II. Additional atta	achments and supporting de	ocuments.
19. Include a check payable to WVDEP - Division of Air	Quality with the appropriate application	fee (per 45CSR22 and
45CSR13).		
20. Include a <b>Table of Contents</b> as the first page of you		
21. Provide a <b>Plot Plan</b> , e.g. scaled map(s) and/or sketo source(s) is or is to be located as <b>Attachment E</b> (Re		rty on which the stationary
Indicate the location of the nearest occupied structure		
<ol> <li>Provide a Detailed Process Flow Diagram(s) show device as Attachment F.</li> </ol>	ving each proposed or modified emission	ns unit, emission point and control
23. Provide a <b>Process Description</b> as <b>Attachment G.</b>		
<ul> <li>Also describe and quantify to the extent possible a</li> </ul>		
All of the required forms and additional information can be	found under the Permitting Section of DA	Q's website, or requested by phone.

24.	Provide <b>Material Safety Data Sheets</b>	(MSDS) for all materials pro	cessed, used or produ	ced as Attachment H.						
– F	or chemical processes, provide a MSI	OS for each compound emitte	ed to the air.							
25.	Fill out the <b>Emission Units Table</b> and	d provide it as Attachment I.								
26.	Fill out the Emission Points Data Su	mmary Sheet (Table 1 and	Table 2) and provide it	as <b>Attachment J.</b>						
27.	Fill out the Fugitive Emissions Data	Summary Sheet and provide	e it as <b>Attachment K.</b>							
28.	Check all applicable Emissions Unit	Data Sheets listed below:								
В	ulk Liquid Transfer Operations	☐ Haul Road Emissions	☐ Quarry							
C	hemical Processes	☐ Hot Mix Asphalt Plant		ls Sizing, Handling and Storage						
□c	Concrete Batch Plant Incinerator Facilities									
	rey Iron and Steel Foundry	Indirect Heat Exchange	r Storage Tank	SS .						
G	eneral Emission Unit, specify: Plastics	s Pyrolysis units (2) and a Fla	are							
Fill c	ut and provide the Emissions Unit Da	ata Sheet(s) as Attachment	L.							
29.	Check all applicable Air Pollution Co	ntrol Device Sheets listed b	elow:							
□ A	bsorption Systems	☐ Baghouse		Flare						
□ A	dsorption Systems	Condenser								
□ A	fterburner	☐ Electrostatic Precip	oitator							
	ther Collectors, specify									
Fill c	ut and provide the Air Pollution Cont	trol Device Sheet(s) as Atta	chment M.							
	Provide all <b>Supporting Emissions Ca</b> ltems 28 through 31.	alculations as Attachment	N, or attach the calcula	tions directly to the forms listed in						
	Monitoring, Recordkeeping, Report testing plans in order to demonstrate of application. Provide this information a	compliance with the propose								
	Please be aware that all permits must measures. Additionally, the DAQ may are proposed by the applicant, DAQ w	not be able to accept all me	asures proposed by the	e applicant. If none of these plans						
32.	Public Notice. At the time that the a	pplication is submitted, place	a Class I Legal Adve	rtisement in a newspaper of general						
,	circulation in the area where the source	e is or will be located (See 4	5CSR§13-8.3 through	45CSR§13-8.5 and <i>Example Legal</i>						
	Advertisement for details). Please su	ubmit the Affidavit of Public	ation as Attachment l	P immediately upon receipt.						
33.	Business Confidentiality Claims. D	• •	onfidential information	(per 45CSR31)?						
	☐ YES	⊠ NO								
	If <b>YES</b> , identify each segment of inforr segment claimed confidential, includin <b>Notice – Claims of Confidentiality</b> "	g the criteria under 45CSR§	31-4.1, and in accordar	nce with the DAQ's "Precautionary						
	Sec	ction III. Certification	n of Information							
	Authority/Delegation of Authority. Check applicable Authority Form bel		e other than the respon	sible official signs the application.						
□ A	uthority of Corporation or Other Busin	ess Entity	☐ Authority of Partner	rship						
□ A	uthority of Governmental Agency		☐ Authority of Limited	l Partnership						
	nit completed and signed <b>Authority F</b>	orm as Attachment R.	_ , ,	·						
			no Pormittina Continu of	DAO's wobsite or requested by the						
All C	n die required forms and additional Info	imauon can be ioung unger ti	ie remitting section of	DAQ's website, or requested by phone.						

35A. Certification of Information. To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.
, and the second
Certification of Truth, Accuracy, and Completeness
I, the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.
Compliance Certification  Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.
SIGNATURE DATE: 08/08/25  (Please use blue ink)  Please use blue ink)
35B. Printed name of signee: Daniel Bates 35C. Title: CEO
35D. E-mail: Dan@clean-seas.com 36E. Phone: 310-387-7636 36F. FAX:
36A. Printed name of contact person (if different from above): Roger Hanshaw  36B. Title: Attorney
36C. E-mail: rhanshaw@bowlesrice.com 36D. Phone: 304-347-1100 36E. FAX: 304-343-2867
Attachment A: Business Certificate  Attachment B: Map(s)  Attachment C: Installation and Start Up Schedule  Attachment D: Regulatory Discussion  Attachment F: Plot Plan  Attachment F: Detailed Process Flow Diagram(s)  Attachment H: Material Safety Data Sheets (MSDS)  Attachment H: Material Safety Data Sheets (MSDS)  Attachment I: Emission Units Table  Attachment M: Air Pollution Control Device Sheet(s)  Attachment N: Supporting Emissions Calculations  Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans  Attachment P: Public Notice  Attachment P: Public Notice  Attachment R: Authority Forms  Attachment R: Authority Forms  Attachment S: Title V Permit Revision Information  Attachment S: Title V Permit Revision Information  Application Fee
FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:
<ul> <li>☐ Forward 1 copy of the application to the Title V Permitting Group and:</li> <li>☐ For Title V Administrative Amendments:</li> <li>☐ NSR permit writer should notify Title V permit writer of draft permit,</li> <li>☐ For Title V Minor Modifications:</li> <li>☐ Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,</li> <li>☐ NSR permit writer should notify Title V permit writer of draft permit.</li> <li>☐ For Title V Significant Modifications processed in parallel with NSR Permit revision:</li> <li>☐ NSR permit writer should notify a Title V permit writer of draft permit,</li> <li>☐ Public notice should reference both 45CSR13 and Title V permits,</li> <li>☐ EPA has 45 day review period of a draft permit.</li> </ul> All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

# WEST VIRGINIA STATE TAX DEPARTMENT BUSINESS REGISTRATION CERTIFICATE

ISSUED TO:
CLEAN-SEAS WEST VIRGINIA, INC.
600 QUARRIER ST
CHARLESTON, WV 25301-0000

BUSINESS REGISTRATION ACCOUNT NUMBER:

2444-1316

This certificate is issued on:

04/03/2023

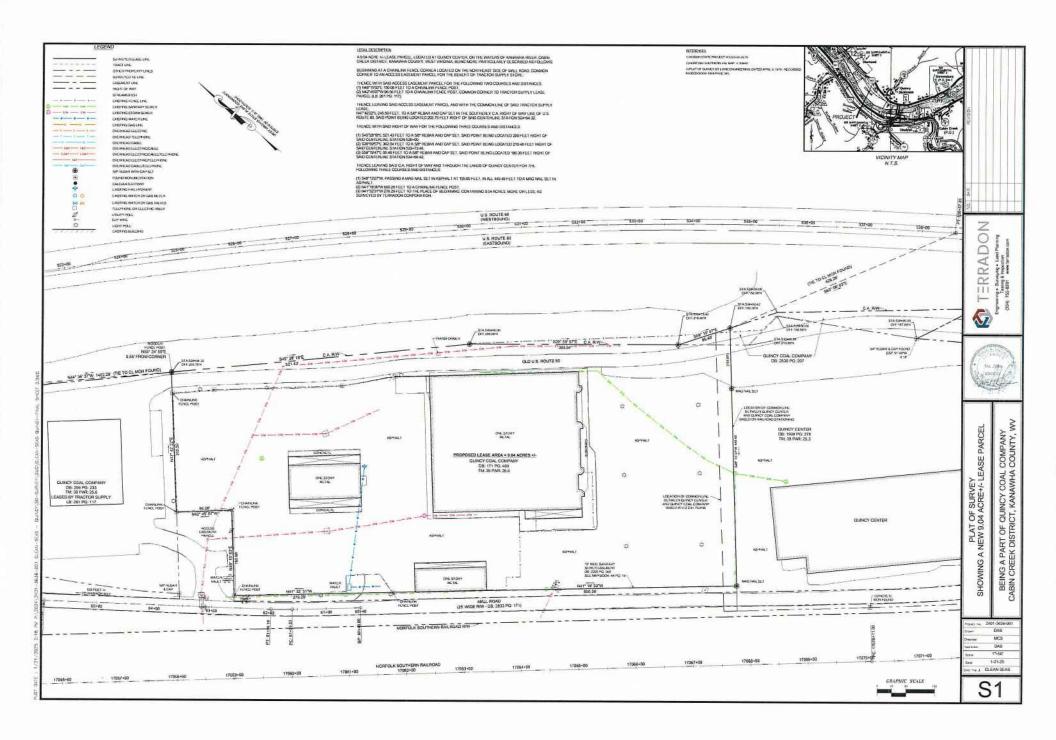
This certificate is issued by the West Virginia State Tax Commissioner in accordance with Chapter 11, Article 12, of the West Virginia Code.

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued. This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

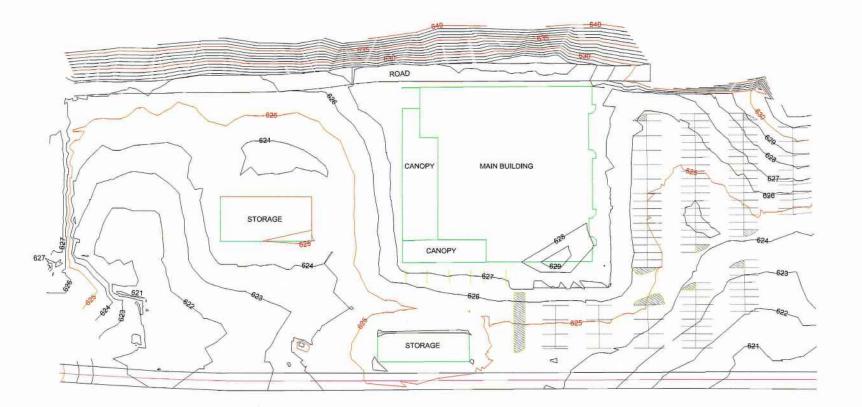
TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.







NEW RIVER ENGINEERS, INC. 702 SERVICES







PAGE 1 OF 1 JOB NO. : 363-01

## Clean Seas West Virginia

# Attachment C – Installation and Start-Up Schedule

The sources described in this application will be installed at the facility and start-up will occur as soon as possible. However, the schedule is entirely dependent on the availability of equipment from the manufacturers. It is anticipated that the entire facility may begin operating in 2025 or 2026, but this is subject to change.

#### Attachment "D" Clean Seas Facility Regulatory Discussion

The regulatory Discussion reviews the federal and West Virginia regulations potentially applicable to the proposed Clean Seas Facility in Kanawha County, West Virginia, owned and operated by Clean Seas West Virginia LLC.

- D.0 Federal Regulations
- D.01 Prevention of Signification
  - o D.01.01 Prevention of Significant Deterioration (40 CFR Part 51)
  - o D.01.02 Nonattainment New Source Review (40 CFR Part 51)
- D.02 New Source Performance Standards (40 CFR Part 60)
  - D.02.01 NSPS 40 CFR Part 60 Subpart CCCC and DDDD Standards of Performance and Emission Guidelines and Compliance for Commercial and Industrial Solid Waste Incineration Units
- D.03 National Emission Standards for Hazardous Air Pollutants (40 CFR 63)
- D.04 Chemical Accident Prevention (40 CFR 68)
- D.05 State Operating Permit Program (40 CFR 70)
- D.06 Mandatory Greenhouse Gas Reporting (40 CFR 98)
- D.07 Maximum Achievable Control Technology (MACT) applicability
- D.08 Risk Management Plan
- D.09 Stack height
- D1.0 West Virginia State Regulations
  - D1.01 45CSR10 To Prevent and Control Air Pollution from Emission of Sulfur Oxides <a href="https://dep.wv.gov">https://dep.wv.gov</a>
  - o D1.02 45CSR13 Permits for Construction
- D2.0 Insignificant Activities.

#### **D.0 Federal Regulations**

The Code of Federal Regulations (CFR) are regulations adopted by the US EPA and published in the Federal Register pursuant to the authority of the grant by Congress in the Clean Air Act. The CFR addresses multiple aspects, including but not limited to, permitting requirements, performance standards, testing methods, and monitoring requirements. The (CFR's) may be viewed online.

#### **D.01 Prevention of Significant Deterioration Determination**

The Prevention of Significant Deterioration (PSD) permitting program is a Clean Air Act permitting program for new and modified major stationary sources of air pollution.

Implementation of the federal PSD regulations is delegated to the state of West Virginia by U.S. EPA and these regulations are contained at 40 CFR Part 52.21. Therefore, BAPC implements the federal PSD regulations directly. These regulations specify federally required permitting procedures for each "major stationary source." The PSD regulations define a "stationary source" as "any buildings, structure, facility or installation which emits or may emit any air pollutant subject to regulation under the Act." A building structure facility or installation" is defined as "all of the pollutant-emitting activities which belong to the same industrial grouping, are located on one or more contiguous or adjacent properties, and are under the control of the same person (or persons under common control) except the activities of ant vessel. Pollutant-emitting activities shall be considered as part of the same industrial grouping if they belong to the same 'Major Group' (i.e., which have the same first two-digit code) as described in the Standard Industrial Classification Manual, 1972, as amended by the 1977 Supplement."

"Major" is defined as the potential to emit of a stationary source, which equal or exceeds a specified threshold (in tons per year) or any air pollutants regulated under the Clean Air Act (40 CFR 52.21(b)(1)). The first threshold is for a stationary source that emits or has the potential to emit 100 tons per year or more of any regulated NSR pollutants and is defined as one of 28 specific categories of sources (see 40 CFR 52.21(b)(1)(i)(a)). The other applicability threshold is for any other stationary source that emits or has the potential to emit 250 tons per year of any regulated NSR pollutant (see 40 CFR 52.21(b)(1)(i)9b)). The Clean-Seas facility is not a major source as defined by PSD.

#### D.01.01 Prevention of Significant Deterioration (40 CFR 51)

Prevention of Significant Deterioration (PSD) applies to all criteria pollutants in an area that has been designated as attainment, such as the city of Belle, WV. The PSD program is set forth in 40 CFR 51 and is part of the federal New Source Review (NSR) permitting program for pollutants in an attainment area. Potential emissions of each PSD pollutant are below the program threshold; therefore, federal PSD review does not apply.

#### D.01.02 Nonattainment New Source Review (40 CFR Part 51)

Nonattainment New Source Review (NNSR) applies to major stationary sources located in nonattainment areas. The proposed plant will be located in Kanawha County, which is currently in attainment for all pollutants. Therefore, NNSR does not apply.

#### D.02 New Source Performance Standards (40 CFR Part 60)

Section 111 of the Clean Air Act, Standards of performance for New Stationary Sources, (NSPS) requires US EPA to establish federal emission standards for source categories which cause or contribute significantly to air pollution. Each NSPS defines the facilities subject to these requirements and prescribes emission limits for specific pollutants, compliance requirements monitoring requirements and test methods and procedures. These standards are intended to promote use of best air pollution control technologies, taking into account the cost of such technology and any other non-air quality, health, and environmental impact and energy requirements. These standards apply to sources which have been constructed or modified since the proposal of the standard. These standards can be found in the CFR at Title 40 (Protection of Environment), Part 60 (Standards of Performance for New Stationary Sources). Generally, state and local air pollution control agencies are responsible for implementation, compliance assistance, and enforcement of the NSPS. US EPA retains concurrent enforcement authority and is also available to provide technical assistance when a state of local agency seeks help. US EPA also retains a few of the NSPS responsibilities such as the ability to approve alternative monitoring methods to maintain a minimum level of national consistency. There are several federal and state regulations that apply to new source constructed and operating in an attainment area such as "Other Solid Waste Incineration Units" (OSWI) or "Commercial and Industrial Solid Waste Incineration Units" (CISWI). Brief overviews of these requirements are listed in subsections that follows. The Clean Air Act of 1970 directed US EPA to establish new source performance standards for specific industrial categories. There are few NSPS applicable to this project.

# D.02.01 NSPS — 40 CFR Part 60 Subparts CCCC and DDDD — Standards of Performance and Emission Guidelines and Compliance for Commercial and Industrial Solid Waste Incineration Units

Clean-Seas is subject to Subparts CCCC and DDDD as a Commercial and Industrial Solid Waste Incineration Unit.

Commercial and industrial solid waste incineration unit (CISWI) means any distinct operating unit of any commercial or industrial facility that combusts, or has combusted in the preceding 6 months, any solid waste as that term is defined in 40 CFR part 241. If the operating unit burns materials other than traditional fuels as defined in § 241.2 that have been discarded, and you do not keep and produce records as required by § 60.2740(u), the operating unit is a CISWI. While not all CISWIs will include all of the following components, a CISWI includes, but is not limited to, the solid waste feed system, grate system, flue gas system, waste heat recovery equipment, if any, and bottom ash system. The CISWI does not include air pollution control equipment or the stack. The CISWI boundary starts at the solid waste hopper (if applicable) and extends through two areas: The combustion unit flue gas system, which ends immediately after the last combustion chamber or after the waste heat recovery equipment, if any; and the combustion unit bottom ash system, which ends at the truck loading station or similar equipment that transfers the

ash to final disposal. The CISWI includes all ash handling systems connected to the bottom ash handling system.

Despite the applicability Subparts CCCC and DDDD and Clean-Seas units being determined to be CISWI units, Clean-Seas notes that the units do not utilize combustion in any way. The primary product from the facility, Plastic Pyrolysis Oil, is a marketable product. The syngas generated in the facility has sufficient BTU content to power the process, and the remaining residue is expected to have commercial applications as well, and the facility is therefore not subject to regulation as an industrial incinerator.

#### Clean-Seas Minor Source Construction Permit Application

Clean-Seas is proposing to construct and operate a Plastic Pyrolysis Plant. The proposed Clean-Seas facility will convert plastic to plastic pyrolysis oil (PPO) as a precursor to new plastic and ultra-low sulfur fuels, lubricants, and other products.

#### Plastic Feedstock Specifications

Clean-Seas only accepts feedstock that: (1) is plastic derived from industrial, commercial, agricultural, or other such activities; (2) is not mixed with solid waste or hazardous waste onsite or during processing at the facility; (3) is intended use as a feedstock for the manufacturing of plastic and chemical feedstocks, other basic hydrocarbons, raw materials, or other intermediate products or final products using advanced recycling; and (4) has been sorted from solid waste and other regulated waste but may contain residual amounts of solid waste such as organic material and incidental contaminants or impurities (e.g., paper labels and metal rings).

The feedstock is typically items made of polyethylene (LDPE, LLDPE, or HDPE) and polypropylene (PP) such as containers, trays, cups, films, and bags.

All items free of contents or free flowing liquids and rinsed.

Minimum 85% polyethylene or polypropylene

Maximum moisture content: 7%

# D.03 National Emission Standards for Hazardous Air Pollutants (NESHAP) (40 CFR Part 63)

The NESHAPs contained in 40 CFR 63 have been adopted by the USEPA to regulate hazardous air pollutants via industrial controls. There are no sources at the proposed facility which will be subject to these standards.

#### D.04 Chemical Accident Prevention (40 CFR Part 68)

The facility does not have more than a threshold quantity of the chemicals listed in this subpart;

therefore, this regulation does not apply.

#### D.05 State Operating Permit Programs (40 CFR 70)

West Virginia's Operating Permit Program applies to major sources of criteria pollutants or hazardous air pollutants. The proposed facility is below both of these thresholds and is not subject to this regulation.

#### D.06 Mandatory Greenhouse Gas Reporting (40 CFR 98)

The proposed facility is subject to greenhouse gas reporting in accordance with 40 CFR 98.2(a)(3). Specifically, all three of the conditions in this section have been met:

- The facility will meet the requirements of either 40 CFR 98.2(a)(1) or (a)(2).
- The aggregate maximum rated heat input capacity of the stationary fuel combustion units at the facility is 8 MMBTU/hr or greater.
- The facility emits 25,000 metric tons CO2e or more per year in combined emissions from all stationary fuel combustion sources.

#### D.07 Maximum Achievable Control Technology Standards

Maximum Achievable Control Technology (MACT) Standards were established under Section 112 of Clean Air Act for control of hazardous air pollutants ("HAPs"). These MACT standards are specified based on the category and subcategory list applicable to the major source. A minor source of HAPs is a source with total predicted HAP emissions of 25 TPY or greater or any single HAP emissions equal to 10 TPY or greater.

#### **MACT Applicability**

Predicted HAP emissions from the Clean-Seas' Plant are less than 25 tons per year total and less than 10 tons per year of any single HAP, hence Clean-Seas is not defined as a major source of HAPs.

#### D.08 Risk Management Plan

40 CFR 68 requires that Risk Management Plan (RMP) be developed for any regulated substance in excess of the threshold quantity as defined in subpart F. The Clean-Seas Plant does not have any regulated substance in excess of threshold limit.

#### D.09 Stack Height

The stack height regulations promulgated by U.S. EPA on July 8, 1985 (50 FE27892), established a stack height limitation to assure that stack height increases, and other plume dispersion techniques would not be used in lieu of constant emission controls. These regulations apply to facilities that commenced construction after December 31, 1970, and to dispersion techniques implemented after that date. These federal requirements have been included in the

regulations for Good Engineering Practice Stack Height. The regulations specify that Good Engineering Practice (GEP) stack height is the maximum creditable stack height a source may use in establishing its applicable State Implementation Plan (SIP) emission limitation. A GEP stack height means the greater of one of the following two options:

- 1. 65 meters, measured from ground-level elevation at the base of the stack (deminimus stack height); or
- 2. For stacks uninfluenced by terrain features, the determination of GEP stack height for a source is based on the following empirical equation:

$$Hg = H + H + 1.5Lb$$

Where:

Hg = GEP stack height;

H = Height of the structure on which the source is located, or

nearby structure; and

Lb = Lesser dimension (height or width) of the structure on which

the source is located, or nearby structure.

Both the height and width of the structure are determined from the frontal area of the structure projected onto a plane perpendicular to the direction of the wind. The area where a nearby structure can have significant influence on the source is limited to 5 times the lesser dimension (height or width) of that structure or within 0.5 mile (0.8 km) of the proposed stack, whichever is less. The methods for determining GEP stack height for various building configurations have been described in U.S. EPA's technical support document (U.S. EPA, 1985).

All stacks at Clean-Seas Plant are less than 65 meters in height.

#### **D1.0 State Regulations**

In addition to the federal air permitting requirements, the WVDEP applicable air quality regulations are summarized in this section.

The West Virginia Air Quality Standards and Regulations (DAQ) contains all state regulations applicable to the proposed site. All new or modified emission sources that are not specifically exempt from permitting requirements must obtain a construction and operating permit from the State of West Virginia Department of Environmental Protection Division of Air Quality prior to commencing construction and/or operation. This application and attached forms fulfill the information requirements needed to obtain a construction and operating permit required by regulation. Applicable sections include:

#### D1.01 45CSR10: Emission of Sulfur Dioxide

Clean-Seas' Plastic Pyrolysis System will burn the synthetic gas generated by, and powering, the pyrolysis reactor. The unit will use natural gas and propane. Both of these fuels have odorant for the purpose of leak detection. The quantities of SO2 from these sources is very low and below

reportable quantities. Plastic materials used as feedstock for the plant will be selected for low chemical content as such S emissions generating SO2 will be minor.

#### D1.02 45CSR13: "Minor New Source" Permit for Construction

Review permitting is divided into three categories:

 NSR (45CSR13) Preconstruction Permit — See Table 9.4 for pollutant NSR (45CSR13) Preconstruction — Requirements This is an existing infrastructure previously used for sales and storage of lumber and

construction materials.

Clean-Seas' Facility will meet all requirements as per NSR (45CSR13) See WVDEP 45CSR 13 Table 13A Revised and Table 1313 as well as Table 9.4.

All potential TAP and HAP emissions as listed in table 45-13A are calculated and included with this application. See permit application and attachments as listed under NSR (CSR13)

Respective Air Pollution for HAPs and TAPs See tables 9.4.1, 9.4.1A, 9.4.2 & 9.4.2A

- 2. 45CSR13 Hazardous Air Pollution (HAP)
- 3. 45CSR13 Toxic Air Pollution (TAP)

West Virginia Minor Source Air Permitting Program is enacted through 45CSR13 in which air Toxins are addressed in 45CSR 13. Any source that proposes to have the potential to emit before control at or above 2 lb/hr or 5 tpy of TAPs considered on aggregated basis for new facility. Clean-Seas will meet the necessary requirements. The EPA has determined that the following units do not require stringent regulations under Part 266, Subpart H.

- 1.0 Units burning gas recovered from hazardous or solid waste.
- 2.0 Units burning hazardous waste exempt from regulation 216.6(a)(s))iii)-v and maybe from 261.5
- 3.0 Applicability and exemptions, there are two classes of units covered under the Part 266, Subpart H. Regulation Boilers and Industrial Furnaces. EPA defines a boiler as an enclosed device that uses controlled flame combustion to recover and export energy in the form of steam. Boilers have a combustion chamber and energy recovery efficiency of 60 percent. Reference RCRA, 40 CFR Part 266H Boilers and Industrial Furnaces.

Emissions from Clean-Seas Operation — Attachments 'N' for all tables starting with No. 9.

- Table 9.4 Emission Factors/Emission Calculations Note 1 Attachment N
- b) Tables 9.4.1, 9.4.1A, 9.4.2 & 9.4.2A Emission Summary (Section 9.0)
- c) Table 9.4.3 Metals and Other Emission Factors/Emission (Section 9.0)
- d) TAP & HAP Emission Summary (Section 9.0)
   Organic HAPs Emission Summary (Section 9.0)
- e) Table 9.4.5 Hazardous Air Pollutants Summary (Section 9.0)

#### Including Metallic HAPs Summary

3.0 Emergency Generator (Section 9.0) Subsection 9.6.2 Generac 150 kw (Attachments I & J)

#### 1.0 Basic Operations & Process Description

Pre-approved plastic feedstock will arrive on the site via semi-trailer trucks and small box trucks. The plastic will be shipped in properly secured gaylord boxes, sacks or bales. The feedstock will be directly unloaded into the facility building. Once inside, the contents are unpacked, and prepared for processing.

The feedstock is manually fed into the American Renewable Technologies Inc. (ARTI) pyrolysis system, designed to operate on a continuous basis except for controlled, planned shutdowns.

#### 2.0 Emissions:

Emission from the following emission units

Emission Unit I.D.	<u>Description</u>	<u>Points</u>
1-S	Pyrolyzer Unit 1	1-E
2-S	Pyrolyzer Unit 2	2-E
3-S	Flare	3-E
4-S	Frac Tanks	4-E
5-S	Generator-backup	5-E
6-S	Truck Loading	6-E
IR	Paved Roads	IR-E

APCD	Description
1C	Pyrolysis Unit 1 Burner
2C	Pyrolysis Unit 2 Burner
3C	Flare

These air pollution components have been selected and arranged to provide targeted and redundant levels of removal for the "nine pollutants" of concern specified the Table 1B of 40 CFR part EC, for which Clean-Seas is not subject to, but are using for reference. These controls include Low NOx Burners (NOx control), and Flare to control emissions.

#### 3. 5-EG5 — Emergency Natural Gas Generator Unit (ID 5-EG5)

Emergency generator will be a Generac 150kWh natural gas generator and provide power during emergency events. The generator will be permitted for 100 hours per year for non-emergency uses including maintenance and upkeep activities.

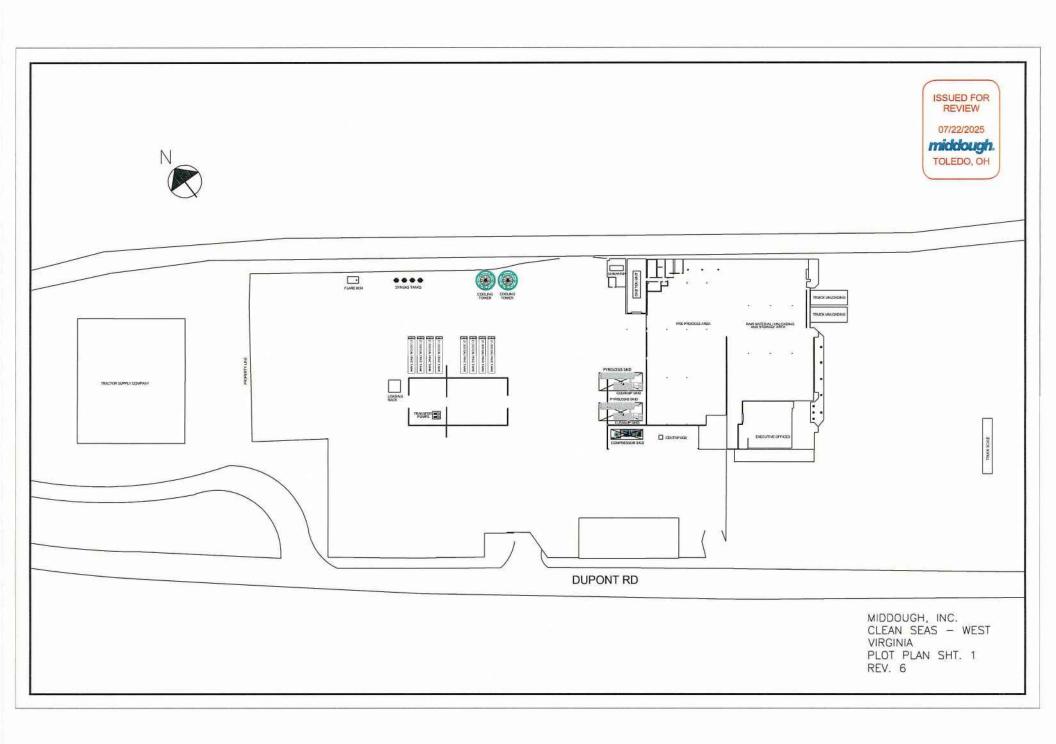
#### **D2.0** Insignificant Activities Exempt from Permitting

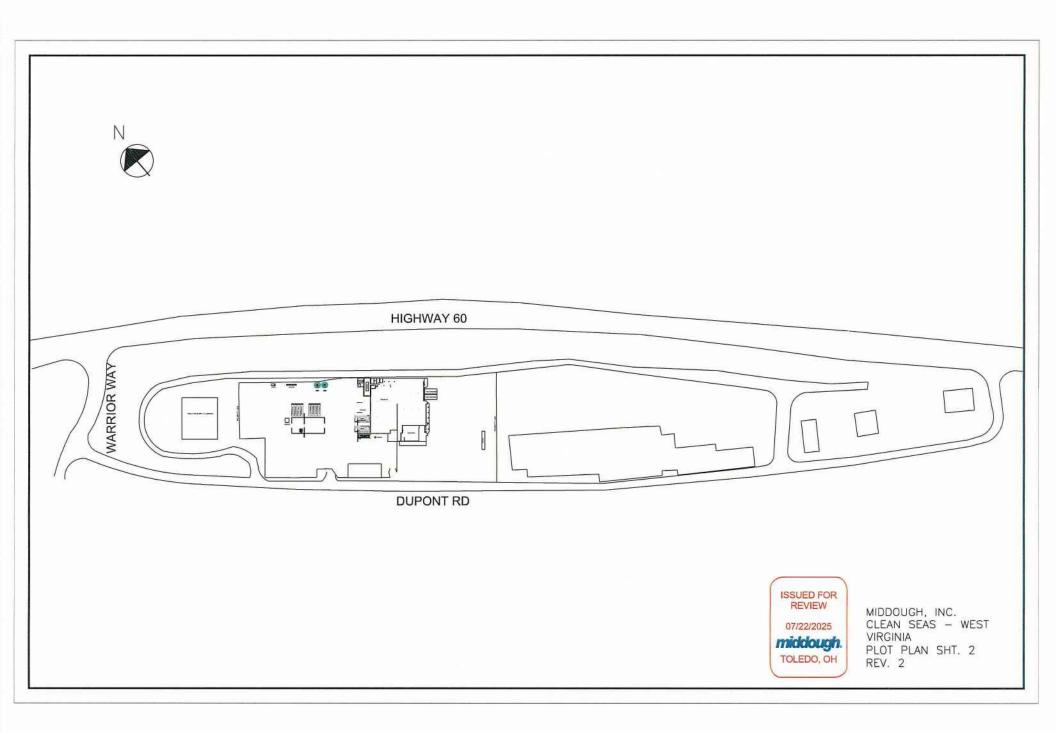
Certain sources, operations, and activities are considered to be insignificant based on following categories.

- A. Size or emission rate
- B. Type of activity
- C. Type of pollutant

#### Table List of Insignificant Activities

Insignificant Activity	Insignificant Activity
	Subcategory Class
- Two 0.2-MMBtuihr gas-fired HVAC furnaces	A-5
- Six 0.05-MMBtu/hr space heaters	





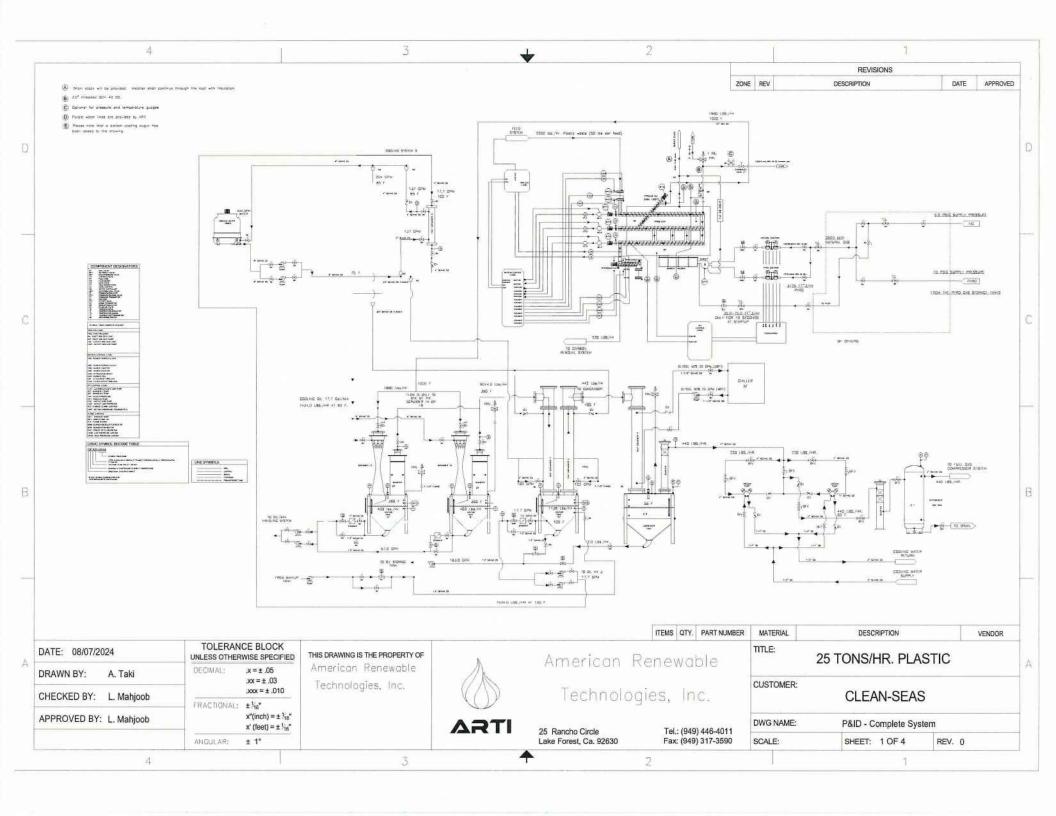


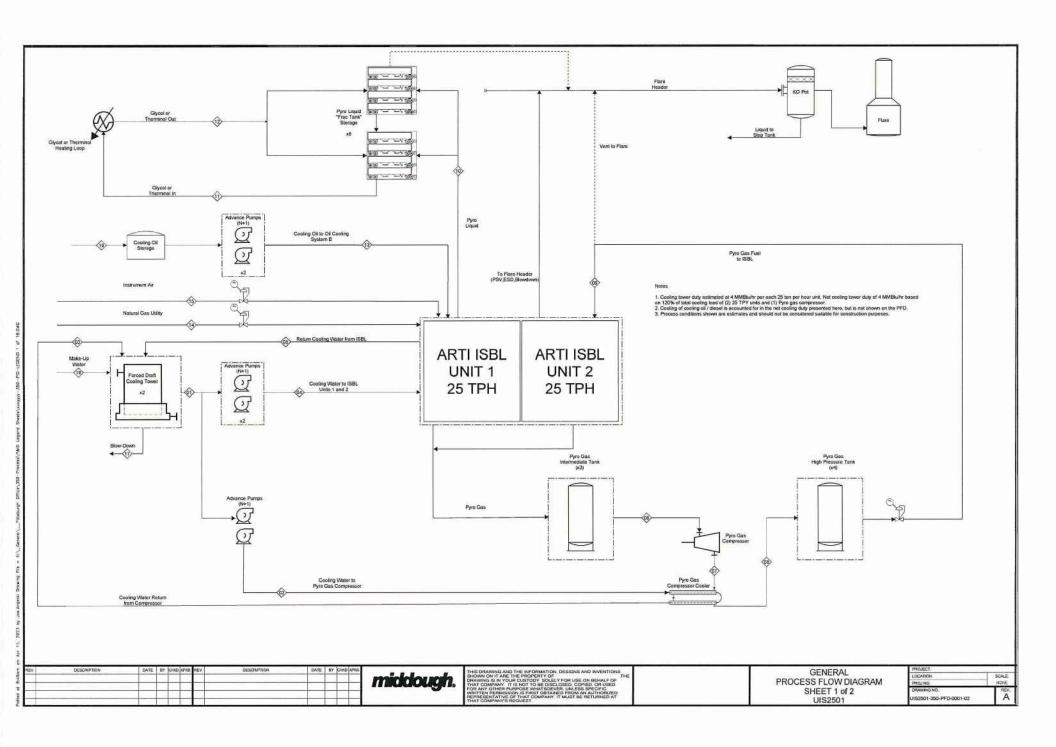


ISSUED FOR REVIEW

07/22/2025

middough. TOLEDO, OH MIDDOUGH, INC. CLEAN SEAS — WEST VIRGINIA PLOT PLAN SHT. 3 REV. 1





middou	igh.	01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16	17	18
		01	02	03	04	05	06	07	08	09	10	11	12	13	14	15	16	17	18
Total Properties	- Discourse																		
Temperature	The Fa	85.0	85.0	111.3	85.0	94.6	60.0	450.2	95.0	93.2	94.3	250.0	2211	95.0	100.0	70.0	85.0	85.0	95.0
Pressure	psig	10.0	10.0	10.0	10.0	10.0	13	100.0	100.0	10.0	1.3	10.0	5.0	5.0	5.0	100.0	0.0	0.0	13
Molar Flow	MMSCFD	89.2	2.5	2.5	86.7	86.7	0.4	0.4	0.4	0.4	6.32E-02	0.2	0.2	0.3	0.1	0.3	14	0.2	0.2
Mass Flow	lb/hr	176459.0	5027.3	5027.3	171431.7	171431.7	466.2	466.2	440.0	440.0	1057.3	500.0	500.0	7220.8	110,3	1000.0	2685.0	466.4	6141.9
Mass Enthalpy	Btullb	-6794.8	-6794.8	-6768.5	-6794.8	-6785.1	-1337.5	-1035.5	-1332.8	-1332.6	-925.6	-4848.4	-4874.1	-923.6	-1924.2	-2.7	-6794.8	-6794.8	-924.4
Vapour Fraction		0.00	0.00	0.00	0.00	0.00	1.00	1.00	1.00	100	0.00	0.00	0.00	0.00	1.00	1.00	0.00	0.00	0.00
Liquid Fraction	SOURCE OF THE PARTY	1.00	1.00	1,00	1.00	1.00	0.00	0,00	0.00	0.00	1.00	1.00	1.00	1.00	0.00	0.00	100	100	1.00
Vapor Properties				1 2	1 170		TI.nv.	D Thorn	I DELLO	I / /Florer	1 17000	75		D Reserve	T. OWLGO		1		
Std Gas Flow	MSCFD	228	I	I	I		371.3	371.3	361.8	361.8			ommin <del>i de</del> comes	<del></del>	60.0	314.6	I	I	
Actual Gas Flow	ACFM			† — —	1		237.4	57.9	34.3	159.0	i 1				33.4	28.3	<del> </del>	<u> </u>	T
Molar Flow	MMSCFD				<del> </del>		0.4	0.4	0.4	0.4					0.1	0.3			
Mass Flow	lb/hr			<del> </del>			466.2	468.2	440.0	440.0					110.3	1000.0	H		
Mass Enthalpy	Bullb			I	<del>   </del>		-1337.5	-1035.5	-1332.8	-1332.8					-1924.2	-2.7	H-I-		-
Molecular Weight			***				11.44	11.44	11.08	11.08					16.74	28.95			
Mass Density	1b/fe3			<u></u>	+ = -		0.03	0.13	0.21	0.05					0.06	0.59	h		
Mass Heat Capacity	Bu/lb-F			<del> </del>	+		0.03	0.85	0.74	0.03		<u></u>		<u></u>	0.53	0.55			
SG Air	re_to_air		H-II-		+-=-	<u>II</u>	0.71	0.00	0.74	0.73					0.53	1.00			<del> </del>
Compressibility	Tel man			<del> </del>			1.00	1.00	100	100					100	0.99			<u></u>
Co/Cv/Gamma)				<del> </del>			1.33	1.00	1.33	133		_==			100				Announce in the last
Higher Heating Value	Btu/SCF							<del></del>								142	ļ		
	THE RESERVE AND ADDRESS OF THE PARTY OF THE			ļ	T			ļ							1040.2				
Viscosity	оР			ļ <del></del>				ļ <del></del>		<del></del>					1.1644E-02				
GastWater Content	INMMSCF					344	777												
Liquid Properties	-													-			1 1 1 1 1 1 1	1 1000	100000
Standard Ideal Liquid Volume Flov	USGPM	353.1	10.1	10.1	343,1	343.1					2.669	0.9	0.9	17.4			5.373	0.9	14.8
Actual Volume Flov	USGPM	351.0	10.0	10.1	341,0	342.4					2.716	1.0	1.0	17.7		7-7-7	5.341	0.9	15,1
Molar Flow	lbmole/hr	9795.0	279.1	279.1	9515.9	9515.9					6.9444	17.9	17.9	32.0		Samuel TT Lance	149.0	25.9	27.3
Mass Flow	lb/hr	176459.0	5027.3	5027.3	171431.7	171431.7					1057.3	500.0	500.0	7220.8			2685.0	466.4	6141.9
Mass Enthalpy	Brulb	-6794.B	-6794.8	-6768.5	-6794.8	-6785.1			-		-925.6	-4848.4	-4874.1	-923.6			-6794.8	-6794.8	-924.4
Molecular Weight	The state of the s	18.0	18.0	18.0	18.0	18.0					152.3	27.9	27.9	225.3			18.0	18.0	225.0
Mass Density	Б/ <del>1</del> (3	62.7	62.7	62.0	62.7	62.4					48.5	61.6	62.5	50.9			62.7	62.7	50.8
Mass Density	SG_60/60api	1.0	1.0	1.0	1.0	1.0					0.8	1.0	10	0.8		- 1 <del>-</del>	10	1.0	0.8
Mass Heat Capacity	Bru/lb-F	1.0	1.0	1.0	10	1.0					0.5	0.9	0.9	0.5	I I		10	10	0.5
Compressibility		0.0	0.0	0.0	0.0	0.0		<del></del>			0.0	0.0	0.0	0.0			0.0	0.0	0.0
Cp/Cv (Gamma)		1.2	1.2	1.2	1.2	12					12	1.1	1.1	1.3	-		12	12	1,2
Viscosity	αP	0.8	0.8	0.6	0.8	0.7					13	0.5	0.6	4.7			0.8	0.8	4.8
Surface Tension	dyneicm	71.3	713	68.8	713	70.4	777				23.7	46.5	48.7	27.2		wa-	71.3	713	26.4
Reid VP at 37.8 C	psia							i			1.7			0.0					0.6
True VP at 37.8 C	psia										16.D			0.0			l		15.9
WatsonK								1			11.9			12.2					12.2

REV	DESCRIPTION	DATE	BA	OHD	APRID.	MIV.	DATE	CHAD	APHD.
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GENERAL PROCESS FLOW DIAGRAM SHEET 2 of 2 UIS2501

PROJECT				
LOCATION	SCALE			
PROJ NO.	NONE			
DRAWING NO.	REV.			
UIS2501-350-PPD-0001-02	I A			

#### Clean Seas Facility

#### Attachment G - Process Description

Clean Seas West Virginia LLC (Clean Seas) is constructing the Clean Seas facility near Belle in Kanawha County West Virginia. The facility will process plastics into marketable products: precursors for plastics, fuel, and oil.

This thermochemical pyrolysis process converts used plastic material into oil, gas and residue by heating in the absence of oxygen. The process involves breaking down large plastic molecules into smaller hydrocarbon molecules resulting in the production of these three main outputs.

The facility will receive plastic feedstock from outside suppliers. The supplier will clean and sort to remove paper, metals and dirt, and the plastic is then shredded into smaller pieces to increase the surface area in preparation for conversion.

The pyrolysis reactors feed the plastic through two valves sequenced to prevent escape of gases and air from entering the piping in the furnace. This piping is called a retort and has several passes that have powered augers to push the plastic through heating it to between 700F and 1200F. This temperature increase converts the plastic into oil, gas and residue.

Natural gas will be used to initially fire burners converting the plastic into pyrolysis oil, pyrolysis gas and solid residue. When sufficient non-condensable synthetic gas is generated, the two Pyrolysis furnace burners will be fueled by the synthetic gas using low NOx burners. The Pyrolysis equipment is combined onto a skid. The equipment will operate at a slight vacuum to prevent leakage.

Cooling, separation, centrifuge, pumping and refrigeration equipment separate the oil, gas and residue into concentrated streams that will be stored and sold. A flare will collect flows from pressure relief valves, vents and sources of overpressure due to shutdowns or upsets designed to efficiently combust gases preventing raw gas emissions to the atmosphere.

The pyrolysis oil (oil) will be stored in 8 portable storage tanks (Baker style) which will be nitrogen blanketed and have pressure vacuum vents connected to the flare. Nitrogen and the venting controls will eliminate emissions to the atmosphere as any vapors will go to the flare for combustion. Tanks will be in dikes to contain any spills. Oil will be sold and shipped by third party trucks. Truck loading will be a closed system to eliminate vapor emissions. Truck loading will have curbing to contain any potential spills. Trucks delivering plastic feedstock and shipping products will be weighed into and out of the facility.

A backup generator will provide backup electrical power to enable safe shutdown of the operations in the event of a power outage. This generator will reduce the possibility of flaring in the event of a power outage. The generator is intended for backup power and will be fueled by natural gas to reduce emissions.

Pyrolysis gases are the non-condensable gases, mainly methane, ethane, propane, butane, CO, CO2 and H2 that can be used as a fuel source to power the pyrolysis process or other industrial applications. Pyrolysis gases will be stored in cylinders for use in the pyrolysis process.

Solid residue will enter a covered bin to contain any dust. The residue will be sold for soil amendment or other applications.

The system consists of the following subsystems:

#### 1. The Furnace:

An insulated enclosure which contains two burners that provide the heat needed to sustain the pyrolysis process. The hot flue gases flow up and around the three retort tubes inside of the furnace before exiting the stack. The material in the inside diameter of the retorts are isolated from the furnace environment so the hot flue gases cannot come into direct contact with the process material being conveyed through the retorts. The furnace is equipped with burners capable of operating with natural gas or pyrolysis gas. The heat from the burners travels across the outer diameter of three passes to efficiently heat the retorts. The flue gas temperature is normally 150 to 200 °F above the retort operating temperature. The furnace is designed to allow the retorts to thermally expand and contract during the operation.

#### 2. The Retorts:

The retorts are installed within the furnace having an inlet and an outlet end. The material is fed to the retort via a double blade air sealed valve. This valve is important because it prevents the passage of air into the retort. The material is fed into the retorts from a manually loaded hopper, when the top blade opens it allows the material to enter the empty cavity of the valve below. Once the top blade has closed the bottom blade opens to feed the material into the retort. This valve is synchronized with an auger to introduce feed into the retort. As the feedstock material travels through the retorts it gasifies. The gases are collected under a slight negative pressure and flow out of the retorts. As the gasification sequence of the material ends, the residue exits the retorts through a similarly designed double blade valve thus maintaining the slight vacuum during the discharge of this residue. This residue is passed through a water-cooled auger to reduce the temperature to a level which is safe for handling.

The solid residue, typically a maximum 5% of the original value, can be landfilled or diverted to industrial use. At initial start-up Clean-Seas will transfer to EPA approved landfill as we characterize the material and find a beneficial use for it.

#### 3. The Augers:

The retorts are equipped with high temperature stainless steel augers which move the material from the inlet, through the retort, and finally to the discharge point. The speed of the augers can be changed at the Operator Control Panel to suit the material processed.

#### 4. The Burners:

The furnace is equipped with burners fueled with either natural gas or pyrolysis gas. The burners are supplied with a flame safeguard control and can be modulated to a higher firing rate on demand. A temperature control installed on the retorts allows the burner to start and to modulate. Once the burners are turned on, they modulate to a firing position where they heat the retorts to the pre-set temperature. When the temperature demand is satisfied the burners modulate back to the lower firing rate. If the temperature exceeds its preset upper limit the burners automatically shut down. If the retort temperature falls below the lower set point the burner will automatically start and raise the temperature back to the upper set point.

#### 5. The Cyclone Separator:

The Cyclone Separator is installed at the exhaust point of the gases. This unit will separate any particles from the gas before the gas travels to the gas Particle Wash System.

#### 6. The Particle Wash System:

The Particle Wash System is installed after the Cyclone Separator. The Particle Wash System contains 10 to 15 gallons of light oil. The Wash Pump energizes as the unit starts to operate and recirculates the washing media. This washing process takes place in a venturi and any heavy particles such as tar or wax can be removed from the gas and will be retained within the Particle Wash System. A glass level indicator is supplied with the Particle Wash System. The unit must be drained from time to time to keep the level low enough for the gas to travel through. Once the gas has been cleaned through the venturi it travels through the demister and liquid particles are stripped from the gas.

#### 7. The Condenser:

As the gas exits the Particle Wash System, it enters a Vertical Condenser. All condensable gases or water is stripped from the gas and non-condensable gases travel through another demister to the gas blowers.

#### 8. The Gas Blower

A Gas Blower is supplied to remove the gases from the system while maintaining the slight negative pressure within the system. It is a Roots-type positive displacement blower. The blower is controlled through the use of a pressure transducer installed on the retort. This transducer senses the rate of gasification. As the gasification process gas flow changes, the retort pressure rises or falls and sends a signal to the blower speed control to compensate. In this way the operating retort vacuum is maintained at a preset level. This ensures the quality and uniformity of the byproducts.

#### 9. PPO Product Storage

Once plastic pyrolysis oil liquid exits the process, it is then sent to storage prior to shipping to offtakers. The oil will be stored in (8) 21,000 gallon portable storage tanks (Baker Style) tanks with a maximum of 18,000 gallon storage capacity to allow freeboard space for thermal expansion of material. The tanks have an internal coil that will allow the flow of heated water to keep the contents above pour point temperature ~100F

#### 10. PPO Loading Rack

The PPO will be transported via pipe to a loading rack. Trucks will enter the facility to transfer oil into approved tanker trailers supplied by the offtaker. The system will be closed loop, meaning that the vapors from the tanker will enter the process to eliminate venting of vapors to the atmosphere.

#### Attachment I **Emissions Unit Table**

(includes all emission units and air pollution control device

that will be part of this permit aplication review, regardles of permit status)

Emissions Unit IDEmissions Units DescriptionYear Installed / ModifiedDesign CapacityType and Date of Change1S1EPyrolysis Unit #1TBD3 mmBTU/HrNew2S2EPyrolysis Unit #2TBD3 mmBTU/HrNew3S3EFlareTBD1-5 mmBTU/HrNew4S4EFrac Tanks (8 total)TBD21,000 gal/tkNew5S5EGenerator Nat Gas FuelTBD150 kWhNew6S6ETruck Loading RackTBD15k gal/dayNew7S7EGycol Circulation HeaterTBD2.5 mmBTU/HrNew8S8ETRE-Training, Research & EvalTBD0.2 mmBTU/HrNew9S9ETRE-FlareTBD0.1 mmBTU/HrNew	Control Device
Unit IDPoint IDModifiedCapacityChange1S1EPyrolysis Unit #1TBD3 mmBTU/HrNew2S2EPyrolysis Unit #2TBD3 mmBTU/HrNew3S3EFlareTBD1-5 mmBTU/HrNew4S4EFrac Tanks (8 total)TBD21,000 gal/tkNew5S5EGenerator Nat Gas FuelTBD150 kWhNew6S6ETruck Loading RackTBD15k gal/dayNew7S7EGycol Circulation HeaterTBD2.5 mmBTU/HrNew8S8ETRE-Training, Research & EvalTBD0.2mmBTU/HrNew	Western Branch
2S 2E Pyrolysis Unit #2 TBD 3 mmBTU/Hr New  3S 3E Flare TBD 1-5 mmBTU/Hr New  4S 4E Frac Tanks (8 total) TBD 21,000 gal/tk New  5S 5E Generator Nat Gas Fuel TBD 150 kWh New  6S 6E Truck Loading Rack TBD 15k gal/day New  7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New  8S 8E TRE- Training, Research & Eval TBD 0.2mmBTU/Hr New	12 22
3S 3E Flare TBD 1-5 mmBTU/Hr New 4S 4E Frac Tanks (8 total) TBD 21,000 gal/tk New 5S 5E Generator Nat Gas Fuel TBD 150 kWh New 6S 6E Truck Loading Rack TBD 15k gal/day New 7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New 8S 8E TRE- Training, Research & Eval TBD 0.2mmBTU/Hr New	1C
4S 4E Frac Tanks (8 total) TBD 21,000 gal/tk New 5S 5E Generator Nat Gas Fuel TBD 150 kWh New 6S 6E Truck Loading Rack TBD 15k gal/day New 7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New 8S 8E TRE- Training, Research & Eval TBD 0.2mmBTU/Hr New	2C
5S 5E Generator Nat Gas Fuel TBD 150 kWh New 6S 6E Truck Loading Rack TBD 15k gal/day New 7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New 8S 8E TRE-Training, Research & Eval TBD 0.2mmBTU/Hr New	3C
6S 6E Truck Loading Rack TBD 15k gal/day New 7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New 8S 8E TRE- Training, Research & Eval TBD 0.2mmBTU/Hr New	4C
7S 7E Gycol Circulation Heater TBD 2.5 mmBTU/Hr New 8S 8E TRE- Training, Research & Eval TBD 0.2mmBTU/Hr New	5C
8S 8E TRE-Training, Research & Eval TBD 0.2mmBTU/Hr New	6C
	7C
9S 9E TRE-Flare TBD 0.1 mmBTU/Hr New	8C
	9C

<sup>&</sup>lt;sup>1</sup> For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
<sup>2</sup> For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.

3 New, modification, removal

<sup>&</sup>lt;sup>4</sup> For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

### Attachment J EMISSION POINTS DATA SUMMARY SHEET

							Table 1:	Emissions D	ata <sup>7</sup>	est Data	provided i	by ARTI			
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type <sup>1</sup>	Ven Throug Po (Must Emissio	ion Unit nted gh This pint match on Units Plot Plan)	Air Pollution Control Device (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS³ (Speciate VOCs & HAPS)	Maximum Potential Uncontrolled Emissions <sup>4</sup>		Maximum Potential Controlled Emissions <sup>5</sup>		Emission Form or Phase (At exit canditions, Solid, Liquid	Est. Method Used <sup>6</sup>	Emission Concentration <sup>7</sup> (ppmv or mg/m³)
		ID No.	Source	ID No.	Device Type	Shart Term²	Max (hr/yr)	patriere	lb/hr	ton/yr	lb/hr	ton/yr	Gas/Vapor)		
1E	UPWARD STACK	18	BURNER	10	ANALYZER	С	8,000	NOx CO PE VOC	.12 .12 .0015 0.0	0.872 0.872 0.010 0.000	0.12 0.12 0.005 0.000	0.872 0.872 0.010 0.000	GAS	ST	30 PPM 50 PPM 0.005LB/MMBTU 0.0 PPM
2E	UPWARD STACK	28	BURNER	2C	ANALYZER	С	8,000	NOx CO PE VOC	.12 .12 .0015 0.0	0.872 0.872 0.010 0.000	0.120 0.120 0.005 0.000	0.436 0.436 0.005 0.000	GAS	ST	30 PPM 50 PPM 0.005 LB/MMBTU 0.0 PPM
3E	UPWARD STACK	3S	BURNER	3C	ANALYZER	note A	144	NOx CO PE VOC	0.240 0.240 0.003 0.000	0.047 0.047 0.0 0.0 0.0	0.240 0.240 0.003 0.000	0.047 .013 0.00 0.00	GAS	ST	30 PPM 50 PPM 0 PPM 0 PPM
4E	Upward Vent to Flare	4S	Press vac vent	4C	Process Monitoring	To Flare	N/A	VOCs	TBD	TBD	TBD	TBD	Vapor/N2 to flare	EE	TBD
5E	Upward Stack	58	Natural gas engine	5C	Catalytic Converter	During Power Outage	70	NOx CO PE VOC	0.878 Nil	0.030 0.029 Nil 0.008	0.050 0.374 Nil 0.071	0.002 0.012 Nil 0.002	Gas	ST	TBD
6E	Vapor to Tank	6S	Vapor Line From Truck	6C	vapor contain- ment	During Truck Loading	1,500	VOCs	TBD	TBD	TBD	TBD	Gas	EE	TBD
7E	Upward Stack	7S	Burner	7C	Low NOx Burners	Heat for Process Tanks / Lines	8,760	NOx CO PE VOC	0.100 0.400 0.018 0.015	1.752 0.077	0.075 0.400 0.018 0.015	0.329 1.752 0.077 0.066	Gas	EE	TBD
8E	Upward Stack	88	TRE Burner	8C	Samples During Trials	Test & Training 4 days / week	1,000	NOx CO PE VOC	0.032 0.001	0.035 0.140 0.006 0.005	0.006 0.032 0.001 0.001	0.026 0.140 0.006 0.005	Gas	EE	TBD
9E	Upward Stack	98	TRE Flare	9C	Samples During Trials	Test & Training 4 days / week	1,000	NOx CO PE VOC	0.016 0.001	0.002 0.008 0.000 0.001	0.004 0.016 0.001 0.001	0.002 0.008 0.000 0.001	Gas	EE	TBD

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

<sup>&</sup>lt;sup>1</sup> Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

<sup>&</sup>lt;sup>2</sup> Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

<sup>3</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO., CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O3, and Noble Gases.

<sup>&</sup>lt;sup>4</sup> Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>5</sup> Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>6</sup> Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

<sup>7</sup> Books for the substant and the second seco

Provide for all pollutant emissions. Typically, the units of parts per milluse units of milligram per dry cubic meter (mg/m³) at standard conditions (i	ilion by volume (ppmv) are u 68 °F and 29.92 inches Hg) (	sec. If the emission is a mineral acid (sulfur see 45CSR7). If the pollutant is $SO_2$ , use uni	c, nitne, nyaroeniorie or pnospnorie) s of ppmv (See 45CSR10).						
Note A Flare operational for approximately 2x/mo for 6 hrs each SU/SD event for 144hrs/yr									
	page _1_ of _2_		WVDEP-DAQ Revision 2/11						

#### Attachment J **EMISSION POINTS DATA SUMMARY SHEET**

			Table 2: Rel	ease Faiaili	elei Dala		T		
Emission Point ID No. (Must match Emission Units Table)	Inner Diameter (ft.)		Exit Gas		Emission Point E	levation (ft)	UTM Coordinates (km)		
		Temp. (°F)	Volumetric Flow <sup>1</sup> (acfm) at operating conditions	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height <sup>2</sup> (Release height of emissions above ground level)	Northing	Easting	
1S	14 INCHES	460	1700	26.5	1500 FT	35 FT			
2S	14 INCHES	460	1700	26.5	1500 FT	35 FT			
3S	24 INCHES	1800	11820	62.0	1500 FT	35 FT			
4S	TBD	1440	TBD	1500FT	TBD				
5S	TBD	TBD	TBD 1	500FT	TBD				
6S	TBD	TBD	TBD	TBD	1500FT	TBD			
7S	TBD	TBD	TBD	TBD	1500FT	TBD			
8S	TBD	TBD	TBD	TBD	1500FT	TBD			
9S	TBD	TBD	TBD	TBD	1500FT	TBD			

<sup>&</sup>lt;sup>1</sup>Give at operating conditions. Include inerts. <sup>2</sup> Release height of emissions above ground level.

#### Attachment K

#### **FUGITIVE EMISSIONS DATA SUMMARY SHEET**

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	☐ Yes No
	☐ If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
	☐ Yes No
	$\begin{tabular}{l} \hline \end{tabular} If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET. \\ \hline \end{tabular}$
3.)	Will there be Liquid Loading/Unloading Operations?
	Yes No
	If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	☐ Yes No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	Yes No
	If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	Yes No
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	☐ Yes No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
	ou answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions mmary."

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FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants - Chemical Name/CAS <sup>1</sup>	Maximum Uncontrolled		Maximum Po Controlled Em	Est. Method		
	Official Name, OAO	lb/hr	ton/yr	lb/hr	ton/yr	Used <sup>4</sup>	
Haul Road/Road Dust Emissions Paved Haul Roads	N/A						
Unpaved Haul Roads	N/A						
Storage Pile Emissions	N/A						
Loading/Unloading Operations	Diesel Fuel / 68334-30-5 Plastics Pyrolysis Oil/ Not Available	.015lb/connect	0.005 ton/yr	.0015lb/connect	.0005 ton/yr	EPA 42 7.1=9	
Wastewater Treatment Evaporation & Operations	N/A						
Equipment Leaks Reference EPA AP-42 section 7.1.4-9	Process Equipment – pumps, exchangers, valves, piping, relief valves, compressors, sample stations, loading hoses, etc.	Does not apply	VOCs 25 tons/yr	Does not apply	VOCs 4.376	EPA 42 7.1-9	
General Clean-up VOC Emissions See estimates on pages 3 and 4	Operation and Maintenance of the equipment listed above	3.03 lb/hr	12.1 tons/yr	0.0003 lb/hr	2.67 lb/yr	AP-42 7.1-9	
Other							

<sup>&</sup>lt;sup>1</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.

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<sup>&</sup>lt;sup>2</sup> Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>3</sup> Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>4</sup> Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

## EPA 42 equipment leak emission factors for

6 50hp pumps, 6 small heat exchangers at 1psi, 6 small relief valves set at 60psi, 2 small compressors 4psi in 65 psi out, rubber truck loading hoses used 12 times per week

•			
Equipment Type	Service Pressure	Unit Emission Factor	Reference (AP-42, Section 7.1.4)
Centrifugal Pump (unpressurized seal)	-	0.11 lb/hr per seal	Table 7.1-4, Light Liquid Service
Centrifugal Pump (pressurized seal)	_	0.50 lb/hr per seal	Table 7.1-4, Light Liquid Service
Small Heat Exchanger (shell-and-tube)	1 psig	0.06 lb/hr per exchanger	Table 7.1-7
Pressure Relief Valve	Set at 60 psig	0.03 lb/hr per valve	Table 7.1-8
Reciprocating Compressor	4 psig inlet / 65 psig outlet	2.2 lb/hr per compressor	Table 7.1-5
Truck-Loading Hose	12 connect/disconnects per week	0.015 lb/event (0.18 lb/week)	Table 7.1-9

## EPA 42 controlled equipment leak emission factors for

6 50hp pumps, 6 small heat exchangers at 1psi, 6 small relief valves set at 60psi, 2 small compressors 4psi in 65 psi out, rubber truck loading hoses used 12 times per week

Equipment Type	Uncontrolled EF (lb/hr or lb/event)	Control Efficiency (%)	Controlled EF (lb/hr or lb/event)
Centrifugal Pump (50 hp, light liquid)	0.50 lb/hr per seal	90	0.05 lb/hr per seal
Small Heat Exchanger (1 psig)	0.06 lb/hr per exchanger	90	0.006 lb/hr per exchanger
Relief Valve (60 psig)	0.03 lb/hr per valve	90	0.003 lb/hr per valve
Reciprocating Compressor	2.2 lb/hr per unit	90	0.22 lb/hr per unit
Truck-Loading Hose (per connect/disconnect)	0.015 lb/event	90	0.0015 lb/event

Controlled emission factors assume a generic **90% reduction** from typical LDAR (Leak Detection and Repair) or equivalent control program as referenced in EPA guidance (e.g., EPA OAQPS memorandum on LDAR efficiencies).

Applying Controlled Factors

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Each controlled factor is calculated as:

controlled EF = uncontrolled EF  $\times$  (1 – control efficiency)

For example, a centrifugal pump uncontrolled factor of 0.50 lb/hr with 90% control yields 0.05 lb/hr.

#### Total Controlled Emissions Calculation

To estimate your facility's controlled emissions:

- 1. Pumps: 6 pumps  $\times$  2 seals each  $\times$  0.05 lb/hr = 0.60 lb/hr
- 2. Heat exchangers: 6 × 0.006 lb/hr = 0.036 lb/hr
- 3. Relief valves: 6 × 0.003 lb/hr = 0.018 lb/hr
- 4. Compressors: 2 × 0.22 lb/hr = 0.44 lb/hr Sum of 1-4 = 1.094 lb/hr Annual 8000hrs x 1.094 / 2000 lbs/ton= 4.376 Tons/yr Controlled
- 5. Loading hoses: 12 events/week × **0.0015 lb/event** = **0.018 lb/week**

Convert to consistent units as needed (e.g., lb/year or kg/year).

#### EPA 42 general clean up voc emission factors for

6 50hp pumps, 6 small heat exchangers at 1psi, 6 small relief valves set at 60psi, 2 small compressors 4psi in 65 psi out, rubber truck loading hoses used 12 times per week

#### **Pumps and Mechanical Seals**

For each of the six **50 hp centrifugal pumps**, AP-42 Table 7.1-4 gives an emission factor of **0.28 lb/hr** under clean-up service conditions with mechanical seals. Total VOCs from pumps = 6 pumps × 0.28 lb/hr = **1.68 lb/hr**.

#### **Heat Exchangers**

Each of the six small shell-and-tube heat exchangers leaking at **1 psig** uses gasketed flanges. AP-42 Table 7.1-5 lists **0.015 lb/hr** per exchanger. Total VOCs = 6 exchangers  $\times$  0.015 lb/hr = **0.09 lb/hr**.

#### **Relief Valves**

Six small relief valves set at **60 psig** in chemical service emit **0.20 lb/hr** each (AP-42 Table 7.1-6). Total VOCs = 6 valves × 0.20 lb/hr = **1.20 lb/hr**.

## Compressors

Two reciprocating compressors with **4 psig** suction and **65 psig** discharge fall under AP-42 Table 7.1-7. The factor is **0.032 lb/hr** per unit. Total VOCs =  $2 \text{ compressors} \times 0.032 \text{ lb/hr}$ .

## **Rubber Truck Loading Hoses**

AP-42 Section 5.2.3 provides a *per-unload* factor of **0.006 lb VOC** for rubber hoses in tank truck loading. At **12 unloads per week**, annualized emissions are: 12 unloads/week × 52 weeks × 0.006 lb = **3.74 lb/year**.

## **Annual and Hourly Totals**

• Hourly Total (continuous leaks)
1.68 (pumps) + 0.09 (exchangers) + 1.20 (valves) + 0.064 (compressors) = 3.03 lb/hr

• Annual Hose Emissions 3.74 lb/year (hose fugitive only)

## EPA 42 general clean up controlled voc emission factors for

6 50hp pumps, 6 small heat exchangers at 1psi, 6 small relief valves set at 60psi, 2 small compressors 4psi in 65 psi out, rubber truck loading hoses used 12 times per week

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\*Assumes operation (52 hr exchanger weeks). per per week \*\*Assumes relief two valve actuations per year. \*\*\*Assumes 2 hr/week operation (52 weeks). **Direct Annual Emissions Summary** The total VOC emissions from all listed annual equipment are: pumps × 0.19) + (6 exchangers × 0.005) + (6 valves × 0.02) + (2 compressors × 0.63) + (1 hose set × 0.12)= 1.14 + 0.03 + 0.12 + 1.26 + 0.12 = 2.67 lb VOC/yr

#### **Notes on Calculations**

- The pump factor comes from a generic reciprocating seal system (AP-42 Section 7.1).
- For **heat exchangers**, emissions are negligible; assumed minimal purge and leakage hours.
- Relief valves in non-fire cases are rarely actuated; default two events per year.
- Compressors use the same seal-leakage factors as pumps but scaled to horsepower and operating hours.
- Loading hoses use AP-42's storage-tank loading emission fraction adjusted to cycles.

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## Attachment L EMISSIONS UNIT DATA SHEET BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification Nu	mber (as assigned	d on <i>Equipment Li</i>	ist Form):				
1. Loading Area	Name:						
2. Type of cargo vessels accommodated at this rack or transfer point (check as many as apply):  □ Drums □ Marine Vessels □ Rail Tank Cars □ Tank Trucks							
3. Loading Rack	or Transfer Point	Data:					
Number of pu	mps						
Number of liqu	uids loaded						
Maximum number of marine vessels, tank trucks, tank cars, and/or drums loading at one time							
Does ballasting of marine vessels occur at this loading area?     ☐ Yes ☐ No ☐ Does not apply							
5. Describe cleaning location, compounds and procedure for cargo vessels using this transfer point:							
6. Are cargo vessels pressure tested for leaks at this or any other location?  ☐ Yes ☐ No  If YES, describe:							
7. Projected Ma	ximum Operating	Schedule (for rac	k or transfer point	as a whole):			
Maximum	Jan Mar.	Apr June	July - Sept.	Oct Dec.			
hours/day							
days/week							

weeks/quarte	er							
8. Bulk Liqui	id D	ata (add pages as	s necessar	y):		1		Т
Pump ID No.								
Liquid Name								
Max. daily thro	ough	put (1000 gal/day)						
Max. annual t	hrou	ghput (1000 gal/yr)						
Loading Meth	od <sup>1</sup>							
Max. Fill Rate	(gal	/min)						
Average Fill T	ïme	(min/loading)						
Max. Bulk Liq	uid 1	emperature (°F)						
True Vapor Pressure <sup>2</sup>								
Cargo Vessel	Cargo Vessel Condition <sup>3</sup>							
Control Equipment or Method <sup>4</sup>								
Minimum control efficiency (%)								
Maximum	Lo	ading (lb/hr)						
Emission Rate	An	nual (lb/yr)						
Estimation Me	ethod	d <sup>5</sup>						
<sup>1</sup> BF = Bottom	ı Fill	SP = Splash F	ill SUB	B = Subm	nerged Fill			
<sup>2</sup> At maximum bulk liquid temperature								
<sup>3</sup> B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)								
List as many as apply (complete and submit appropriate <i>Air Pollution Control Device Sheets</i> ):CA = Carbon Adsorption								
<sup>5</sup> EPA = EPA MB = Mater		ission Factor as sta alance	ited in AP-4	12				

TM = Test Measurement based upon test data submittal O = other (describe)

## 9. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING	RECORDKEEPING
Attended truck driver loading	Loading comments, spill reporting, bills of lading
REPORTING	TESTING
Incident reporting	

**MONITORING.** PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

**RECORDKEEPING.** PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

**REPORTING.** PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

**TESTING.** PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

Design is in progress

Truck Loading Rack 4mm gallons/yr 6000 gal/truck

> 15385 gal/workday 3957642.9 gal/yr 2.6 trucks/day 12.8 trucks/week 100.0 loading rate gpm 153.8 loading time minutes 2.6 hrs Loading time/day

> > 613.3 Annual loading hours

The estimated True Vapor Pressure (TVP) for the plastics pyrolysis oil at \*\*100°F\*\* is approximately \*\*1.43 psia\*\*.

The estimated True Vapor Pressure (TVP) for the plastics pyrolysis oil at \*\*60°F\*\* is approximately \*\*0.42 psia\*\*. As always, this is a rough estimate based on assumed Antoine constants. For more accurate results, specific constants for the actual pyrolysis oil should be used.

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# Attachment L EMISSIONS UNIT DATA SHEET STORAGE TANKS

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

### I. GENERAL INFORMATION (required)

1.	Bulk Storage Area Name	2.	Tank Name			
	Baker Tanks		PPO Baker Tanks			
3.	Tank Equipment Identification No. (as assigned on <i>Equipment List Form</i> )	4.	Emission Point Identification No. (as assigned on <i>Equipment List Form</i> )			
	4E, 4S Baker Tanks 1-8		4 E			
5.	Date of Commencement of Construction (for existing	tank	rs) TBD			
6.	Type of change ⊠ New Construction □ N	lew	Stored Material			
7.	Description of Tank Modification (if applicable) Eight (8) Tanks (21,000 gallons each) will be leased or pu	urcha	ased and installed in tank dikes designed to hold 110% of			
	contents plus planned rainfall (TBD). Nitrogen purge and atmosphere.	d ver	nting to the flare will prevent emissions of vfapor to the			
	Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tank	k?)	⊠ Yes □ No			
7B.	7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).					
	During statup and shutdown one of the PPO tanks to hold intermediates will be reprocessed to meet sales specs.	start	up products before meeting specifications for sales. These			
7C.	7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.):					
	Tanks to be heated in the winter, purged with nitrogen and vapors vented to the flare for safe and low emissions operation.					
•	II. TANK INFORM	ATIO	ON (required)			
8.	Design Capacity (specify barrels or gallons). Use height.	the	internal cross-sectional area multiplied by internal			
	Tanks size 21,000 gallons with					
9A.	Tank Internal Diameter (ft)	9B.	Tank Internal Height (or Length) (ft)			
	rectangular		length 36 ft			
10A	A. Maximum Liquid Height (ft)	10E	3. Average Liquid Height (ft)			
	9.75 ft		8.4 ft			
11A	A. Maximum Vapor Space Height (ft)	11E	B. Average Vapor Space Height (ft)			
	9.75		5 ft			
12.	Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights.		-			
	18,00	)0 ga	llons			

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)
3.96 mm gal/yr	10,850 gal
14. Number of Turnovers per year (annual net throughpu 27.5 turno	t/maximum tank liquid volume) overs per year
15. Maximum tank fill rate (gal/min) 8.33 gal/min	
16. Tank fill method ⊠ Submerged	☐ Splash
17. Complete 17A and 17B for Variable Vapor Space Tar	nk Systems
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year
18. Type of tank (check all that apply):  ☐ Fixed Roof vertical horizontal  other (describe)  ☐ External Floating Roof pontoon roof  ☐ Domed External (or Covered) Floating Roof	
<ul> <li>☐ Internal Floating Roof</li> <li>☐ Variable Vapor Space</li> <li>☐ Pressurized</li> <li>☐ Underground</li> <li>☐ Other (describe) rectangular frac tank, N2 purged and</li> </ul>	diaphragm
III. TANK CONSTRUCTION & OPERATION INFORMA	ATION (optional if providing TANKS Summary Sheets)
19. Tank Shell Construction:	d mirrata
☐ Riveted ☐ Gunite lined ☐ Epoxy-coated  20A. Shell Color TBD 20B. Roof Color	T .
21. Shell Condition (if metal and unlined):	<u> </u>
☐ No Rust ☐ Light Rust ☐ Dense Ru  22A. Is the tank heated? ☐ YES ☐ NO	ust Not applicable
	100F
22C. If YES, please describe how heat is provided to ta	ank. 50/50 Glycol/water circulation from a natural gas
23. Operating Pressure Range (psig): 0 to 2 psig	
24. Complete the following section for Vertical Fixed Ro	of Tanks 🗵 Does Not Apply
24A. For dome roof, provide roof radius (ft)	
24B. For cone roof, provide slope (ft/ft)	
25. Complete the following section for Floating Roof Tar	nks Does Not Apply
25A. Year Internal Floaters Installed:	
25B. Primary Seal Type: ☐ Metallic (Mechanical) (check one) ☐ Vapor Mounted Resili	
25C. Is the Floating Roof equipped with a Secondary S	Seal?
25D. If YES, how is the secondary seal mounted? (che	eck one) Shoe Rim Other (describe):
25E. Is the Floating Roof equipped with a weather shie	eld?

25F. Describe deck fittings; indica	te the number of ea	ch type of fitting:				
	ACCESS	S HATCH				
BOLT COVER, GASKETED: TBD	UNBOLTED COVER, GASKETED: UNBOLTED COVER, UNGASKETED:					
	ALITOMATIC GAL	JGE FLOAT WELL	i .			
BOLT COVER, GASKETED: TBD	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:			
	COLUM	N WELL				
BUILT-UP COLUMN – SLIDING COVER, GASKETED: TBD	BUILT-UP COLU COVER, UNGASH		PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:			
	LADDE	R WELL	i			
PIP COLUMN – SLIDING COVER, G TBD			SLIDING COVER, UNGASKETED:			
	GAUGE-HATCH	//SAMPLE PORT				
SLIDING COVER, GASKETED: TBD		SLIDING COVER	, UNGASKETED:			
	ROOF LEG OR	HANGER WELL				
WEIGHTED MECHANICAL ACTUATION, GASKETED: TBD		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)			
	VACIIIM	BREAKER	İ			
WEIGHTED MECHANICAL ACTUAT TBD			ANICAL ACTUATION, UNGASKETED:			
	RIM.	· VENT				
WEIGHTED MECHANICAL ACTUAT TBD			ANICAL ACTUATION, UNGASKETED:			
	DECK DRAIN (3-	INCH DIAMETER)				
OPEN:	DEGREDIVAN (O-	90% CLOSED:				
	OT' IS	DDAIN				
STUB DRAIN 1-INCH DIAMETER:						
	DIDE 4	NTION	IE NEOEO AES 2			
OTHER (DESC Tanks not purchased or leased at this tim	RIBE, ATTACH ADI e.	DITIONAL PAGES I	IF NECESSARY)			

26. Complete the following section for Internal	Floating R	oof Tank	s	□ Does Not Apply	,		
26A. Deck Type: Bolted We	elded						
26B. For Bolted decks, provide deck constru	uction:						
26C. Deck seam:							
☐ Continuous sheet construction 5 feet wi ☐ Continuous sheet construction 6 feet wi							
Continuous sheet construction 7 feet w							
☐ Continuous sheet construction 5 × 7.5 f ☐ Continuous sheet construction 5 × 12 fe							
Other (describe)							
26D. Deck seam length (ft)		26E.	Are	ea of deck (ft²)			
For column supported tanks:		26G.		meter of each column:			
26F. Number of columns:							
IV. SITE INFORMANTION	(optional it	f providir	ıg T	ANKS Summary Sheet	s)		
27. Provide the city and state on which the dat	a in this se	ction are	: ba	sed.			
28. Daily Average Ambient Temperature (°F)							
29. Annual Average Maximum Temperature (°	F)						
30. Annual Average Minimum Temperature (°F	=)						
31. Average Wind Speed (miles/hr)							
32. Annual Average Solar Insulation Factor (B	TU/(ft²·day	·))					
33. Atmospheric Pressure (psia)							
V. LIQUID INFORMATION	(optional i	f providir	ng T	ANKS Summary Shee	ts)		
34. Average daily temperature range of bulk lic	quid:	T					
34A. Minimum (°F) 100F		34B.	Ma	ximum (°F) 120F estim	nated		
35. Average operating pressure range of tank:							
35A. Minimum (psig) -1 psig slight vacuus	m est	35B.	Ма	ximum (psig) 2 psig	estimated		
36A. Minimum Liquid Surface Temperature	(°F)	36B.		rresponding Vapor Pre	ssure (psia)		
60F Est	0-1			2 psia est			
37A. Average Liquid Surface Temperature (	°F)	37B.		rresponding Vapor Pres	ssure (psia)		
38A. Maximum Liquid Surface Temperature	100F est 1.43 psia est  38A. Maximum Liquid Surface Temperature (°F) 38B. Corresponding Vapor Pressure (psia)						
100F est 1.43 psia est							
39. Provide the following for each liquid or gas	to be store	ed in tanl	κ. <i>Α</i>	Add additional pages if	necessary.		
39A. Material Name or Composition	P	PO		Plastics Pyrolysis Oil			
39B. CAS Number	UN-No	o (DOT)		3295	Hydrocarbons, liq		
39C. Liquid Density (lb/gal)	6.7	lb/gal					
39D. Liquid Molecular Weight (lb/lb-mole)	150	to 200		estimated			
39E. Vapor Molecular Weight (lb/lb-mole)	50 to	o 100		estimated	-		

Maximum Vapor Press	sure								
39F. True (psia)		-	at 100F est						
39G. Reid (psia)		2.15	osia est						
Months Storage per Young 39H. From	eai	Jan to Dec	entire year						
39I. To			ontine year						
0011	VI. EMISSIONS A	ND CONTR	OL DEVICE	DATA (required)	<u> </u>				
VI. EMISSIONS AND CONTROL DEVICE DATA (required)  40. Emission Control Devices (check as many as apply):   Does Not Apply									
☐ Carbon Adsorption¹									
☐ Condenser¹									
☐ Conservation Vent (psig)									
Vacuum S			Pressure Se	ettina					
	lief Valve (psig)			3					
☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐ ☐									
☐ Insulation of Ta									
Liquid Absorpti									
☐ Refrigeration o									
☐ Rupture Disc (									
☐ Vent to Incinera									
☐ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○ ○	e): Vent vapors to flar	·e							
· ·	oriate Air Pollution Cont		Sheet.						
	n Rate (submit Test Dat			or elsewhere in the apr	olication).				
	·	Workin	1	Annual Loss					
Material Name & CAS No.	Breathing Loss (lb/hr)	Amount	Units	Annual Loss (lb/yr)	Estimation Method <sup>1</sup>				
G 1	, ,	7	• • • • • • • • • • • • • • • • • • •						
See above									
Throughput Data, O =	ion Factor, MB = Ma Other (specify) ch emissions calculation								

## Attachment L EMISSIONS UNIT DATA SHEET CHEMICAL PROCESS

For chemical processes please fill out this sheet and all supplementary forms (see below) that apply. Please check all supplementary forms that have been completed.								
□ Emergency Vent Summary Sheet □ Leak Sources Data Sheet □ Toxicology Data Sheet □ Reactor Data Sheet □ Distillation Column Data Sheet								
Chemical process area name and	equipment ID number (as shown in Eq	quipment List Form)						
PYROLYSIS SYSTEM								
2. Standard Industrial Classification (	Codes (SICs) for process(es)							
1311								
<ol> <li>List raw materials and ☐ attach M PLASTIC WASTE</li> </ol>	4SDSs							
LACTIO WASTE								
4. List Products and Maximum Produ	<u> </u>	l						
Description and CAS Number	Maximum Hourly (lb/hr)	Maximum Annual (ton/year)						
ONE TON/HR. PLASTIC PYRO	2200	8000						
ONE TON/HR. PLASTIC PYRO	2200	8000						
· · · · · · · · · · · · · · · · · · ·	ummary Sheet for all emergency relief of							
6. Complete the Leak Source Data Sheet and describe below or attach to application the leak detection or maintenance program to minimize fugitive emissions. Include detection instruments, calibration gases or methods, planned inspection frequency, and record-keeping, and similar pertinent information. If subject to a rule requirement (e.g. 40CFR60, Subpart VV), please list those here. SYSTEM OPERATED AT -2 TO -4 INCHES OF WATER PRESSURE. ALL EMERGENCY RELIEFS SHALL BE SENT TO AN ENCLOSED AND EMISSION CONTROLLED FLARE SYSTEM.								
spill or release. FLOOR SPILLS SHALL BE DRIED	o application Accident Procedures to be D USING SAW DUST FIRST AND <sup>T</sup> BE SAVED FRO PROPER SEPAR	THEN WASHED WITH PROPER						

8A. Complete the Toxicology Data Sheet or attach to application a toxicology report (an up-to-date material safety data sheets (MSDS) may be used) outlining the currently known acute and chronic health effects of each compound or chemical entity emitted to the air. If these compounds have already been listed in Item 3, then a duplicate MSDS sheet is not required. Include data such as the OSHA time weighted average (TWA) or mutagenicity, teratogenicity, irritation, and other known or suspected effects should be addressed. Indicate where these are unknown, and provide references. 8B. Describe any health effects testing or epidemiological studies on these compounds that are being or may be conducted by the company or required under TSCA, RCRA or other federal regulations. Discuss the persistence in the environment of any emission (e.g. pesticides, etc.). Waste Products - Waste products status: (If source is subject to RCRA or 45CSR25, please contact the Hazardous Waste Section of WVDEP, OAQ at (304) 926-3647.) 9A. Types and amounts of wastes to be disposed: NONE 9B. Method of disposal and location of waste disposal facilities: Carrier: 9C. Check here if approved USEPA/State Hazardous Waste Landfill will be used 10. Maximum and Projected Typical Operating Schedule for process or project as a whole (circle appropriate units). (days), (batches/day), (batches/week) circle units: (hrs/day) (hr/batch) (days/yr), (weeks/year) 330 DAYS PERYEAR 10A. Maximum 24 HRS/DAY 330 DAYS PER YEAR 10B. Typical 24 HOURS/DAY 11. Complete a Reactor Data Sheet for each reactor in this chemical process. 12. Complete a Distillation Column Data Sheet for each distillation column in this chemical process. 13. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits. MONITORING OPERATION SHALL BE RECORDKEEPING RECORDED 24/7 AND DATA DATA SHALL BE STORED AND DUPLICATED. SHALL BE STORED. REPORTING TESTING SHALL BE REPORTED WEEKLY. SHALL BE PERFORMED DAILY. **MONITORING.** Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment operation or air pollution control device. **RECORDKEEPING.** Please describe the proposed recordkeeping that will accompany the monitoring. REPORTING. Please describe the proposed frequency of reporting of the recordkeeping. **TESTING.** Please describe any proposed emissions testing for this process equipment or air pollution control device. 14. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty EMISSION TESTS SHALL BE PERFORMED ON BURNERS USING STACK ANALYZER FOR CO, NOX, CO2, O2, N2 EMISSIONS WEEKLY.

#### INFORMATION REQUIRED FOR CHEMICAL PROCESSES

The notes listed below for chemical processes are intended to help the applicant submit a complete application to the OAQ; these notes are not intended to be all inclusive. The requirements for a complete application for a permit issued under 45CSR13 are designed to provided enough information for a permit reviewer to begin a technical review. Additional information beyond that identified may be required to complete the technical review of any individual application.

#### **Process Description**

Please keep these points in mind when completing your process description as part of this permit application.

- 1. Provide a general process overview. This brief, but complete, process description should include chemical or registered trademark names of chemical products, intermediates, and/or raw materials to be produced or consumed, and the ultimate use(s) of the product(s). A list of the various chemical compounds is helpful.
- 2. Describe <u>each process step</u>. Include the process chemistry and stoichiometrically balanced reaction equation or material mass balance on all components.
- 3. Describe the methods and equipment used to receive, store, handle, and charge raw materials.
- 4. Describe the methods and equipment used to handle, store, or package final products and intermediates.
- 5. Provide process flow diagrams or equipment layout drawings which clearly show the process flow relationships among all pieces of process and control equipment. Identify all air emission discharge points. Discuss instrumentation and controls for the process.
- 6. Discuss the possibilities of process upsets, the duration and frequency of upsets, and consequences (including air emissions) of these upsets. Include a description of rupture discs, pressure relief valves, and secondary containment systems.
- 7. Discuss any fugitive emissions and the methods used to minimize them.
- 8. Include the following plans for the process if available:
  - a. preventative maintenance and malfunction abatement plan (recommended for all control equipment).
  - b. continuous emissions (in-stack) monitoring plan
  - c. ambient monitoring plan
  - d. emergency response plan

#### **Regulatory Discussion**

The following state and federal air pollution control regulations may be applicable to your chemical process. You should review these regulations carefully to determine if they apply to your process. Please summarize the results of your review in your permit application along with any other regulations you believe are applicable.

- Title 45 Legislative Rule Division of Environmental Protection, Office of Air Quality contains West Virginia's air pollution control regulations, including the following promulgated rules which may require emissions reductions or control technologies for your chemical process:
  - a. 45CSR27 Best Available Technology (BAT) for Toxic Air Pollutants (TAPs)
  - b. 45CSR21 VOC emissions controls for ozone maintenance in Kanawha, Cabell, Putnam, Wayne, and Wood counties.
  - c. 45CSR13 (Table 45-13A) plantwide emission thresholds for permitting for certain pollutants.
- Federal Guidelines for case-by-case MACT determinations under section 112(g) of the 1990 CAAA for individual and total HAPs greater than 10 and 25 tons per year, respectively.
- There are also subparts of the federal Standards of Performance for New Stationary Sources (NSPS), 40CFR60 60, and the National Emission Standards for Hazardous Air Pollutants (NESHAP) at 40CFR61 and 40CFR63, which apply to various chemical and nonchemical processes. These subparts are too numerous to list here, but these areas of the federal regulations should be consulted carefully to determine applicability to your process.

#### **Emissions Summary and Calculations**

Please keep these points in mind when submitting your emissions calculations as part of this permit application.

- 1. For each pollutant, provide the basis for the emissions estimate and for all emission reduction(s) or control efficiency(ies) claimed.
- 2. For all batch processes provide the following
  - a. Emissions of each pollutant in pound(s) per batch, from each process step
  - b. Annual emissions based on number of batches requested per year
  - c. The total time for each process step and the duration of the emissions during the process step
  - d. Total batch time, total emissions per batch (or per day), and annual emissions based on the number of batches requested per year.

## **EMERGENCY VENT SUMMARY SHEET**

List below all emergency relief devices, rupture disks, safety relief valves, and similar openings that will vent only under abnormal conditions.

Emission Point ID <sup>1</sup>	Equipment to Relief Vent (type, ID if available) <sup>2</sup>	Relief Vents (type) & Set Pressure (psig)	Name of Chemical(s) or Pollutants Controlled	Worst Case Emission per Release Event (lbs)
Detailed design is in progr	ess, this sheet will be update	d as the designs are complet	ed.	
				-
				-
N/A				

All routine vents (non-emergency) should be listed on the Emission Points Data Summary Sheet.

<sup>&</sup>lt;sup>1</sup> Indicate the emission point, if any, to which source equipment normally vents. Do <u>not</u> assign emission point ID numbers to each emergency relief vent or device.

<sup>2</sup> List all emergency relief devices next to the piece of equipment from which they control releases.

## **LEAK SOURCE DATA SHEET**

Source Category	Pollutant	Number of Source Components <sup>1</sup>	Number of Components Monitored by Frequency <sup>2</sup>	Average Time to Repair (days) <sup>3</sup>	Estimated Annual Emission Rate (lb/yr) <sup>4</sup>
Pumps <sup>5</sup>	light liquid VOC <sup>6,7</sup>	Detailed design is in prog	ress, this sheet will be updated as the c	esigns are completed.	
	heavy liquid VOC <sup>8</sup>				
	Non-VOC <sup>9</sup>				
Valves <sup>10</sup>	Gas VOC				
	Light Liquid VOC				
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves <sup>11</sup>	Gas VOC				
	Non VOC				
Open-ended Lines <sup>12</sup>	VOC				
	Non-VOC				
Sampling Connections <sup>13</sup>	VOC				
	Non-VOC				
Compressors	VOC				
	Non-VOC				
Flanges	VOC				
	Non-VOC				
Other	VOC				
	Non-VOC				

<sup>&</sup>lt;sup>1-13</sup> See notes on the following page.

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## **Notes for Leak Source Data Sheet**

- 1. For VOC sources include components on streams and equipment that contain greater than 10% w/w VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.
- 2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in ppm. Do not include monitoring by visual or soap-bubble leak detection methods. "M/Q(M)/Q/SA/A/O" means the time period between inspections as follows:

Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/Other (specify time period)

If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category "valves, gas service:" 0/50/0/75/0/50 (bimonthly).

- 3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.
- 4. Note the method used: MB material balance; EE engineering estimate; EPA emission factors established by EPA (cite document used); O other method, such as in-house emission factor (specify).
- 5. Do not include in the equipment count sealless pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)
- 6. Volatile organic compounds (VOC) means the term as defined in 40 CFR 51.100 (s).
- 7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a light liquid.
- 8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a heavy liquid.
- 9. LIST CO, H<sub>2</sub>S, mineral acids, NO, NO<sub>2</sub>, SO<sub>3</sub>, etc. DO NOT LIST CO<sub>2</sub>, H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.
- 10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.
- 11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or if the valve vents to a control device.
- 12 Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.
- 13. Do not include closed-purge sampling connections.

## TOXICOLOGY DATA SHEET<sup>1</sup>

Descriptor Name/CAS	OSHA	Limits <sup>2</sup>	Acute <sup>3</sup> TC <sub>LO</sub> - Animal	Chronic⁴	Irritation⁵	References
Number	riptor Name/CAS Number  TWA  CL  TC <sub>LO</sub> - Animal LC <sub>LO</sub> - Animal LC <sub>50</sub> - Animal					

Indicate by "ND" where no data exists, in company's knowledge.
 Time Weighted Average, Ceiling Limit, or other, with units.
 If inhalation data is not available, provide other data as available.
 Relying on animal or human studies, indicate if any data suggests: C = carcinogenicity, M = mutagenicity, T = teratogenecity, O = oncogenicity.
 Indicate if there are dermal or eye irritation effects and whether they are considered to be low, moderate, or severe.

## **REACTOR DATA SHEET**

Provide the following information for  $\underline{each}$  piece of equipment that is a potential or actual source of emissions as shown on the  $\underline{Equipment\ List\ Form}$  and other parts of application.

Identifica	Identification Number (as shown on Equipment List Form):									
		of equipment	(e.g. CSTR, plug flow	w, batch, etc.	)					
2. Type	of operatio	n 🗌 Ba	atch [	✓ Continuous	S		Semi-batch	1		
3. Proje	ected Actual	Equipment C	)perating Schedule (	edule (complete appropriate lines):						
24 hrs/day 7 days/week 52 weeks/year										
	hrs/batch			es/day, weeks le one)	S		•	day,weeks/yr (Circle one)		
4. Feed	l Data	Flow In =	g	gal/hr, or gal/b	patch					
	al Name & S No.	Phase <sup>a</sup>	Specific Gravity	Vapor Pressure <sup>b</sup>	Cl Normal	narge Ra Max	ite Units	Fill Time (min/batch, run) <sup>c</sup>		
PLAST	IC WASTE	S	0.32	0	2200 LBS/HF	ł.	2	N/A		
a. S = S	Solid, L = Li	quid, G = gas	or vapor	ļ	! !		I	1		
	ed condition		lling per batch or run	(ctart up) fo	ur tank or ve	accal tun	o oguinma	ant		
			ns that will be involv							
react	tions that ma	ay occur as we	ell as gases that may							
are e	exothermic	or endothermi	C.							

6.	Maximum Temperatu		7A. Maximum Pressure 7B. Max. Set Pressure for venting								
	o	С				mmH	łg			mmHg	
	٥	F				psig				psig	
8.	Output Data Flow	ī		gal/hr or gal/b	oatch						
Material Name and CAS Phase Specific					Vapor		Hour	-	ch Output		
	No.		Gravit	ly P	ressure	Normal		Maxi	mum	Uni	ts
9.	Complete the following	na omice	rion data	for or	nuinmont	connected to	a hoa	dor oybo	uet evete	om giving o	missions
9.	levels before entering							uei exile	iusi sysic	iii, giviiig e	11115510115
	☐ Check here if not a	applicab	le								
Em	ission Point ID (exhau	st point	of heade	er syste	em):			ı			
Ma	terial Name and CAS	No.		Maxir	num Pot	ential Emissio	n Rate	(lb/hr)		Method **	
**	MB - material balance:	EE - En	gineering	g Estin	nate: TM	- Test Measur	rement	(submit	test data	): O - other	(Explain)

10.	addition	the following information pertaining to each condenser that may be attached to this reactor. Attach hal pages as necessary if more than one condenser is used for this reactor. Complete the Condenser Air n Control Device Sheet if necessary.									
	☐ Che	ck here if not applicable									
	10A.	Cooling material									
	10B.	Minimum and Maximum flowrate	te of cooling material (gal	//hr)							
	10C.	Inlet temperature of cooling ma	terial (°F)								
	10D.	Outlet temperature of cooling material (°F)									
	10E.	Pressure drop of gas to be con	densed from inlet to outle	et (psig)							
	10F.	Inlet temperature of gas stream	ı (°F)								
	10G.	Outlet temperature of gas stream	ım (°F)								
	10H.	Number of passes									
	10I.	Cooling surface area									
11.	Provide	the following pertaining to auxil	iary equipment that burns	s fuel (heaters, dryers, etc.):							
	☐ Che	ck here if not applicable									
	11A.	Type of fuel and maximum fuel	hurn rate ner hour:								
	1177.	Type of fact and maximum fact	barriate, per riour.								
	11B.	Provide maximum percent sulfu	ır (S), ash content of fuel,	and the energy content using appropriate units:							
		%S	% Ash	BTU/lb, std. ft³/day, gal							
				(circle one)							
	11C.	Theoretical combustion air requ PSIA:	irement in SCFD per unit	of fuel (circle appropriate unit) @ 70°F and 14.7							
		SCFD/lb, S	SCFD, gal (circle one)								
	445										
	11D.	Percent excess air:	%								
	11E.	Type, amount, and BTU rating	of burners and all other fi	iring equipment that are planned to be used:							
	445	Tatal mandament design to 10	4.	406 DTIVIE							
	11F.	Total maximum design heat inp	out:	×10 <sup>6</sup> BTU/hr.							

12. Proposed Monitoring, Recordkeeping, Rep Please propose monitoring, recordkeeping, an operating parameters. Please propose testing limits.	porting, and Testing and reporting in order to demonstrate compliance with the proposed g in order to demonstrate compliance with the proposed emissions
MONITORING	RECORDKEEPING
REPORTING	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE NOTE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION OR
RECORDKEEPING. PLEASE DESCRIBE THE PROPE	OSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.
REPORTING. PLEASE DESCRIBE THE PROPOSED FI	REQUENCY OF REPORTING OF THE RECORDKEEPING.
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EM CONTROL DEVICE.	ISSIONS TESTING FOR THIS PROCESS EQUIPMENT OR AIR POLLUTION
13. Describe all operating ranges and maintenan	ce procedures required by Manufacturer to maintain warranty

NOTE: An *AIR POLLUTION CONTROL DEVICE SHEET* must be completed for any air pollution device(s) (except emergency relief devices) used to control emissions from this reactor.

## **DISTILLATION COLUMN DATA SHEET**

lde	ntification Number (as assigned on E	quipment List Form):	
1.	Name and type of equipment		
#.	Projected actual equipment operatin	g schedule (complete appropriate lines):	
	hrs/day	days/week	weeks/year
	hrs/batch	batches/day, batches/week (circle one)	days/yr, weeks/yr (circle one)
2.	Number of stages (plates), excluding	g condenser	
3.	Number of feed plates and stage loc	ation	
4.	Specify details of any reheating, recy	ycling, or stage conditioning along with the stage lo	ocations
5.	Specify reflux ratio, R (where R is def R=L/D, where L = liquid down colum	fined as the ratio of the reflux to the overhead produnn, D = distillation product)	ıct, given symbolically as
6.	Specify the fraction of feed which is v continuously as vapor).	raporized, f (where f is the molal fraction of the feed t	hat leaves the feed plate
	Type of condenser used:	I ☐ partial ☐ multiple soperating details including all inlet and outlet temper	☐ other eratures, pressures, and
8. 9.	Feed Characteristics A. Molar composition B. Individual vapor pressure of eac C. Total feed stage pressure D. Total feed stage temperature E. Total mass flow rate of each stree Overhead Product		
	<ul><li>A. Molar composition of component</li><li>B. Vapor pressure of components</li></ul>	ns leaving the system as overhead products	
10.	Bottom Product  A. Molar composition of all componers  B. Total mass flow rate of all steam	nents	

General Information     A. Distillation column diameter	
B. Distillation column height	
C. Type of plates     D. Plate spacing	
E. Murphree plate efficiency	
F. Any other information necessary of describe the	operation of this distillation column.
	and Testing ting in order to demonstrate compliance with the proposed er to demonstrate compliance with the proposed emissions
MONITORING	RECORDKEEPING
REPORTING	TESTING
	SS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE HTHE OPERATION OF THIS PROCESS EQUIPMENT OPERATION OR
RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED REC	CORDKEEPING THAT WILL ACCOMPANY THE MONITORING.
REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY	CY OF REPORTING OF THE RECORDKEEPING.
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMISSIONS CONTROL DEVICE.	TESTING FOR THIS PROCESS EQUIPMENT OR AIR POLLUTION
13. Describe all operating ranges and maintenance proce	edures required by Manufacturer to maintain warranty

NOTE: An AIR POLLUTION CONTROL DEVICE SHEET must be completed for any air pollution device(s) (except emergency relief devices) used to control emissions from this distillation column.

## Attachment L Emission Unit Data Sheet

(INDIRECT HEAT EXCHANGER)

Control Device ID No. (must match List Form): 1S and 2S, 1C and 2C

## **Equipment Information**

1. Manufacturer: ARTI	Model No. Pyrolysis Heater     Serial No. 1 and 2						
3. Number of units: 2	Use - Heat Industrial Plastics to pyrolysis gas, pyrolysis oil and char residue						
5. Rated Boiler Horsepower: N/A hp	6. Boiler Serial No.: N/A						
7. Date constructed: Q3 2025	8. Date of last modification and explain: New						
9. Maximum design heat input per unit:	10. Peak heat input per unit:						
2.6 ×10 <sup>6</sup> BTU/hr	3.5 ×10 <sup>6</sup> BTU/hr						
11. Steam produced at maximum design output:  0 N/A LB/hr psig  13. Type of firing equipment to be used:	12. Projected Operating Schedule:  Hours/Day 24  Days/Week 7  Weeks/Year 48  14. Proposed type of burners and orientation:  Vertical  Front Wall  Opposed  Tangential  Others, specify EFGR External Flue Gas  16. Percent of ash retained in furnace: 0 %						
17. Will flyash be reinjected? ☐ Yes ☐ No	18. Percent of carbon in flyash: %						
Stack or	Vent Data						
19. Inside diameter or dimensions: 14 inches ft.	20. Gas exit temperature: 460 °F						
21. Height: 35 ft.	22. Stack serves:  ☑ This equipment only						
<ul> <li>23. Gas flow rate: 699 / stack (2 stacks) ft³/min</li> <li>24. Estimated percent of moisture: 15 to 30% on Pyro</li> </ul>	<ul> <li>Other equipment also (submit type and rating of all other equipment exhausted through this stack or vent)</li> </ul>						
gas %							

## **Fuel Requirements**

25.	Туре	Fuel Oil No.	Natural Gas	Gas (other, specify)	Coal, Type:	Other:			
	Quantity (at Design Output)	gph@60°F	ft³/hr	3125/unit ft³/hr	TPH				
	Annually	×10³ gal ×10⁶ ft³/hr		50 ×10 <sup>6</sup> ft <sup>3</sup> /hr	tons				
	Sulfur	Maximum: wt. % Average: wt. %	gr/100 ft <sup>3</sup>	0 gr/100 ft <sup>3</sup>	Maximum: wt. %				
	Ash (%)			0	Maximum				
	BTU Content	ent  BTU/Gal.  BTU/ft³  Lbs/Gal.@60°F		1041 BTU/ft <sup>3</sup> BTU/lb					
	Source	2.00, 00(0,00 :		Pyrolysis Process					
	Supplier			self produced					
	Halogens (Yes/No)			nil					
	List and Identify Metals			nil					
26.	Gas burner mode o		omatic hi-low	?7. Gas burner man	ufacture: ARTI				
	Automatic full n			≀8. Oil burner manu	facture:				
29.	If fuel oil is used, h	ow is it atomized?	☐ Oil Pressur ☐ Compresse ☐ Other, spec	ed Air 🔲 Rotary Cu					
30.	Fuel oil preheated:	Yes [	☐ No 3	31. If yes, indicate to	emperature:	°F			
		feet (ACF) per uni	t of fuel:	r combustion of the		f fuels described			
	30253scfh /unit@ 55 °F, atm PSIA, 40 % moisture  33. Emission rate at rated capacity: 0.245/unit lb/hr								
34.	Percent excess air	actually required f	or combustion of t	he fuel described:	15 assumed %				
			Coal Charac	cteristics					
35.	Seams: N/A								
36.	Proximate analysis	% of	Fixed Carbon: N/ Moisture: Ash:		6 of Sulfur: 6 of Volatile Matter:				

#### **Emissions Stream**

Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО	0.12	0.020	460	atm
Hydrocarbons				
NOx	0.12	0.020	460	atm
Pb				
PM <sub>10</sub>	0.01	0.002	460	atm
SO <sub>2</sub>				
VOCs	0	0	460	atm
Other (specify)				
What quantities of pollo	utants will be emitted from t	he boiler after contro	ols?	
What quantities of pollu	utants will be emitted from t  Pounds per Hour Ib/hr	he boiler after contro	ols? @°F	PSIA
	Pounds per Hour	ĺ		PSIA atm
Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	
<b>Pollutant</b>	Pounds per Hour lb/hr	grain/ACF	@ °F	
Pollutant CO Hydrocarbons	Pounds per Hour Ib/hr 0.12	grain/ACF	<b>@ °F</b> 460	atm
Pollutant  CO  Hydrocarbons  NO <sub>x</sub>	Pounds per Hour Ib/hr 0.12	grain/ACF	<b>@ °F</b> 460	atm
Pollutant CO Hydrocarbons NO <sub>x</sub> Pb	Pounds per Hour Ib/hr  0.12  0.12	9rain/ACF 0.020 0.020	@ °F 460	atm
Pollutant  CO Hydrocarbons NO <sub>x</sub> Pb PM <sub>10</sub>	Pounds per Hour Ib/hr  0.12  0.12	9rain/ACF 0.020 0.020	@ °F 460	atm

39. How will waste material from the process and control equipment be disposed of?

Any waste produced will be analyzed and placed in the proper disposal location.

- 40. Have you completed an Air Pollution Control Device Sheet(s) for the control(s) used on this Emission Unit. y
- 41. Have you included the air pollution rates on the Emissions Points Data Summary Sheet? partial

#### 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

**MONITORING PLAN:** Please list (1) describe the process parameters and how they were chosen (2) the ranges and how they were established for monitoring to demonstrate compliance with the operation of this process equipment operation or air pollution control device.

Pyrolysis Unit 1 and 2 - Natural Gas or Pyrolysis Gas Fired Low NOx Burners

#### 1. Emissions Monitoring

Continuous Emissions Monitoring Systems (CEMS): Fired heater management controls will be installed. Operations will continuously monitor fired heater performance with analyzers monitoring excess CO, O2, combustibles and firebox draft. Stack Testing/Performance Tests: On initial startup and annually, emissions testing will be completed to demonstrate compliance with emission limits for CO, NOx, SO2, CO2, VOC and particulates.

**TESTING PLAN:** Please describe any proposed emissions testing for this process equipment or air pollution control device.

Operations will monitor pyrolysis gas for sulfur, Cl, and CO content daily using gas detection tubes or other methods. Operations will log these readings in operating logs and note trends. Annually the data will be summarized and included in the report to site management.

Pyrolysis Furnace Stack -monitor for particulates, NOx, CO and VOC

Pyrolysis Gas - monitor for the following S, Cl and CO.

**RECORDKEEPING:** Please describe the proposed recordkeeping that will accompany the monitoring. Emissions Records: Clean Seas will maintain records of testing daily and annual testing data, including CEMS data, stack test results, and calculations based on emission factors.

Operating Parameters: Records of daily operational parameters and trends, such as fuel usage, operating hours, and equipment settings will be maintained.

Maintenance Records: Records of maintenance and repairs performed on the burners and associated control equipment will be kept.

Compliance Records: Documentation of plant performance with respect to permitted limits and applicable regulations will be maintained at the plant site offices.

## **REPORTING:** Please describe the proposed frequency of reporting of the recordkeeping.

Annual Emissions Inventory: A record of the annual emissions inventory will be reported to the WVDEP, detailing the monitoring of regulated pollutants emitted by the facility. This will include Malfunction and Upset Reports that resulted in emissions exceeding permit limits. Compliance Reports: Clean Seas will submit periodic compliance reports as specified in the permit discussing how the facility performed with respect to permitted limits.

43.	Describe	all ope	rating r	ranges	and ma	ıntenanc	e proce	dures re	equired	by Man	utacture	to mainta	ıın wa	rranty.

## Attachment L Emission Unit Data Sheet

(INDIRECT HEAT EXCHANGER)

Control Device ID No. (must match List Form): 8S and 8C

## **Equipment Information**

1. Manufacturer: ARTI -	2. Model No. TRE Pyrolysis Heater		
	Serial No. TRE=Training, Research and Evaluation		
3. Number of units: ONE (1)	4. Use - Trial Unit - Heat Industrial Plastics to pyrolysis gas, pyrolysis oil and char residue		
5. Rated Boiler Horsepower: N/A hp	6. Boiler Serial No.: N/A		
7. Date constructed: Undetermined, being rebuilt 3Q 2025	8. Date of last modification and explain: moved from ARTI shop in California to Belle WV for Training of operators, Research and Evaluation.		
9. Maximum design heat input per unit:	10. Peak heat input per unit:		
0.200 ×10 <sup>6</sup> BTU/hr	0.230 ×10 <sup>6</sup> BTU/hr		
11. Steam produced at maximum design output:  0 N/A LB/hr psig  13. Type of firing equipment to be used:	12. Projected Operating Schedule:  Hours/Day 4-6  Days/Week 5  Weeks/Year approximately 50  14. Proposed type of burners and orientation:  Vertical  Front Wall  Opposed  Tangential  Others, specify EFGR External Flue Gas  16. Percent of ash retained in furnace: 0 %		
17. Will flyash be reinjected? ☐ Yes ☐ No	18. Percent of carbon in flyash: %		
Stack or '	Vent Data		
19. Inside diameter or dimensions: 14 inches ft.	20. Gas exit temperature: 460 °F		
21. Height: 35 ft.	22. Stack serves:  ☑ This equipment only		
23. Gas flow rate: 699 / stack (2 stacks) ft³/min	<ul> <li>Other equipment also (submit type and rating of all other equipment exhausted through this</li> </ul>		
24. Estimated percent of moisture: 15 to 30% on Pyro	stack or vent)		

## **Fuel Requirements**

25.	Туре	Fuel Oil No.	Natural Gas	Gas (other, specify)	Coal, Type:	Other:	
	Quantity (at Design Output)	gph@60°F	ft³/hr	80 ft³/hr	TPH		
	Annually	×10³ gal	×10 <sup>6</sup> ft <sup>3</sup> /hr	0.08 ×10 <sup>6</sup> ft <sup>3</sup> /hr	tons		
	Sulfur	Maximum: wt. % Average: wt. %	gr/100 ft <sup>3</sup>	0.0097 gr/100 ft <sup>3</sup>	Maximum: wt. %		
	Ash (%)			0	Maximum		
	BTU Content	BTU/Gal. Lbs/Gal.@60°F	BTU/ft³	2516 BTU/ft <sup>3</sup>	BTU/lb		
	Source	2.50, 00(0,00 :		Propane			
	Supplier			TBD			
	Halogens (Yes/No)			nil			
	List and Identify Metals			nil			
26.	Gas burner mode o		omatic hi-low	27. Gas burner mar	nufacture: ARTI		
	Automatic full n			28. Oil burner manu	ıfacture:		
29.	29. If fuel oil is used, how is it atomized?  Oil Pressure  Steam Pressure  Rotary Cup  Other, specify						
30.	Fuel oil preheated:	Yes [	☐ No (	31. If yes, indicate t	emperature:	°F	
	32. Specify the calculated theoretical air requirements for combustion of the fuel or mixture of fuels described above actual cubic feet (ACF) per unit of fuel:						
	30253scfh /unit@ 55 °F, atm PSIA, 40 % moisture  33. Emission rate at rated capacity: 0.245/unit lb/hr						
34.	Percent excess air	actually required f	or combustion of t	the fuel described:	15 assumed %		
			Coal Chara	cteristics			
35.	Seams: N/A						
36.	36. Proximate analysis (dry basis): % of Fixed Carbon: N/A % of Sulfur: % of Moisture: % of Volatile Matter: % of Ash:						

#### **Emissions Stream**

Pollutant Pounds per Hour Ib/hr grain/ACF @ °F								
СО	0.032	0.077	460	atm				
Hydrocarbons								
NOx	0.008	0.019	460	atm				
Pb								
PM <sub>10</sub>	0.001	0.002	460	atm				
SO <sub>2</sub>	0.00008	0.0002	460	atm				
VOCs	0.001	0.002	460	atm				
Other (specify)								

38. What quantities of pollutants will be emitted from the boiler after controls?

Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО	0.032	0.077	460	atm
Hydrocarbons				
NO <sub>x</sub>	0.006	0.014	460	atm
Pb				
PM <sub>10</sub>	0.001	0.002	460	atm
SO <sub>2</sub>	0.000080	0.0002	460	atm
VOCs	0.001	0.001	460	atm
Other (specify)				

39. How will waste material from the process and control equipment be disposed of?

Any waste produced will be analyzed and placed in the proper disposal location.

- 40. Have you completed an Air Pollution Control Device Sheet(s) for the control(s) used on this Emission Unit. y
- 41. Have you included the air pollution rates on the Emissions Points Data Summary Sheet? partial

#### 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

**MONITORING PLAN:** Please list (1) describe the process parameters and how they were chosen (2) the ranges and how they were established for monitoring to demonstrate compliance with the operation of this process equipment operation or air pollution control device.

Pyrolysis Unit 1 and 2 - Natural Gas or Pyrolysis Gas Fired Low NOx Burners

#### 1. Emissions Monitoring

Fired heater management controls will be installed. Operations will continuously monitor fired heater performance.

**TESTING PLAN:** Please describe any proposed emissions testing for this process equipment or air pollution control device.

Operations will monitor using gas detection tubes or other methods.

Operations will log these readings in operating logs and note trends.

Annually the data will be summarized and included in the report to site management.

**RECORDKEEPING:** Please describe the proposed recordkeeping that will accompany the monitoring.

Emissions Records: Clean Seas will maintain records of testing.

Operating Parameters: Records of daily operational parameters and trends, such as fuel usage, operating hours, and equipment settings will be maintained.

Maintenance Records: Records of maintenance and repairs performed on the burners and associated control equipment will be kept.

**REPORTING:** Please describe the proposed frequency of reporting of the recordkeeping.

Annual Emissions Inventory: A record of the annual emissions inventory will be reported to the WVDEP, detailing the amount of fuel fired in the TRE and operating hours per year.

43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.

## Attachment L Emission Unit Data Sheet

(INDIRECT HEAT EXCHANGER)

Control Device ID No. (must match List Form): 7 S

## **Equipment Information**

1. Manufacturer: Heatec (proposed)	2. Model No. HCI-3010-25G Serial No. N/A				
3. Number of units: One (1)	4. Use Glycol circulation heater for warming lines, tanks, process, etc.				
5. Rated Boiler Horsepower: N/A hp	6. Boiler Serial No.: N/A				
7. Date constructed: TBD	8. Date of last modification and explain:				
9. Maximum design heat input per unit:	10. Peak heat input per unit:				
2.5 ×10 <sup>6</sup> BTU/hr	2.5 ×10 <sup>6</sup> BTU/hr				
11. Steam produced at maximum design output:	12. Projected Operating Schedule:				
Zero (0) LB/hr	Hours/Day 24				
. ,	Days/Week 7				
psig	Weeks/Year 52				
13. Type of firing equipment to be used:  ☐ Pulverized coal ☐ Spreader stoker ☐ Oil burners ☐ Natural Gas Burner ☐ Others, specify - Pyrolysis Gas	14. Proposed type of burners and orientation:  ☐ Vertical ☐ Front Wall ☐ Opposed ☐ Tangential ☐ Others, specify				
15. Type of draft: ⊠ Forced ☐ Induced	16. Percent of ash retained in furnace: 0 %				
17. Will flyash be reinjected? ☐ Yes ☐ No	18. Percent of carbon in flyash: N/A %				
Stack or '	Vent Data				
19. Inside diameter or dimensions: 24 inches ft.	20. Gas exit temperature: 300 to 400 °F				
21. Height: Approx 15 ft over adjacent structures, 32 ft.	22. Stack serves:  ☑ This equipment only				
23. Gas flow rate: 492 @ 350F ft³/min	<ul> <li>Other equipment also (submit type and rating of all other equipment exhausted through this</li> </ul>				
24. Estimated percent of moisture: 10-15% NG, 15 to 30% Pyro Gas %	stack or vent)				

## **Fuel Requirements**

25.	Туре	Fuel Oil No.	Natural Gas	Gas (other, specify)	Coal, Type:	Other:
	Quantity (at Design Output)	gph@60°F	2500 ft <sup>3</sup> /hr	2500 ft³/hr	TPH	
	Annually	×10³ gal	22 ×10 <sup>6</sup> ft³/hr	21.9 ×10 <sup>6</sup> ft <sup>3</sup> /hr	tons	
	Sulfur	Maximum: wt. % Average: wt. %	4 gr/100 ft <sup>3</sup>	0 gr/100 ft <sup>3</sup>	Maximum: wt. %	
	Ash (%)				Maximum	
	BTU Content	BTU/Gal. Lbs/Gal.@60°F	1045 BTU/ft³	1011 BTU/ft <sup>3</sup>	BTU/lb	
	Source	<u> </u>	Dominion Energy	Self Produced Pyrolysis Gas		
	Supplier		Dominion/Hope Gas	Self		
	Halogens (Yes/No)		no	nil		
	List and Identify Metals		no	nil		
26.	Gas burner mode o ☐ Manual		omatic hi-low	27. Gas burner mar	nufacture: Heatec	
	Automatic full n			28. Oil burner manu		
29.	If fuel oil is used, h	now is it atomized?	☐ Oil Pressur ☐ Compresse ☐ Other, spec	ed Air 🔲 Rotary Cu		
30.	Fuel oil preheated:	: Yes [	☐ No 3	31. If yes, indicate to	emperature:	°F
	32. Specify the calculated theoretical air requirements for combustion of the fuel or mixture of fuels described above actual cubic feet (ACF) per unit of fuel:					
22	© Emission rate at ra	°F,	PSIA,	% mo	oisture	
	33. Emission rate at rated capacity: Ib/hr 34. Percent excess air actually required for combustion of the fuel described: %					
54.	r ercent excess all	actually required in	Coal Charac		%	
35.	Seams:					
36.	36. Proximate analysis (dry basis): % of Fixed Carbon: % of Sulfur: % of Moisture: % of Volatile Matter: % of Ash:					

## **Emissions Stream**

Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО	0.400	0.095	350	Atm
Hydrocarbons	nil			
NO <sub>x</sub>	0.100	0.024		
Pb	nil			
PM <sub>10</sub>	0.018	0.004		
SO <sub>2</sub>	0.00234	0.0006		
VOCs	.015	0.003		
Other (specify)	Natural Gas Fuel			
		492 ft3/min		
		29520 ft3/hr		
Note- These are estimated	Manufacturer data not	used in estimates		

Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО	0.400	0.095	350	Atm
Hydrocarbons	nil			
NO <sub>x</sub>	0.075	0.018		
Pb	nil			
PM <sub>10</sub>	0.018	0.004		
SO <sub>2</sub>	nil			
VOCs	0.015	0.003		
Other (specify)	Pyrolysis Gas Fuel			
Note;these are estimated	based on the pyro gas	and low NOx burner		
data will be updated with	manufacturer data	once purchased		

39. How will waste material from the process and control equipment be disposed of?

Any waste produced will be analyzed or assesed and properly disposed of.

- 40. Have you completed an Air Pollution Control Device Sheet(s) for the control(s) used on this Emission Unit. y
- 41. Have you included the air pollution rates on the Emissions Points Data Summary Sheet? partially

### 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

**MONITORING PLAN:** Please list (1) describe the process parameters and how they were chosen (2) the ranges and how they were established for monitoring to demonstrate compliance with the operation of this process equipment operation or air pollution control device.

Operator monitoring of heater performance. Initial performance testing to demonstrate compliance with permit emission limits. Annual stack testing or as required by permitting. Periodic monitoring as recommended by the manufacturer.

**TESTING PLAN:** Please describe any proposed emissions testing for this process equipment or air pollution control device.

Maintain records of operational hours, fuel usage (natural gas or pyrolysis gas) and maintenance activities. Records deviations from normal operations or emissions limits.

**RECORDKEEPING:** Please describe the proposed recordkeeping that will accompany the monitoring.

Document emissions data, including results from any required testing or monitoring. Maintain records of any exceedances of emission limits.

**REPORTING:** Please describe the proposed frequency of reporting of the recordkeeping.

Annual Emission Inventory and Compliance Report

Submit an annual emission inventory report to the WVDEP, detailing emissions from the glycol heater and other sources. Submit periodic compliance reports as specified in the operating permit, which may include results from emission testing and monitoring, excursions and incidents. Notify the WVDEP of any deviations from permit conditions or emissions limits, including any malfunctions or breakdowns.

43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.

This section will be completed when the equipment is purchased.

#### Attachment L Emission Unit Data Sheet

(INDIRECT HEAT EXCHANGER)

Control Device ID No. (must match List Form):

#### **Equipment Information**

1. Manufacturer: Howard Engineering	2. Model No.		
	Serial No.		
3. Number of units: 3 Engineering in progress	4. Use Cooling gases using water		
5. Rated Boiler Horsepower: N/A hp	6. Boiler Serial No.: Not a boiler, heat exchangers		
7. Date constructed:	8. Date of last modification and explain:		
9. Maximum design heat input per unit:	10. Peak heat input per unit:		
×10 <sup>6</sup> BTU/hr	×10 <sup>6</sup> BTU/hr		
11. Steam produced at maximum design output:	12. Projected Operating Schedule:		
LB/hr	Hours/Day		
	Days/Week		
psig	Weeks/Vear		
<ul> <li>13. Type of firing equipment to be used:  Pulverized coal  Spreader stoker  Oil burners  Natural Gas Burner  Others, specify</li> </ul>	<ul> <li>14. Proposed type of burners and orientation:</li> <li>Vertical</li> <li>Front Wall</li> <li>Opposed</li> <li>Tangential</li> <li>Others, specify</li> </ul>		
15. Type of draft: ☐ Forced ☐ Induced	16. Percent of ash retained in furnace: %		
17. Will flyash be reinjected? ☐ Yes ☐ No	18. Percent of carbon in flyash: %		
Stack or '	Vent Data		
19. Inside diameter or dimensions: ft.	20. Gas exit temperature: °F		
21. Height: ft.	22. Stack serves:  This equipment only		
23. Gas flow rate: ft <sup>3</sup> /min	<ul> <li>Other equipment also (submit type and rating of all other equipment exhausted through this</li> </ul>		
24. Estimated percent of moisture:	stack or vent)		

#### **Fuel Requirements**

25.	Type Fuel Oil No. Natural Gas		Gas (other, specify) Coal, Type: Other			
	Quantity (at Design Output)	gph@60°F	ft <sup>3</sup> /hr	ft <sup>3</sup> /hr	TPH	
	Annually	×10³ gal	×10 <sup>6</sup> ft <sup>3</sup> /hr	×10 <sup>6</sup> ft <sup>3</sup> /hr	tons	
	Sulfur	Maximum: wt. % Average: wt. %	gr/100 ft <sup>3</sup>	gr/100 ft <sup>3</sup>	Maximum: wt. %	
	Ash (%)				Maximum	
	BTU Content	BTU/Gal. Lbs/Gal.@60°F	BTU/ft <sup>3</sup>		BTU/lb	
	Source	200/ Call. © 00 1				
	Supplier					
	Halogens (Yes/No)					
	List and Identify Metals					
26.	Gas burner mode o		omatic hi-low	27. Gas burner mar	nufacture:	
	Automatic full n			28. Oil burner manu	facture:	
29.	If fuel oil is used, h	ow is it atomized?	☐ Oil Pressur ☐ Compresse ☐ Other, spec	ed Air 🔲 Rotary Cu		
	Fuel oil preheated:			31. If yes, indicate to		°F
	above actual cubic	feet (ACF) per uni	t of fuel:	r combustion of the		of fuels described
33.		°F, ated capacity:	PSIA, lb/hr	% MC	oisture	
		actually required for		the fuel described:	%	
			Coal Charac			
35.	Seams:					
36. Proximate analysis (dry basis): % of Fixed Carbon: % of Sulfur: % of Moisture: % of Volatile Matter: % of Ash:						

#### **Emissions Stream**

Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО				
Hydrocarbons				
NO <sub>x</sub>				
Pb				
PM <sub>10</sub>				
SO <sub>2</sub>				
VOCs				
Other (specify)				
3. What quantities of poll	utants will be emitted from t	he boiler after contro	ls?	
Pollutant	Pounds per Hour lb/hr	grain/ACF	@ °F	PSIA
СО				
Hydrocarbons				
NO <sub>x</sub>				
Pb				
PM <sub>10</sub>				
SO <sub>2</sub>				
VOCs				
Other (specify)				
). How will waste materia	al from the process and con	trol equipment be dis	sposed of?	
	al from the process and con			Emission Unit.

42.	Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.
	<b>MONITORING PLAN:</b> Please list (1) describe the process parameters and how they were chosen (2) the ranges and how they were established for monitoring to demonstrate compliance with the operation of this process equipment operation or air pollution control device.
	<b>TESTING PLAN:</b> Please describe any proposed emissions testing for this process equipment or air pollution control device.
	<b>RECORDKEEPING:</b> Please describe the proposed recordkeeping that will accompany the monitoring.
	<b>REPORTING:</b> Please describe the proposed frequency of reporting of the recordkeeping.
43.	Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.

#### Attachment L **EMISSIONS UNIT DATA SHEET GENERAL**

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): 5 E 5 S

Tachtineation Namber (as assigned on Equipment List Form). 3 E 35
Name or type and model of proposed affected source:
Generac SG150 229 BHP, 150kWh, 2042 scfh NG @ full load
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
Natural Gas fueled 150 kW Generac electric generator for power supply during power outages to enable safe plant shutdown.  Fuel rate 2042 scfh Natural Gas at full rate.
4. Name(s) and maximum amount of proposed material(s) produced per hour:
150 kW Electricity Generator engine exhaust
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
Combustion of natural gas and air to electricity, CO2, H2O, NOx, CO, SO2, VOC, PM

The identification number which appears here must correspond to the air pollution control device identification number appearing on the List Form.

6.	. Combustion Data (if applicable):								
	(a) Type and amount in appropriate units of fuel(s) to be burned:								
	2042 scfh natural gas at full power for power supply backup approximately 14 hours per year. Minimal natural gas for a weekly test run every week for one (1) hour - 52 hours/yr.								
	(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percent sulfur and ash:								
N	Natuarl gas composed of Methane with Sulfur odorant concentration of appromately 4 ppm.								
	(c) Theoretical combustion	n air requirement (A	ACF/unit of fue	I):					
	14.5 ft3 air @	60	°F and	Atm	psia.				
	(d) Percent excess air:	15% estimated not from	n Generac data sh	eet					
	(e) Type and BTU/hr of bu	rners and all other	firing equipme	ent planned to b	e used:				
G	enerac Piston Engine powered ge								
	(f) If coal is proposed as a coal as it will be fired:	a source of fuel, ide	ntify supplier a	nd seams and	give sizing of the				
	(g) Proposed maximum de		2.0	142	× 10 <sup>6</sup> BTU/hr.				
7.	Projected operating sched	ule: 							
Но	ours/Day Days/Week 1 Weeks/Year 52								

8.	8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	1440	°F and		14.73	psia	
a.	NO <sub>X</sub>	0.894	lb/hr	0.079	grains/ACF	
b.	SO <sub>2</sub>	0.0023	lb/hr	0.0002	grains/ACF	
C.	СО	0.878	lb/hr	0.078	grains/ACF	
d.	PM <sub>10</sub>	nil	lb/hr	nil	grains/ACF	
e.	Hydrocarbons	0.252	lb/hr	0.023	grains/ACF	
f.	VOCs	included in e	lb/hr		grains/ACF	
g.	Pb	nil	lb/hr	nil	grains/ACF	
h.	Specify other(s)		I			
			lb/hr		grains/ACF	
			lb/hr		grains/ACF	
			lb/hr		grains/ACF	
			lb/hr		grains/ACF	

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

9. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

#### **MONITORING**

The site will record the annual hours of operation including non-emergency usage such as maintenance checks and testing. The site will test run the generator once per week for approximately and hour.

Natural Gas Fuel Usage: Record the quantity of natural gas consumed by the generator.

#### RECORDKEEPING

Operating Logs: Clean Seas will maintain records of the dates, times, and duration of all emergency and non-emergency operations.

Fuel Purchase Records: The site will keep records of natural gas purchases to document fuel consumption. Maintenance Records: Document all maintenance and repairs performed on the generator.

Manufacturer Specifications: Keep records of the generator's manufacturer's specifications and compliance demonstrations

#### REPORTING

Reporting

Annual Emission Reports: Submit reports detailing the generator's emissions of regulated air pollutants, often using the DEP's emissions inventory system or required forms.

Compliance Certifications and Deviation Reports: Submit periodic certifications of compliance with the permit conditions. Report any deviations from permit conditions or regulations, such as exceeding operational hour limits or emission limits.

#### **TESTING**

Emission Limits: The manufacturer has performed testing on the generator and has reported the emissions of nitrogen oxides (NOx), carbon monoxide (CO), CO2, PE, sulfur dioxide (SO2), and volatile organic compounds (VOCs) based on natural gas fuel.

Initial and period testing will be used to demonstrate compliance with these emission limits.

**MONITORING.** PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

**RECORDKEEPING.** PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

**REPORTING.** PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

**TESTING.** PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

#### Oil Spill Response Procedure

Clean Seas West Virginia

Oil spill response procedure for a plastics pyrolysis plant producing 3960000gal/yr oil heavier than diesel fuel. 8 21000 gal frac tanks, truck loading rack loading 2 to 3 trucks per day 5 days per week, located in west virginia near Belle, WV.

\*\*Immediate Spill Response Actions\*\*

- 1. \*\*Stop the Source: \*\* Shut off pumps, close valves, and isolate the leaking equipment.
- 2. \*\*Containment:\*\* Deploy booms and absorbent pads around the tank, rack, or transfer area to prevent migration.
- 3. \*\*Recovery:\*\* Use skimmers, vacuum trucks, or sorbent materials to remove free oil from paved surfaces or containment areas.
- 4. \*\*Secure Waste:\*\* Place recovered oil and oily materials into labeled, sealable containers for proper disposal.

\*\*Spill Prevention & Preparedness\*\*

Effective prevention minimizes the need for response.

#### Training & Drills

- Conduct quarterly drills simulating a 21,000-gal tank release.
- Train all operators in valve shutdown, emergency contact procedures, and use of spill kits.

#### **Equipment & Facilities**

- Maintain \*\*eight 21,000-gal\*\* frac tanks with secondary containment rated at \*\*110%\*\* of single-tank capacity.
- Install high-level alarms on each tank and truck loading rack.

- Keep spill kits (absorbents, neutralizers, booms) within \*\*100 ft\*\* of loading areas.
- Ensure all transfer hoses and fittings are inspected monthly and replaced every two years or upon signs of wear.

#### \*\*Notification & Reporting\*\*

#### **Internal Notifications**

- Immediately alert the Plant Shift Supervisor and EHS Manager.
- Activate the on-call response team and Chemtrec 1-800-424-9300 or local 1-703-527-3887 within \*\*15 minutes\*\* of spill discovery.

#### **External Notifications**

- If spill ≥ 25 gal reaches soil or waters of the state, notify West Virginia Department of Environmental Protection (DEP) Spill Hotline: \*\*(800) 642-3074\*\*.
- If spill threatens navigable waters, notify U.S. Coast Guard National Response Center: \*\*(800) 424-8802\*\*.
- Submit a written incident report to WV DEP within \*\*15 days\*\*.

#### \*\*Spill Response Plan Components\*\*

#### Site Map & Tank Inventory

- Clearly mark all frac tanks, transfer lines, loading racks, and nearby waterways (e.g., Belle vicinity drainage).

#### Resource List

- Contact information for cleanup contractors, waste disposal facilities, and equipment vendors.
- Inventory of on-site spill response gear, including:
- 500 ft of containment boom
- 1,000 sorbent pads

• 2 vacuum pumps (2,000 gal/hr capacity)

#### **Action Flowchart**

- 1. Detection & Alarm
- 2. Source Shutdown
- 3. Containment
- 4. Recovery & Cleanup
- 5. Waste Management
- 6. Incident Evaluation & Reporting
- \*\*Post-Spill Evaluation & Continuous Improvement\*\*
- Conduct root-cause analysis within \*\*7 days\*\* of spill resolution.
- Update standard operating procedures and retrain staff on identified gaps.
- Review and restock spill kits immediately after each event, ensuring readiness for the next incident.

## Attachment M Air Pollution Control Device Sheet

(CONDENSER SYSTEM)

Control Device ID No. (must match Emission Units Table):

#### **Equipment Information and Filter Characteristics**

Manufacturer:     Model No. Howard Engineering	2. Method: ☐ Pressure condensation ☐ Temperature condensation ☐ Surface		
3. Control Device Name: Condensor	☐ Contact ☐ Other, specify		
4. Provide diagram of condenser: Engineering in progre	ess		
<ol> <li>Provide diagram(s) of unit describing capture tayste capacity, horsepower of movers. If applicable at state</li> </ol>	em with duct arrangement and size of duct, air volume, hood face velocity and hood collection efficiency.		
6. Heat exchanger area: 393 ft^2 ft³	7. Reported removal efficiency: N/A %		
8. Coolant Used:	Refrigeration capacity: Ref. One tons		
50/50 water and glycol			
10. Composition of coolant:	11. Internal operating temperature: °F		
See above item 8	42F		
12. Specific heat of coolant:	13. Temperature of condensation: 55 °F		
0.75 BTU/lb.°F, at 77°F	13. Temperature of condensation, 95		
Average Operation:	Maximum Operation:		
14. Coolant Temperature:	15. Coolant Temperature:		
Inlet: 42 °F	Inlet: 42 °F		
Outlet: 52 °F	Outlet: 52 °F		
16. Gas Temperature:	17. Gas Temperature:		
Inlet: 85 °F	Inlet: 90 °F		
Outlet: 55 °F	Outlet: 60 °F		
18. Gas flow rate: 176 ft³/min	19. Gas flow rate: 200 ft³/min		
20. Coolant flow rate per condenser: Type:	21. Coolant flow rate per condenser:  Type:		
Water: 2.4 gal/min	Water: 2.4 gal/min		
Air: ft³/min	Air: ft³/min		
Other: lb/hour	Other: lb/hour		
22. Efficiency of condenser: 80 %	23. Efficiency of condenser: 80 %		
24. Condenser surface area: 393 ft²	25. Condenser surface area: 393 ft <sup>2</sup>		

26. Pollutant	Guaranteed Control Ef		Con	ppmv	Specific BTU/lb-m			of Vaporation BTU/lb-mol
A N/A								
В								
С								
D								
Е								
F								
G								
Total Concentration in ppm	١٧							
	En	nission Gas		The second secon				
27. Before Condenser			28.	After Cond	enser			
Inlet vapor flow rate: N//	A ft³/min			Inlet vapor	flow rate:		ft³/m	nin
Influent vapor temperature	: °F			Influent vap	or tempera	ture:		°F
Effluent vapor temperature	: °F			Effluent vap	or tempera	ture:		°F
29.		INLET		,		OUT	LET	
Pollutant	Vapor Pressure	Condensat Temperati		Rate lb/hr	Rate lb/hr	Vapo Pressu		Condensation Temperature
A N/A								
В								
С								
D								
E								
F								
G								
Total of the POLLUTANT II	b/hr							
30. Moisture content:	%							
31. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas reheating, gas humidification):								
32. Describe the collection material disposal system:  33. Have you included <i>Condenser Control Device</i> in the Emissions Points Data Summary Sheet?								

Please propose m	g parameters. Please propose	and Testing eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the RECORDKEEPING:
Routine mo	nitoring	
REPORTING:		TESTING:
ı		
MONITORING:		ocess parameters and ranges that are proposed to be
	equipment or air control device.	strate compliance with the operation of this process
RECORDKEEPING:		cordkeeping that will accompany the monitoring.
REPORTING:	pollution control device.	emissions testing for this process equipment on air
TESTING:		emissions testing for this process equipment on air
35. Manufacturer's Gua	aranteed Capture Efficiency for ea	ch air pollutant.
36. Manufacturer's Gua	aranteed Control Efficiency for each	h air pollutant.
07 D 3 H 6		
37. Describe all operati	ng ranges and maintenance proce	edures required by Manufacturer to maintain warranty.
1		

## Attachment M Air Pollution Control Device Sheet

(FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table):

#### **Equipment Information**

1.	Manufacturer: ARTI  Model No. ARTFB10	2. Method: ☐ Elevated flare ☐ Ground flare ☐ Other ☐ Describe
3.	Provide diagram(s) of unit describing capture systecapacity, horsepower of movers. If applicable, state	em with duct arrangement and size of duct, air volume, hood face velocity and hood collection efficiency.
4.	Method of system used:  ☐ Steam-assisted	☐ Pressure-assisted ☐ Non-assisted
5.	Maximum capacity of flare:	6. Dimensions of stack:
	350 scf/min 21000.00 scf/hr	Diameter 1.33 ft. Height 15.00 ft.
7.	Estimated combustion efficiency: (Waste gas destruction efficiency)  Estimated: 99.99 %  Minimum guaranteed: 99.9 %	8. Fuel used in burners:  Natural Gas Fuel Oil, Number Other, Specify: Pyro gas from plastic
9.	Number of burners: One	11. Describe method of controlling flame:
	Rating: 10,000,000.00 BTU/hr	
10.	Will preheat be used? ☐ Yes ☑ No	
12.	Flare height: Enclosed flare box ft	14. Natural gas flow rate to flare pilot flame per pilot light: 75 scf/min
13.	Flare tip inside diameter: 14 Inches ft	scf/hr
15.	Number of pilot lights: One	16. Will automatic re-ignition be used?
	Total 450,000.00 BTU/hr	☑ Yes ☐ No
17.	If automatic re-ignition will be used, describe the met	hod: Flow sensing system
	Other, Describe:	☐ No -Red era with monitoring control room
19.	Hours of unit operation per year:	

	Steam Injection					
20.	Will steam injection be used	d? 🗌 Yes	☑ No 2	21. Steam pressure Minimum Expected:	PSIG	
22.	Total Steam flow rate:		LB/hr 2	23. Temperature:	°F	
24.	Velocity	3	ft/sec 2	25. Number of jet streams		
26.	Diameter of steam jets:	1	in 2	27. Design basis for steam in	njected:	
28.	How will steam flow be cont	trolled if steam ini	ection is II	L Isod?	B steam/LB hydrocarbon	
	Tion will occurred by con-	Jones II Steam Ing.	ection is a	15eu :		
				Gas Stream to be Burned		
29.	Name	Quantity Grains of H <sub>2</sub> S		<b>Quantity</b> (LB/hr, ft <sup>3</sup> /hr, etc)	Source of Material	
	Pyro Gas	0		21,000.00 ft^3/hr.	Pyrolysis system	
	-					
	***					
30	Estimate total combustible t	to flaro: 750 to	4000 II	I R/hr	or ACF/hr	
50.	(Maximum mass flow rate o	700 10	o 1300 lb	os./hr. LB/nr	OF ACE/III	
31.	Estimated total flow rate to f	flare including ma	terials to b		kiliary fuel, etc.:	
	750 tp 1300 lbs./hr.	LB/hr or	ACF/hr			
32.	Give composition of carrier	gases: 30% hy	/drogen,	35% CH4 20%	CO 5%CxHy	
	5% Nitrogen 2% Ox	7	100	Consider Mode	5 5700ATTy	
33.	Temperature of emission str			34. Identify and describe all a	auxiliary fuels to be burned.	
	100	°F		See above analysis	BTU/scf	
	Heating value of emission s	2		occ above analysis	BTU/scf	
	1000 Mean molecular weight of e	BTU/ft <sup>3</sup> mission stream:			BTU/scf	
	MW = 28.5 lb/lb-mc				BTU/scf	
35.	Temperature of flare gas:	1800 °F	3	6. Flare gas flow rate: 35	0 scf/min	
37.	Flare gas heat content:	BTU/ft <sup>3</sup>	3	8. Flare gas exit velocity:	scf/min	
39.	Maximum rate during emerg	jency for one maj	or piece o	f equipment or process unit:	175 scf/min	
	Maximum rate during emerg					
41.	Describe any air pollution o	control device inle	et and out	tlet gas conditioning process	ses (e.g., gas cooling, gas	
	reheating, gas humidification	ARTI low er	mission I	burner. Below 50 PPM (	CO and below 80 PPM	
Ν	IOx emissions.					
42.	Describe the collection mate	erial disposal system	em: Eme	ergency flare is only used	about 24 times/yr for	
ma	aximum of 6 hours total f	for a SU/SD cyc		- The Control of the	Đ	
13	Have you included Flare Co	antrol Dovice in t	ho Emissi	one Deinte Dete Cummer C	haat0	

Please propose m	g parameters. Please propose	and Testing eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the
MONITORING	k analyzer data collection	RECORDKEEPING: Data recorder and strip
		printout with date and time.
REPORTING:		TESTING:
MONITORING:		l ocess parameters and ranges that are proposed to be strate compliance with the operation of this process
RECORDKEEPING: REPORTING:	Please describe the proposed re Please describe any proposed	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air
TESTING:	pollution control device.  Please describe any proposed pollution control device.	emissions testing for this process equipment on air
45. Manufacturer's Gua ARTI guarantees tha	aranteed Capture Efficiency for ea t the above mensioned emissio	ch air pollutant. ons at the worse operating condiction will be
performed by the flat	re burenr. Flare burner will be	fired in an insulated box and no flame will be
seen outside of the b	oox. Flame will be totally contain	ined within the box and the combustion will
completed as in a bo	piler.	
	aranteed Control Efficiency for eac below all emission levels mens	
		edures required by Manufacturer to maintain warranty. nsing system to keep proper air/fuel ratios
to keep clean com	bustion.	000 00 100 100 100 100 100 100 100 100

### Attachment I **Emissions Unit Table**

(includes all emission units and air pollution control device that will be part of this permit aplication review, regardles of permit status)

Emissions Unit ID	Emissions Point ID	Emissions Units Description	Year Installed / Modified	Design Capacity	Type and Date of Change	Control Device
<b>1</b> S	1E	Pyrolysis Unit #1	TBD	3 mmBTU/Hr	New	1C
2S	2E	Pyrolysis Unit #2	TBD	3 mmBTU/Hr	New	2C
3S	3E	Flare	TBD	1-5 mmBTU/Hr	New	3C
4S	4E	Frac Tanks (8 total)	TBD	21,000 gal/tk	New	4C
5S	5E	Generator Nat Gas Fuel	TBD	150 kWh	New	5C
6S	6E	Truck Loading Rack	TBD	15k gal/day	New	6C
7S	7E	Gycol Circulation Heater	TBD	2.5 mmBTU/Hr	New	7C
8S	8E	TRE- Training, Research & Eval	TBD	0.2mmBTU/Hr	New	8C
98	9E	TRE- Flare	TBD	0.1 mmBTU/Hr	New	9C

<sup>&</sup>lt;sup>1</sup> For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
<sup>2</sup> For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.

<sup>3</sup> New, modification, removal

<sup>&</sup>lt;sup>4</sup> For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

## Attachment J EMISSION POINTS DATA SUMMARY SHEET

							Table 1	Emissions D	ata 7	Test Data	provided	by ARTI			
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type <sup>1</sup>	Ver Throug Po (Must Emissi	ion Unit nted gh This pint match on Units Plot Plan)	Contro (Musi Emissi	ollution I Device match on Units Plot Plan)	Emissi (che	ime for on Unit mical ses only)	All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOCs & HAPS) ext here	Maxii Pote Uncon Emiss	ntial trolled	Po Cor	ximum tential htrolled ssions <sup>5</sup>	Emission Form or Phase (At exit conditions, Solid, Liquid or	Est. Method Used <sup>6</sup>	Emission Concentration <sup>7</sup> (ppmv or mg/m³)
		ID No.	Source	ID No.	Device Type	Short Term <sup>2</sup>	Max (hr/yr)	ext neve	lb/hr	ton/yr	lb/hr	ton/yr	Gas/Vapor)		
1E	UPWARD STACK	18	BURNER	10	ANALYZER	С	8,000	NOx CO PE VOC	.12 .12 .0015 0.0	0.872 0.872 0.010 0.000	0.12 0.12 0.005 0.000	0.872 0.872 0.010 0.000	GAS	ST	30 PPM 50 PPM 0.005LB/MMBTU 0.0 PPM
2E	UPWARD STACK	28	BURNER	2C	ANALYZER	С	8,000	NOx CO PE VOC	.12 .12 .0015 0.0	0.872 0.872 0.010 0.000	0.120 0.120 0.005 0.000	0.436 0.436 0.005 0.000	GAS	ST	30 PPM 50 PPM 0.005 LB/MMBTU 0.0 PPM
3E	UPWARD STACK	3S	BURNER	3C	ANALYZER	note A	144	NOX CO PE VOC	0.240 0.240 0.003 0.000	0.047 0.047 0.0 0.0	0.240 0.240 0.003 0.000	0.047 .013 0.00 0.00	GAS	ST	30 PPM 50 PPM 0 PPM 0 PPM
4E	Upward Vent to Flare	48	Press vac vent	4C	Process Monitoring	To Flare	N/A	VOCs	TBD	TBD	TBD	TBD	Vapor/N2 to flare	EE	TBD
5E	Upward Stack	5S	Natural gas engine	5C	Catalytic Converter	During Power Outage	70	NOx CO PE VOC	0.894 0.878 Nil 0.252	0.029 Nil	0.050 0.374 Nil 0.071	0.002 0.012 Nil 0.002	Gas	ST	TBD
6E	Vapor to Tank	6S	Vapor Line From Truck	6C	vapor contain- ment	During Truck Loading	1,500	VOCs	TBD	TBD	TBD	TBD	Gas	EE	TBD
7E	Upward Stack	7S	Burner	7C	Low NOx Burners	Heat for Process Tanks / Lines	8,760	NOx CO PE VOC	0.100 0.400 0.018 0.015	1.752	0.075 0.400 0.018 0.015	0.329 1.752 0.077 0.066	Gas	EE	TBD
8E	Upward Stack	88	TRE Burner	8C	Samples During Trials	Test & Training 4 days / week	1,000	NOx CO PE VOC	0.032 0.001	0.035 0.140 0.006 0.005	0.006 0.032 0.001 0.001	0.026 0.140 0.006 0.005	Gas	EE	TBD
9E	Upward Stack	98	TRE Flare	9C	Samples During Trials	Test & Training 4 days / week	1,000	NOx CO PE VOC	0.016 0.001	0.002 0.008 0.000 0.001	0.004 0.016 0.001 0.001	0.002 0.008 0.000 0.001	Gas	EE	TBD

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugilitied and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugilitie emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugilitie emission activities.

Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

<sup>2</sup> Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (i.e., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/hg), 2 days/wk).

3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST. Acids, CO., CS<sub>2</sub>, VOCs, H<sub>2</sub>S.

Just all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.

Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 ib VOC/20

Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 ib VOC/20 minute batch).

<sup>5</sup> Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>6</sup> Indicate method used to determine emission rate as follows: MB = material balance: ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO<sub>2</sub>, use units of ppmv (See 45CSR10).

#### Attachment J **EMISSION POINTS DATA SUMMARY SHEET**

			Table 2: Rel	ease Parar	meter Data			
Emission	Inner		Exit Gas		Emission Point B	Elevation (ft)	UTM Coordina	es (km)
Point ID No. (Must match Emission Units Table)	Diameter (ft.)	Temp.	Volumetric Flow <sup>1</sup> (acfm) at operating conditions	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height <sup>2</sup> (Release height of emissions above ground level)	Northing	Easting
1S	14 INCHES	460	1700	26.5	1500 FT	35 FT		
2S	14 INCHES	460	1700	26.5	1500 FT	35 FT		
3S	24 INCHES	1800	11820	62.0	1500 FT	35 FT		
4S	TBD	1440	TBD 1	500FT	†BD			
5S	TBD	TBD .	TBD 15	OFT	TBD			
6S	TBD	TBD	TBD	TBD	1500FT TI	ВР		·
7S	TBD	TBD	TBD	TBD	1500FT T	BD		
8S	TBD	TBD	TBD	TBD	1500FT T	BD		
9S	TBD	TBD	TBD	TBD	1500FT T	BD		

<sup>&</sup>lt;sup>1</sup> Give at operating conditions. Include inerts. <sup>2</sup> Release height of emissions above ground level.

		density		F
			lbs/hr	
Pyrolyzer 1 25 metric Tons/	Day;		2200	70
Furnace/Reactor 1; nat gas	fired			
	liq/gas out		1980	1000
	solid out		220	1000
Particle Wash 1A -PSV	liq/gas in		1980	1000
	cooling oil in		7220	110
	liq out		7620	260
	gas out		1580	260
Particle Wash 1B- PSV				
Heat Exchanger 1A/B; C/W	gas in		1580	260
	gas out		442	130
	liq out		1138	130
Heat Exch 1C; PSV; Refrige	ration gas in		442	130
	liq out		2	60
	gas out		440	60
Vacuum Pump 1A/B			440	60
Pyro Gas KO & Demister 1				
Cooling Tower 1; no emissi	ons			
Spray Diesel/Oil Cooler 1-	oil in		7220	260
	oil out		7220	110
Compressor -PSV?			440	

Pyro Gas	btu/scf	641			
			Assume %		
Al Pyro gas					
composition	H2	20-40%	34	325	btu/scf
es Tual	co	35-40%	40	325	btu/scf
	C1/C2	19%	19	1011/1783	btu/scf
	CO2	5-15%	7	0%	
	N2		0	0	
			100		
			Estimated	449	btu/scf
		3125	scfh/skid		
		8.24538259	lbmoles/hr		
	C from CO	3,29815303	lbmoles/hr		
	C from C1	1.09663588		70% CH4	
	C from C2	0.46998681		30% C2H6	
	CO2 from gas				
	Total C				
	Mole wt CO2				
			lb/hr CO2/skid	1	
	Annual CO2	1930	tons/yr		
				am/2000lb/to	

Portable Tanks(8 tanks) pyrolysis oil, N2 blanketed

Shredder, Conveyors, Material Handling lbs/hr

4400

4400

Annual CO2 Emissions from

Burners 1930 tons/yr

Flare 262

Generator 233

Total 2425 tons/yr

Frac Tanks( 8 tanks) pyrolysis oil, N2 blanketed

Here are the actual emissions expected from the combustion of the pyro gases:

NOx emissions = <30 PPM corrected to 3.0% cwygen

CO emissions = <50 PPM corrected to 3.0% cwygen

SOx emissions = <15 PPM corrected to 3.0% excess cwygen

PE Emission = <.0005 lbs./MM8TU

Flare 262 tons/yr
Pilot Gas
btu/hr 450,000
CO2 230 tons/yr
6 hr Pyro flaring 2 times per month
1930/(365\*24)\*12\*2\*6 = 32 tons/yr CO2

450000 btw/hr 116.65 lbs CO2 emissions /1mm btu Nat Gas 450000btw/hr X 8760hrs/yr X 116.65 lb CO2 /1 mmbtu Nat Gas /2000lb/ton 229.91715 tons/yr

Pumps-Pyrolyzer 1- 6 oil pumps

Safety Valves for Pyrolyzer 1

Truck Loading Rack
4mm gallons/yr
6000 gal/truck
15385 gal/workday
3957642.9 gal/yr
2.6 trucks/day
12.8 trucks/week
50.0 loading rate gpm
307.7 loading time minutes
5.1 hrs Loading time/day
1333.3 Annual loading hours

density

F

lbs/hr

		lbs/hr	
Pyrolyzer 1 25 metric Tons	/Day;	2200	70
Furnace/Reactor 1; nat gas	s fired		
	liq/gas out	1980	1000
	solid out	220	1000
Particle Wash 1A -PSV	liq/gas in	1980	1000
	cooling oil in	7220	110
	liq out	7620	260
	gas out	1580	260
Particle Wash 1B- PSV			
Heat Exchanger 1A/B; C/W	gas in	1580	260
	gas out	442	130
	liq out	1138	130
Heat Exch 1C; PSV; Refrige	eration gas in	442	130
	liq out	2	60
	gas out	440	60
Vacuum Pump 1A/B		440	60
Pyro Gas KO & Demister 1			
Cooling Tower 1; no emiss	ions		
Spray Diesel/Oil Cooler 1-	oil in	7220	260
	oil out	7220	110
Compressor -PSV?		440	

Pyro Gas	2 Emissions	641			
ryiu Gas	Diursei	041			
			Assume %		
Al Pyro gas					
composition	H2	20-40%	34	325	btu/scf
	co	35-40%	40	325	btu/scf
	C1/C2	19%	19	1011/1783	btu/scf
	CO2	5-15%	7	0%	
	N2		0	0	
			100		
			Estimated	449	btu/scf
CO2 Emission	ns 365 x 0.92 x 5	5700/2200 = 8	370 tons/yr		
		3125	scfh/skid		
		8.24538259			
	C from CO				
	C from C1		1,100,000,000,000,000	70% CH4	
	C from C2			30% C2H6	
	CO2 from gas	INTERNATION OF BUILDING			
	Total C	0.44190201			
	Total C Mole wt CO2		lb/lbmole		
	Mole wt CO2	44		1	
		44 239.44591	lb/hr CO2/skid	1	

Spray Diesel/Oil Cooler 1- oil in	7220
oil out	7220
Compressor -PSV?	440
Chiller 5 Ton - Refrigerant? Design?	
Frac Tanks(8 tanks) pyrolysis oil, N2 blanketed	
Shredder, Conveyors, Material Handling lbs/hr	4400
Dust Collection System cubic feet per minute	4400
Filter Surface 75 M^2	
Filter Sections 3 x 25 M^2	
Dust Emissions < 1.0 mg/M <sup>3</sup>	

Annual CO2 Emissions from

Burners 1930 tons/yr

Flare 262

Generator #REF!

Total #REF! tons/yr

450000 btu/hr

229.91715 tons/yr

116.65 lbs CO2 emissions /1mm btu Nat Gas

450000btu/hr X 8760hrs/yr X 116.65 lb CO2 /1 mmbtu Nat Gas /2000lb/ton

Frac Tanks(8 tanks) pyrolysis oil, N2 blanketed

Flare

Here are the actual emissions expected from the combustion of the pyro gases:

NOx emissions = <30 PPM corrected to 3.0% oxygen

CO emissions = <50 PPM corrected to 3.0% oxygen

SOx emissions = <15 PPM corrected to 3.0% excess oxygen

PE Emission \* < .0005 lbs:/MMBTU

Pumps-Pyrolyzer 1- 6 oil pumps

Safety Valves for Pyrolyzer 1

Truck Loading Rack 4mm gallons/yr 6000 gal/truck

15385 gal/workday 3957642.857 gal/yr 2.564102564 trucks/day 12.82051282 trucks/week Flare

Pilot Gas

btu/hr

CO2

262 tons/yr

450,000

230 tons/yr

6 hr Pyro flaring 2 times per month

1930/(365\*24)\*12\*2\*6 = 32 tons/yr CO2

Flare 262 tons/yr 450000 btu/hr Pilot Gas 116.65 lbs CO2 emissions /1mm btu Nat Gas 450,000 btu/hr 450000btu/hr X 8760hrs/yr X 116.65 lb CO2 /1 mmbtu Nat Gas /2000lb/ton CO2 230 tons/yr 229.91715 tons/yr 6 hr Pyro flaring 2 times per month 1930/(365\*24)\*12\*2\*6 = 32 tons/yr CO2 **Emissions:** Capacity 10,000,000.00 Btu/hr. Pilot 450,000 btu/hr 230 CO2 Tons/yr Burner Pyro Gas Heating value of the gas 800 Btu/ft^3 6250 scfh Gas density 0.052 lbs./ft^3 34 CO2 Tons/yr 478 lb CO2/hr Heating value of gas 15384.61538 Btu/lb. Flare CO2 Emissions 264 Air/fuel ratio 17.3 lbs./lb. Air/fuel ratio at 15.0% excess air 19.895 lbs./lb. Gas flow at max. operation 650.00 lbs./hr. air flow at max. operation 12931.75 lbs./hr. Stack flow max, operation 13581.75 lbs./hr. Carbon monoxide emissions Corrected to 3% Oxygen 50 PPM NOX emissions corrected to 3% Oxygen 80 PPM CO2 emissions 5.6 % NOX emissions flow 0.008 % CO emissions flow 0.005 % NOx mass flow at max. operation 1.08654 lbs/hr. CO mass flow at max. operation 0.6790875 lbs/hr. CO2 emissions max. operation 760,578 lbs/hr. Max. Operating time per year 80 hours 144 2 times/month X 12 Months X 6 hrs/event Max. NOx emissions 86.9232 lbs./year 54.327 lbs/year Max. CO emissions Max. CO2 emissions 60846.24 lbs./year 30.42312 Tons/yr Pilot Emissions 450,000 btu/hr 8760 hrs/yr 116.65 lbs CO2/mm btu NG 229.91715 Tons/yr

260.34027

Uncontrolled Generator Estimate 84.8 lbs/hr Nat Gas 2285 lbs/hr at 15% excess air 150kWh 229 BHP, 150kWh, 2042 scfh NG @ full load, Exhaust -NO catalytic emissions control at 229 BHP CO2 Carbon Dioxide 216-240 lbs/150 kWh Exhaust flow rate CO Carbon Monoxide

2285 lbs/hr at 15% excess air (estimated) CO2 Carbon Dioxide 232 lbs/150 kWh

PM Particulate matter

CO2 Carbon Dioxide

- No significant PM

233 lbs/150 kWh

0.878 lbs/150 kWh demand 0.029 CO tons/yr CO Calc = 1.74gms/HP-hr X 229Hp / 453.6 gms/lb 0.878 lbs/hr at full power

0.0505 lbs/150 kWh demand 0.030 NOx tons/yr NOx Calc = 1.77gms/HP-hr X 229Hp / 453.6 gms/lb 0.894 lbs/hr at full power

On Demand for power outage or testing 1.74 gms/HP-hr

NOx Nitrogen oxides

PM Particulate matter

CO Carbon Monoxide

PM Particulate matter

**THC Estimate** - 0.5 Grams/bhp-hr 0.008 THC tons/yr 0.252 lbs/hr at full power (estimated)

1.77 gms/bhp-hr

- No significant PM Annual CO2tons/yr 6.0 Testing CO2/yr - 232 lbs/operating hr X 1hr/week testing X 52 wks/yr/2000 lbs/ton

Exhaust -catalytic emissions control T =1440F, flow= 1206 cfm, press= 0.75 in HG at 229 BHP Generac SG150 229 BHP, 150kWh, 2042 scfh NG @ full load, CO2 Carbon Dioxide 233 lbs/150 kWh Exhaust flow rate 2285 lbs/hr at 15% excess air (not from Generac data sheet-estimated)

0.74 gms/bhp-hr 0.374 lbs/150 kWh demand 0.012 CO tons/yr

CO Calc = 0.74 gms/bhp-hr X 229 BHP /(453.6 gms/lb) 0.374 lbs/hr at full power NOx Nitrogen oxides

0.0505 lbs/150 kWh demand 0.002 NOx tons/yr NOx Calc = 0.10 gms/bhp-hr X 229 BHP /(453.6 gms/lb) 0.050 lbs/hr at full power **THC Estimate** - 0.14 Grams/bhp-hr 0.002 THC tons/yr

- No significant PM

0.071 lbs/hr at full power (estimated)

0.10 gms/bhp-hr

Annual CO2tons/yr 6.1 Testing CO2/yr - 233 lb: PM Particulate matter - No significant PM









Generator emissions no catalytic control.doc

Nat Gas Glycol Heater Estimate	2285 lbs/hr at 15% excess air (estimated)	1277.778 Tons/yr CO2			
max 4 mmbtu/hr normal 2.5 mm btu/hr	CO2 Carbon Dioxide 232 lbs/150	kWh			
CO2 Carbon Dioxide	2.5 mm btu/hrEstimates	2.5 mm btu/hr Estimates from EPA AP-42	4.0 mm btu/hr Estimates from	EPA AP-42	
CO Carbon Monoxide	0.898 CO tons/yr	1.752 CO tons/yr	2.803 CO tons/yr		
	0.082 lbs/mm btuhr	0.160 lbs/mm btuhr	0.160 lbs/mm btuhr		
	0.205 lbs/hr	0.400 lbs/hr	0.640 lbs/hr		
NOx Nitrogen oxides	1.095 NOx tons/yr	0.438 NOxtons/yr	0.701 NOx tons/yr		
	0.100 lbs/mm btu	0.040 lbs/mm btu	0.040 lbs/mm btu		
	0.255 lbs/hr	0.100 lbs/hr	0.160 lbs/hr		
VOC Estimate	0.000 THC tons/yr	0.066 THC tons/yr	0.105 THC tons/yr		
	0.000 lbs/mm btu	0.006 lbs/mm btu	0.006 lbs/mm btu		
	0.000 lbs/hr	0.015 lbs/hr	0.024 lbs/hr		
PM Particulate matter -	0.055 PM tons/yr	0.077 PM tons/yr	0.123 PM tons/yr		
	0.005 lbs/mm btu	0.007 lbs/mm btu	0.007 lbs/mm btu		
	0.013 lbs/hr	0.018 lbs/hr	0.028 lbs/hr		
	0.010 103111				
Pyro Gas Glycol Heater Estimate max 4 mmbtu/hr normal 2.5 mm btu/hr	Gas Composition				
max 4 mmbtu/hr normal 2.5 mm btu/hr	Gas Composition	Pyrolysis Gas Standard Burners	Pyrolysis Low NOX Burners		
max 4 mmbtu/hr normal 2.5 mm btu/hr	Gas Composition H2	Pyrolysis Gas Standard Burners 2.5 mm btu/hr Estimates from EPA AP-42	Pyrolysis Low NOX Burners 2.5 mm btu/hr Estimates from	EPA AP-42	
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr			EPA AP-42	
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners	2.5 mm btu/hr Estimates from EPA AP-42	2.5 mm btu/hr Estimates from	EPA AP-42	
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr	EPA AP-42	
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr		Composition (est
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr		Composition (est
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr	Pyrolysis Gas C	The state of the s
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr 0.526 NOx tons/yr	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr 0.329 NOx tons/yr	Pyrolysis Gas C H2	34
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr 0.329 NOx tons/yr 0.030 lbs/mm btu	Pyrolysis Gas C H2 CO	34 40
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide  CO Carbon Monoxide  NOx Nitrogen oxides	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr 0.329 NOx tons/yr 0.030 lbs/mm btu	Pyrolysis Gas C H2 CO CH4	34 40 13.3
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide NOx Nitrogen oxides	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu 0.120 lbs/hr	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu 0.100 lbs/hr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.329 NOx tons/yr 0.030 lbs/mm btu 0.075 lbs/hr	Pyrolysis Gas C H2 CO CH4 C2H6	34 40 13.3 5.7
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide CO Carbon Monoxide NOx Nitrogen oxides	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu 0.120 lbs/hr 0.120 lbs/hr	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu 0.100 lbs/hr  0.066 THC tons/yr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.329 NOx tons/yr 0.030 lbs/mm btu 0.075 lbs/hr  0.066 THC tons/yr	Pyrolysis Gas C H2 CO CH4 C2H6	34 40 13.3 5.7 7
max 4 mmbtu/hr normal 2.5 mm btu/hr CO2 Carbon Dioxide  CO Carbon Monoxide  NOx Nitrogen oxides  VOC Estimate	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.120 lbs/hr  0.120 lbs/mm btu 0.120 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu 0.100 lbs/hr  0.066 THC tons/yr 0.006 lbs/mm btu	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.329 NOx tons/yr 0.030 lbs/mm btu 0.075 lbs/hr  0.066 THC tons/yr 0.006 lbs/mm btu	Pyrolysis Gas C H2 CO CH4 C2H6	34 40 13.3 5.7 7
max 4 mmbtu/hr normal 2.5 mm btu/hr	Gas Composition H2 Pyrolysis Gas burning 2.5 mm btu/hr ARTI data used for the Pyrolysis Burners 0.526 CO tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.526 NOx tons/yr 0.048 lbs/mm btu 0.120 lbs/hr  0.000 THC tons/yr 0.000 lbs/mm btu 0.000 lbs/mm btu	2.5 mm btu/hr Estimates from EPA AP-42 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.438 NOx tons/yr 0.040 lbs/mm btu 0.100 lbs/hr  0.066 THC tons/yr 0.006 lbs/mm btu 0.015 lbs/hr	2.5 mm btu/hr Estimates from 1.752 CO tons/yr 0.160 lbs/mm btuhr 0.400 lbs/hr  0.329 NOx tons/yr 0.030 lbs/mm btu 0.075 lbs/hr  0.066 THC tons/yr 0.006 lbs/mm btu 0.015 lbs/hr	Pyrolysis Gas C H2 CO CH4 C2H6	34 40 13.3 5.7 7





Trial Unit Operation will be 1/25 th of the Pyrolysys 25 ton/day skid

TRE Propane Burners TRE					
max 200,000 btu/hr norm	al 150 Gas Composition				
CO2 Carbon Dioxide	H2				
	Propane Gas Standar	d Burners	Propane Low NOX Burners		
	200k btu/hr Estimate:	s from EPA AP-42	200k btu/hr Estimates from EP	A AP-42	
CO Carbon Monoxide		0.140 CO tons/yr	0.140 CO tons/yr		
		0.160 lbs/mm btuhr	0.160 lbs/mm btuhr		
		0.032 lbs/hr	0.032 lbs/hr		
				Propane Ga	s Composition (est)
NOx Nitrogen oxides		0.035 NOx tons/yr	0.026 NOx tons/yr	H2	34
		0.040 lbs/mm btu	0.030 lbs/mm btu	CO	40
		0.008 lbs/hr	0.006 lbs/hr	CH4	13.3
				C2H6	5.7
VOC Estimate		0.005 THC tons/yr	0.005 THC tons/yr	CO2	7
		0.006 lbs/mm btu	0.006 lbs/mm btu		100
		0.001 lbs/hr	0.001 lbs/hr		
PM Particulate matter		0.006 PM tons/yr	0.006 PM tons/yr		
		0.007 lbs/mm btu	0.007 lbs/mm btu		
		0.001 lbs/hr	0.001 lbs/hr		



TRE Flare

Basis: TRE unit produces Pyrolysis Gas which is flared in the TRE flare

TRE Pyro Gas production rate is estimated to be 1/50th of the total 2 skid Pyro Gas production

TRE Pyro Gas =

18.798 lbs/hr

125 lb/lbmole

Here are the actual emissions expected from the combustion of the pyro gases:

NOx emissions = <30 PPM corrected to 3.0% oxygen

CO emissions = <50 PPM corrected to 3.0 % oxygen

SOx emissions = < 15 PPM corrected to 3.0% excess oxygen

PE Emission = < .0005 lbs./MMBTU

TRE Pyro Gas Flare		
max 100,000 btu/hr nori	nal 60,00	0 btu/hr
In service 1000 hrs/yr		
Py	rolysis G	as Flare Burn 100k btu/hr
Es	stimates f	rom EPA AP-42
CO Carbon Monoxide	0.008	CO tons/yr
	0.160	lbs/mm btuhr
	0.016	lbs/hr
NOx Nitrogen oxides	0.002	NOx tons/yr
	0.040	lbs/mm btu
	0.004	lbs/hr
VOC Estimate	0.000	THC tons/yr
	0.006	lbs/mm btu
	0.001	lbs/hr
PM Particulate matter	0.000	PM tons/yr
	0.007	lbs/mm btu
	0.001	lbs/hr

yro Gas	btu/scf	476.594						
Al Pyro gas	composition							
	H2	20-40%	34	325	btu/scf	110.5		
assumed f	CO	35-40%	40	325	btu/scf	130		
	C1/C2	19%	19 1011	/1783	btu/scf	134.463		
	CO2	5-15%	7	0%		101.631		
	N2		0	0				
			100					
			Estimated			476.594	btu/scf	
						59574.25	btu/hr	
CO2 Emiss	ions 9.6lbs/	4.8	tons/yr CO2 emi:	ssions				
		125	scfh				lb/lbmole	lbs
		0.329815	lbmoles/hr			H2	2	0.68
	C from CO	0.131926	lbmoles/hr			СО	28	11.2
	C from C1	0.043865	70%	CH4		CH4	16	2.128
	C from C2	0.018799	30%	C2H6		C2H6	30	1.71
	CO2 from g	0.023087				CO2	44	3.08
	Total C	0.217678	lbmoles/hr			Lbs/hr		18.798
	Mole wt CC	44	lb/lbmole					
	CO2	9.577836	lb/hr CO2 Trial U	nit				
	Annual CO	4.8	tons/yr					



### D2.1 45CSR R-6 — Control of Air Pollution from Combustion of Refuse

This section requires particulate matter emission for new source to be limited as provided to emission standards for incinerators and incineration (Refuse-Combustion) using formula provided by:

Emissions(lb/hr) = F x Incinerator capacity (tons/hr)

Were factor F, as per Table 1: Determining maximum allowable particulate emission. Incinerator Capacity Factor-'F'

- a) less than 15000 lb/hr 5.43
- b) 15000 lb/hr or greater 2.72

Emissions(lb/hr) =  $5.43 \times 0.825$  tons/hr =  $4.479 \times 4.50$ lb/hr Are we "combusting refuse?" Or is this just the relevant regulation? Need guidance from Bowles – what emissions to report for "incineration?"

Pyrolysis Capacity 25 tonnes/day/unit 2 units X 25 tonnes/day X 2200lbs/tonne X 1 day/24hr=

4583 lbs/hr 2.29 tons/hr

5.43

Factor F select a) less than 15000 lb/hr

Emissions lb/hr = 5.43 X 25 X 2 X 2200lbs/tonne / 2000 lbs/ton = tons/hr

12.44 lbs/hr emissions



# UNITED STATES ENVIRONMENTAL PROTECTION AGENCY 2025 MODEL YEAR CERTIFICATE OF CONFORMITY WITH THE CLEAN AIR ACT

OFFICE OF TRANSPORTATION AND AIR QUALITY ANN ARBOR, MICHIGAN 48105

Byron J. Bunker, Division Director

Compliance Division

Certificate Issued To: Generac Power Systems, Inc.

(U.S. Manufacturer or Importer)

Certificate Number: SGNXB08.92O3-015

Effective Date: 11/27/2024

Expiration Date: 12/31/2025

Issue Date: 11/27/2024

Revision Date:

Manufacturer: Generac Power Systems, Inc.

Engine Family: SGNXB08.92O3

Mobile/Stationary Certification Type: Stationary

Fuel: Natural Gas (CNG/LNG)

**Emission Standards:** 

Part 60 Subpart JJJJ Table 1 NOx ( g/Hp-hr ) : 2.0 CO ( g/Hp-hr ) : 4.0 VOC ( g/Hp-hr ) : 1.0

Emergency Use Only: Y

Pursuant to Section 213 of the Clean Air Act (42 U.S.C. section 7547) and 40 CFR Part 60, 1065, 1068, and 60 (stationary only and combined stationary and mobile) and subject to the terms and conditions prescribed in those provisions, this certificate of conformity is hereby issued with respect to the test engines which have been found to conform to applicable requirements and which represent the following nonroad engines, by engine family, more fully described in the documentation required by 40 CFR Part 60 and produced in the stated model year.

This certificate of conformity covers only those new nonroad spark-ignition engines which conform in all material respects to the design specifications that applied to those engines described in the documentation required by 40 CFR Part 60 and which are produced during the model year stated on this certificate of the said manufacturer, as defined in 40 CFR Part 60. This certificate of conformity does not cover nonroad engines imported prior to the effective date of the certificate.

It is a term of this certificate that the manufacturer shall consent to all inspections described in 40 CFR 1068.20 and authorized in a warrant or court order. Failure to comply with the requirements of such a warrant or court order may lead to revocation or suspension of this certificate for reasons specified in 40 CFR Part 60. It is also a term of this certificate that this certificate may be revoked or suspended or rendered void *ab initio* for other reasons specified in 40 CFR Part 60.

This certificate does not cover large nonroad engines sold, offered for sale, or introduced, or delivered for introduction, into commerce in the U.S. prior to the effective date of the certificate.



# STATEMENT OF EXHAUST EMISSIONS 2025 Spark-Ignited Generators Industrial Series - NON-SCAQMD Certified, Stationary Emergency

242350	Engine	EPA Engine	. PLISTON	Catalyst	FPA	Engine Emissions		Grams/bhp-hr.			19529	Fuel	
Model	(L)	Family	Fuel	Required	Certification #	Designation	THC	NMHC	NOx	CO	Rated RPM	BHP	Flow (lb.
SG035, 40, 45, 50NA	4,4	SGNXB04.4MDI	NG		SGNXB04.4MDI-020	A04.5SPN057A0	0.63	0.09	4.42	34.6	1800	75	25.9
SG035, 40, 45, 50NA	4.4	SGNXB04.4MDI	LPV		SGNXB04.4MDI-020	A04.5SPV057A0	0.83	N/A	5.20	63.4	1800	76	29.5
SG050T, 60, 70, 80	4,4	SGNXB04.4MDI	NG		SGNXB04.4MDI-020	A04.5SPN096A0	N/A	0.12	3.32	42.3	1800	129	45.2
SG050T, 60, 70, 80	4.4	SGNXB04,4MDI	LPV	NO	SGNXB04.4MDI-020	A04.5SPV096A0	0.47	N/A	3.23	58.8	1800	129	49.0
SG080	8.9	SGNXB08.9MDA	NG		SGNXB08.9MDA-019	A08.9GSN093A0	0.59	N/A	1.06	91.9	1800	125	62.4
5G080	8.9	SGNXB08.9MDA	LPV		SGNXB08,9MDA-019	A08.9GSV095A0	0.70	N/A	1.52	123	1800	128	61.5
SG080	8.9	SGNXB08.9MDA	LPL		SGNXB08.9MDA-019	A08.9MSL095A0	0.74	N/A	1.31	126	1800	128	60.2
5G080, 100	8.9	SGNXB08.9201	NG		SGNXB08.9201-005	E08.9MDL113A1	0.17	0.00	0.01	1.01	1800	151	51.9
SG080, 100 (LPF)	8.9	SGNXB08.9201	NG		SGNXB08.9201-005	E08.9MDV113A0	0.11	0.00	0.12	0.03	1800	152	46.9
SG080, 100	8.9	SGNXB08.9202	LPV		SGNXB08.9202-001	F08.9MSV106A0	0.01	N/A	0.21	0.22	1800	142	54.8
SG080, 100	8.9	SGNXB08.9202	LPL		5GNXB08.9202-001	F08.9MSL106A0	0.03	0.01	0.00	0.36	1800	155	55.3
SG/MG130, 150	8.9	SGNXB08.9203	NG		SGNXB08.9203-015	E08.9MSN170A0	0.14	0.00	0.10	0.74	1800	228	84.8
SG/MG130, 150	8.9	SGNXB08.9204	LPV		SGNXB08.9204-016	F08.9MSV169A1	0.06	0.00	0.09	0.19	1800	230	85.4
SG/MG150, 200	14.2	SGNXB14.22C1	NG		SGNXB14.22C1-017	E14,2MSN227A3	0.24	0.01	0.12	0.21	1800	304	101
SG/MG230, 250	14.2	SGNXB14.22C1	NG		SGNXB14.22C1-017	E14.2MSN279A3	0.14	0.00	0.35	0.41	1800	374	142
SG/MG275, 300	14.2	SGNXB14.22C1	NG	YES	SGNXB14.22C1-017	E14.2MSN343A3	0.03	0.00	0.04	0.31	1800	460	140
SG/MG350, 400	21.9	SGNXB21.92C1	NG	LE2	SGNXB21.92C1-009	E21.9MSN474A4	0.07	0.00	0.26	0.21	1800	651	176
SG/MG350, 400 (LPF)	21.9	SGNXB21.92C1	NG		SGNXB21.92C1-009	E21.9MSN474A5	0.30	0.00	0.06	0.12	1800	621	214
SG/MG350, 400, 450	21,9	SGNXB21.92C3	NG		5GNXB21.92C3-010	E21.9MSN0502A4	0.15	0.00	0.08	0.32	1800	673	223
5G/MG350, 400, 450 (LPF)	21,9	SGNXB21.92C3	NG		SGNXB21.92C3-010	E21.9MSN0502A5	0.19	0.00	0.05	0.17	1800	673	224
SG/MG500	25.8	5GNXB25.82C1	NG	1 1	SGNXB25.82C1-008	E25.8MSN580A4	0.16	0.00	0.03	0.59	1800	777	280
SG/MG500 (LPF)	25.8	SGNXB25.82C1	NG	- 1	SGNXB25.82C1-008	E25.8MSN580A5	0.19	0.00	0.06	0.57	1800	777	280
SG/MG625	33.9	SGNXB33.92C1	NG		SGNXB33.92C1-035	E33.9MSN677A0	0.13	0.00	0.01	0.21	1800	909	325
SG/MG750	33.9	SGNXB33.92C1	NG		SGNXB33.92C1-035	E33.9MSN803A0	0.18	0.00	0.15	0.91	1800	1077	417
SG/MG1000	49.0	SGNXB49.02C1	NG		SGNXB49.02C1-003	E49.0ASN1100A0	0.12	0.00	0.03	0.64	1800	1475	427

NG/LP: Natural Gas LPV; Liquid Propane Vapor LPL: Liquid Propane Liquid Engine BHP is taken from Engine Emissions Certificate Results LPG: Liquid Propane Vapor or Liquid Propane Liquid LPF: Units with Option Low Pressure Fuel System

N/A: Not Applicable Refer to Page 2 for Definitions and Advisory Notes.

1 OF 2



# STATEMENT OF EXHAUST EMISSIONS 2025 Spark-Ignited Generators Industrial Series - NON-SCAQMD Certified, Stationary Emergency

#### 2025 EPA SPARK-IGNITED EXHAUST EMISSIONS DATA

Effective since 2009, the EPA has implemented exhaust emissions regulations on stationary spark-ignited (gaseous) engine generators for emergency applications. All Generac spark-ignited gensets, including SG, MG, QTA, QT and RG series gensets that are built with engines manufactured in 2009 and later meet the requirements of 40CFR part 60 subpart JJJJ and are EPA certified. These generator sets are labeled as EPA Certified with decals affixed to the engines' valve covers.

The attached documents summarize the general information relevant to EPA certification on these generator sets. This information can be used for submittal data and for permitting purposes, if required. These documents include the following information:

#### **EPA Engine Family**

The EPA Engine Family is assigned by the Manufacturer under EPA guidelines for certification purposes and appears on the EPA certificate.

#### Catalyst Required

Indicates whether a three-way catalyst (TWC) and Air/Fuel Ratio control system are required on the generator set to meet EPA certification requirements. Generally, units rated 80kW and smaller do not require a TWC to meet EPA requirements do need one if the California SCAQMD option is selected. Please see "California SCAQMD" below for additional information on this option.

#### Combination Catalyst or Separate Catalyst

SG and MG series generator sets typically utilize a single combination catalyst/silencer as part of meeting EPA certification requirements. Many QT and RG series generator sets use the same engines as SG series units, but have different exhaust configurations that require the use of conventional silencers with additional separate catalysts installed.

#### **EPA Certificate Number**

Upon certification by the EPA, a Certificate Number is assigned by the EPA.

#### Emissions Actuals - Grams/bhp-hr

Actual exhaust emission data for Total Hydrocarbons (THC), Nitrogen Oxides (NOx) and Carbon Monoxide (CO) that were submitted to EPA and are official data of record for certification. This data can be used for permitting if necessary. Values are expressed in grams per brake horsepower-hour; to convert to grams/kW-hr, multiply by 1,341. Please see advisory notes below for further information.

#### California Units, SCAQMD CEP Number

A separate low-emissions option is available on many Generac gaseous-fueled generator sets to comply with the more stringent South Coast Air Quality Management District requirements that are recognized in certain areas in California. Gensets that include this option are also EPA Certified.

#### General Advisory Note to Dealers

The information provided here is proprietary to Generac and its' authorized dealers. This information may only be disseminated upon request, to regulatory governmental bodies for emissions permitting purposes or to specifying organizations as submittal data when expressly required by project specifications, and shall remain confidential and not open to public viewing. This information is not intended for compilation or sales purposes and may not be used as such, nor may it be reproduced without the expressed written permission of Generac Power Systems, Inc.

#### Advisory Notes on Emissions Actuals

- The stated values are actual exhaust emission test measurements obtained from units representative of the generator types and engines described.
- Values are official data of record as submitted to the EPA and SCAQMD for certification purposes. Testing was conducted in accordance with prevailing EPA protocols, which are typically accepted by SCAQMD and other regional authorities.
- No emission values provided are to be construed as guarantees of emissions levels for any given Generac generator unit.
- · Generac Power Systems, Inc. reserves the right to revise this information without prior notice.
- · Consult state and local regulatory agencies for specific permitting requirements.
- The emissions performance data supplied by the equipment manufacturer is only one element required toward completion of the permitting and installation process. State and local
  regulations may vary on a case-by-case basis and must be consulted by the permit applicant/equipment owner prior to equipment purchase or installation. The data supplied herein by
  Generac Power Systems, Inc. cannot be construed as a guarantee of installability of the generator set.
- The emission values provided are the result of multi-mode, weighted scale testing in accordance with EPA testing regulations, and may not be representative of any specific load point.
- The emission values provided are not to be construed as emission limits.

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

**EPA Certified Stationary Emergency** 



#### Standby Power Rating

150 kW, 188 kVA, 60 Hz



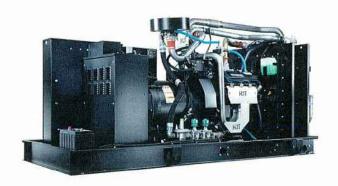


Image used for illustration purposes only

### **Codes and Standards**

Generac products are designed to the following standards:.





UL2200, UL508, UL489



CSA C22.2



BS5514 and DIN 6271



**SAE J1349** 



NFPA 37, 70, 99, 110



NEC700, 701, 702, 708



NEMA ICS10, MG1, 250, ICS6, AB1



ANSI C62.41



IBC 2009, CBC 2010, IBC 2012, ASCE 7-05, ASCE 7-10, ICC-ES AC-156 (2012)

## **Powering Ahead**

Generac provides superior quality by designing and manufacturing most of its generator components, such as alternators, enclosures, control systems and communications software. Generac also makes its own spark-ignited engines, and you'll find them on every Generac gaseous-fueled generator. We engineer and manufacture them from the block up — all at our facilities throughout Wisconsin. Applying natural gas and LP-fueled engines to generators requires advanced engineering expertise for reliability, durability and necessary performance. By designing specifically for these dry, hotter-burning fuels, the engines last longer and require less maintenance. Building our own engines also means we control every step of the supply chain and delivery process, so you benefit from single-source responsibility.

Plus, Generac Industrial Power's distribution network provides all parts and service so you don't have to deal with third-party suppliers. It all leads to a positive owner experience and higher confidence level. Generac spark-ignited engines give you more options in commercial and industrial generator applications as well as extended run time from utility-supplied natural gas.

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

EPA Certified Stationary Emergency

#### STANDARD FEATURES

#### **ENGINE SYSTEM**

- · Oil Drain Extension
- · Air Cleaner
- · Fan Guard
- Stainless Steel Flexible Exhaust Connection
- · Factory Filled Oil and Coolant
- Radiator Duct Adapter (Open Set Only)
- · Critical Silencer/Catalyst

#### **FUEL SYSTEM**

- · NPT Fuel Connection on Frame
- · Primary and Secondary Fuel Shutoff

#### **COOLING SYSTEM**

- · Closed Coolant Recovery System
- · UV/Ozone Resistant Hoses
- · Factory-Installed Radiator
- · 50/50 Ethylene Glycol Antifreeze
- · Radiator Drain Extension

#### **ELECTRICAL SYSTEM**

- · Battery Charging Alternator
- Battery Cables
- Battery Tray
- Rubber-Booted Engine Electrical Connections
- · Solenoid Activated Starter Motor

#### ALTERNATOR SYSTEM

- UL2200 GENprotect™
- · Class H Insulation Material
- 2/3 Pitch
- · Skewed Stator
- · Permanent Magnet Excitation
- · Sealed Bearings
- · Amortisseur Winding
- · Full Load Capacity Alternator

#### **GENERATOR SET**

- · Internal Genset Vibration Isolation
- · Separation of Circuits High/Low Voltage

GENERAC INDUSTRIAL

- · Separation of Circuits Multiple Breakers
- · Wrapped Exhaust Piping
- · Standard Factory Testing
- · 2 Year Limited Warranty (Standby Rated Units)
- Silencer Mounted in the Discharge Hood (Enclosed Only)

#### **ENCLOSURE (If Selected)**

- Rust-Proof Fasteners with Nylon Washers to Protect Finish
- High Performance Sound-Absorbing Material (Sound Attenuation Enclosures)
- Gasketed Doors
- · Stamped Air-Intake Louvers
- Upward Facing Discharge Hoods (Radiator and Exhaust)
- · Stainless Steel Lift Off Door Hinges
- · Stainless Steel Lockable Handles
- RhinoCoat™ Textured Polyester Powder Coat Paint

#### CONTROL SYSTEM



#### Digital H Control Panel- Dual 4x20 Display

#### **Program Functions**

- · Programmable Crank Limiter
- · 7-Day Programmable Exerciser
- Special Applications Programmable Logic Controller
- · RS-232/485 Communications
- 3 Phase Sensing Digital Voltage Regulator
- · 2-Wire Start Capability

- · Date/Time Fault History (Event Log)
- · Isochronous Governor Control
- · Waterproof/Sealed Connectors
- · Audible Alarms and Shutdowns
- · Not in Auto (Flashing Light)
- · Auto Off/Manual Switch
- E-Stop (Red Mushroom-Type)
- NFPA110 Level I and II (Programmable)
- · Customizable Alarms, Warnings, and Events
- Modbus<sup>®</sup> Protocol
- Predictive Maintenance Algorithm
- Sealed Boards
- · Password Parameter Adjustment Protection
- · Single Point Ground
- 16 Channel Remote Trending
- · 0.2 msec High Speed Remote Trending
- Alarm Information Automatically Annunciated on the Display

#### **Full System Status Display**

- · Power Output (kW)
- Power Factor
- · kW Hours, Total, and Last Run

- · Real/Reactive/Apparent Power
- · All Phase AC Voltage
- · All Phase Currents
- · Oil Pressure
- · Coolant Temperature
- Coolant Level
- · Engine Speed
- Battery Voltage
- Frequency

#### **Alarms and Warnings**

- · Oil Pressure
- · Coolant Temperature
- · Coolant Level
- Engine Overspeed
- · Battery Voltage
- · Alarms and Warnings Time and Date Stamped
- Snap Shots of Key Operation Parameters During Alarms and Warnings
- Alarms and Warnings Spelled Out (No Alarm Codes)

#### PARALLELING CONTROLS

- · Auto-Synchronization Process
- · Isochronous Load Sharing
- Reverse Power Protection

- Maximum Power Protection
- Electrically Operated, Mechanically Held Paralleling Switch
- · Sync Check System
- Independent On-Board Paralleling
- Optional Programmable Logic Full Auto Back-Up Controls (PLS)
- · Shunt Trip and Auxiliary Contact

### SG150 | 9.0 L | 150 kW

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

EPA Certified Stationary Emergency

## GENERAC INDUSTRIAL ENERGY

#### CONFIGURABLE OPTIONS

#### **ENGINE SYSTEM**

- Engine Block Heater
- o Oil Heater
- o Air Filter Restriction Indicator
- o Radiator Stone Guard (Open Set Only)
- o Baseframe Cover/Rodent Guard
- Level 1 Fan and Belt Guards (Enclosed Units Only)
- Shipped Loose Critical Silencer (Open Set Only)

#### **FUEL SYSTEM**

- o NPT Flexible Fuel Line
- Dual Fuel NG/LPV
- o Dual Fuel NG/LPL

#### **ELECTRICAL SYSTEM**

- o 10A UL Battery Charger
- Battery Warmer

#### ALTERNATOR SYSTEM

- Alternator Upsizing
- o Anti-Condensation Heater
- o Tropical Coating

#### **CIRCUIT BREAKER OPTIONS**

- o Main Line Circuit Breaker
- o 2<sup>nd</sup> main Line Circuit Breaker
- Shunt Trip and Auxiliary Contact
- o Electronic Trip Breakers

#### **GENERATOR SET**

- Demand Response Rating
- Extended Factory Testing (3 Phase Only)
- o IBC Seismic Certification
- 8 Position Load Center

#### **ENCLOSURE**

- Weather Protected Enclosure
- Level 1 Sound Attenuated
- Level 2 Sound Attenuated
- Level 2 Sound Attenuated with Motorized Dampers
- Steel Enclosure
- Aluminum Enclosure
- o AC/DC Enclosure Lighting Kit
- Enclosure Heater
- Pad Vibration Isolation
- Up to 200 MPH Wind Load Rating (Contact Factory for Availability)
- o Door Open Alarm Switch

#### **CONTROL SYSTEM**

- NFPA 110 Compliant Level 1 21-Light Remote Annunciator
- Remote Relay Assembly (8 or 16)
- o Oil Temperature Indication and Alarm
- Remote E-Stop (Break Glass-Type, Surface Mount)
- Remote E-Stop (Red Mushroom-Type, Surface Mount)
- Remote E-Stop (Red Mushroom-Type, Flush Mount)
- 10A Engine Run Relay
- Ground Fault Annunciator
- o 100 dB Alarm Hom
- o 120V GFCI and 240V Outlets
- Damper Alarm Contacts (Motorized Dampers Only)
- Auxiliary Circuit Breaker Contacts to Controller

#### WARRANTY (Standby Gensets Only)

- 2 Year Extended Limited Warranty
- o 5 Year Extended Limited Warranty
- o 7 Year Extended Limited Warranty
- o 10 Year Extended Limited Warranty

#### **ENGINEERED OPTIONS**

#### **ENGINE SYSTEM**

- Coolant Heater Ball Valves
- o Fluid Containment Pan

#### ATLERNATOR SYSTEM

o 3rd Breaker System

#### **CONTROL SYSTEM**

Battery Disconnect Switch

#### GENERATOR SET

- Special Testing
- Battery Box

## SG150 | 9.0 L | 150 kW

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

EPA Certified Stationary Emergency

## GENERAC INDUSTRIAL

#### APPLICATION AND ENGINEERING DATA

#### **ENGINE SPECIFICATIONS**

#### General

Make	Generac
Cylinder #	8
Туре	V
Displacement - in3 (L)	543 (8.9)
Bore - in (mm)	4.49 (114.3)
Stroke - in (mm)	4.25 (108)
Compression Ratio	G18 - 10.5:1 / G26 - 9.1:1 *
Intake Air Method	Turbocharged/Aftercooled
Number of Main Bearings	5
Connecting Rods	Forged Steel
Cylinder Head	Cast Iron
Cylinder Liners	No
Ignition	High Energy
Piston Type	Aluminum Alloy
Crankshaft Type	Forged Steel
Lifter Type	Hydraulic Roller
Intake Valve Material	Steel Alloy
Exhaust Valve Material	Stainless Steel
Hardened Valve Seats	Yes

#### **Engine Governing**

Governor	Electronic	
Frequency Regulation (Steady State)	±0.25%	

#### Lubrication System

Oil Pump Type	Gear Driven
Oil Filter Type	Full-Flow Spin-On Cartridge
Crankcase Capacity: qt (L)	G18 - 8.5 (8.0) / G26 - 9.5 (10.0)

#### Cooling System

Cooling System Type	Pressurized Closed
Fan Type	Pusher
Fan Speed (RPM)	G18 - 2,330 / G26 - 2,386 *
Fan Diameter - in (mm)	22 (559)

#### Fuel System

Fuel Type	Natural Gas, Propane Vapor/ Liquid
Carburetor	Down Draft
Secondary Fuel Regulator	Standard
Fuel Shut Off Solenoid	Standard
Operating Fuel Pressure - in H <sub>2</sub> O	7 - 11 (1.7 - 2.7)
Optional Operating Fuel Pressure (LPL) — psi (KPa)	30 - 312 (206 - 2,151)

\*When designing the external fuel system, assume a 20% safety factor to the upper and lower limit of the specified fuel pressure range to account for site variation and measurement at the generator test port. Refer to Generac 10000046207, latest rev, for proper gas supply guidelines (Contact Factory for Details).

#### Engine Electrical System

System Voltage	12 VDC
Battery Charger Alternator	Standard
Battery Size	See Battery Index 0161970SBY
Battery Voltage	12 VDC
Ground Polarity	Negative

\* G18 refers to all engines manufactured before August 3rd, 2018. G26 refers to all engines manufactured after August 3rd, 2018.

#### **ALTERNATOR SPECIFICATIONS**

Standard Model	K0150124Y26
Poles	4
Field Type	Revolving
Insulation Class - Rotor	H
Insulation Class - Stator	H
Total Harmonic Distortion	<5%
Telephone Interference Factor (TIF)	<50

Standard Excitation	Permanent Magnet	
Bearings	Single Sealed Ball	
Coupling	Direct Drive	
Prototype Short Circuit Test	Yes	
Voltage Regulator Type	Full Digital	
Number of Sensed Phases	All	
Regulation Accuracy (Steady State)	±0.25%	

## SG150 | 9.0 L | 150 kW

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

EPA Certified Stationary Emergency



#### **OPERATING DATA**

#### **POWER RATINGS**

	G18, G26 - Na	atural Gas *	G18, G26 - Propane/Dual Fuel *		
Single-Phase 120/240 VAC @ 1.0pf	144 kW/144 kVA	Amps: 600	134 kW/134 KVA	Amps: 558	
Three-Phase 120/208 VAC @0.8pf	150 kW/188 kVA	Amps: 521	140 kW/175 kVA	Amps: 486	
Three-Phase 120/240 VAC @0.8pf	150 kW/188 kVA	Amps: 452	140 kW/175 kVA	Amps: 422	
Three-Phase 277/480 VAC @0.8pf	150 kW/188 kVA	Amps: 226	140 kW/175 kVA	Amps: 211	
Three-Phase 346/600 VAC @0.8pf	150 kW/188 kVA	Amps: 181	140 kW/175 kVA	Amps: 169	

#### **MOTOR STARTING CAPABILITIES (skVA)**

#### skVA vs. Voltage Dip

277/480 VAC	30%	208/240 VAC	30%
K0150124Y26	327	K0150124Y26	250
K0200124Y21	478	K0200124Y21	361

#### **FUEL CONSUMPTION RATES\***

Natural Gas – scfh (m³/hr)		Propane Vapor – scfh (m3/hr)		Propane Liquid – gal/hr (Lph)	
Percent Load	Standby	Percent Load	Standby	Percent Load	Standby
25%	668 (18.9)	25%	280 (7.9)	25%	6.7 (25.4)
50%	1,127 (31.9)	50%	430 (12.2)	50%	11.4 (43.2)
75%	1,583 (44.8)	75%	573 (16.2)	75%	15.7 (59.4)
100%	2,042 (57.8)	100%	720 (20.4)	100%	20.0 (75.7)

<sup>\*1.5</sup>X maximum site rated fuel consumption should be used for gas supply design practices. Refer to Generac 10000046207, latest rev., for more information or contact factory for details.

#### COOLING

	Standby
cfm (m³/min)	5,598 (158.5)
gpm (Lpm)	27.5 (104)
gal (L)	6.3 (24.0)
°F (°C)	122 (50)
See Bulletin 0199270SSD	
in H₂O (kPa)	0.5 (0.12)
	gpm (Lpm) gal (L) °F (°C) See Bullet

#### **COMBUSTION AIR REQUIREMENTS**

	Standby	
Flow at Rated Power cfm — (m³/min)	343 (9.7)	

#### **ENGINE**

# Rated Engine Speed RPM 1,800 Horsepower at Rated kW\*\* hp 229 Piston Speed ft/min (m/min) 1,275 (389) BMEP psi (kPa) 185 (1,277)

#### **EXHAUST**

		Standby
Exhaust Flow (Rated Output)	cfm (m³/min)	1,206 (34.1)
Maximum Exhaust Backpressure	inHG (kPa)	0.75 (2.54)
Exhaust Temp (Rated Output - Post Silencer)	°F (°C)	1,440 (782)

Deration – Operational characteristics consider maximum ambient conditions. Derate factors may apply under atypical site conditions.

Please contact a Generac Power Systems Industrial Dealer for additional details. All performance ratings in accordance with BS5514 and DIN6271 standards.

Standby - See Bulletin 0187500SSB

<sup>\*\*</sup> Refer to "Emissions Data Sheet" for maximum bHP for EPA and SCAQMD permitting purposes.

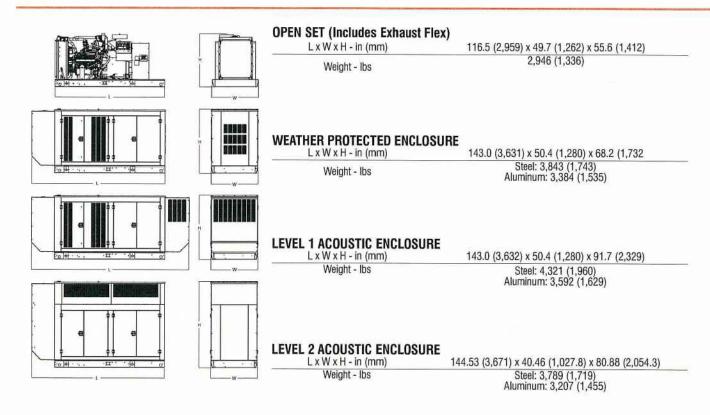
# SG150 | 9.0 L | 150 kW

#### INDUSTRIAL SPARK-IGNITED GENERATOR SET

EPA Certified Stationary Emergency



#### **DIMENSIONS AND WEIGHTS\***



\*All measurements are approximate and for estimation purposes only.

YOUR FACTORY RECOGNIZED GENERAC INDUSTRIAL DEALER					

Specification characteristics may change without notice. Dimensions and weights are for preliminary purposes only. Please consult a Generac Power Systems Industrial Dealer for detailed installation drawings.

Determining the precise per-hour emissions of carbon monoxide (CO), nitrogen oxides (NOx), and particulate matter (PM) from a 150 kW natural gas generator at full load without catalytic control is complex, and can vary based on several factors, including:

- Engine Design and Technology: Different engine manufacturers and models will have varying combustion efficiencies and emissions characteristics.
- Operating Conditions: Parameters like air-fuel ratio and engine load influence emissions output.
- Maintenance: Well-maintained engines generally produce lower emissions.
- Fuel Quality: Variations in natural gas composition can impact combustion and emissions.

Despite these variables, available data and emissions factors offer some insights. For example:

- A Cummins C150 N6 natural gas generator, rated at 150 kW, has the following emissions when operating at full load without catalytic control:
  - CO: 412 ppmvd (parts per million by volume, dry basis) or 1.74 grams per HP-hour.
  - NOx: 360 ppmvd or 1.77 grams per HP-hour.
- Other studies have found that CO emissions factors tend to decrease with increasing engine load, while NOx emissions factors increase up to mid-loads and decrease slightly at high loads.
- Natural gas combustion generally produces low filterable particulate matter (PM)
  emissions because it is a gaseous fuel. Studies estimate these particles are
  typically less than 1 micrometer in size and have filterable and condensable
  fractions. PM emissions factors are also influenced by engine load and age, with
  newer engines tending to have lower PM emissions.

Below is an order-of-magnitude estimate of uncontrolled CO, NO<sub>x</sub>, VOC and particulate (PM<sub>10</sub>/PM<sub>2·5</sub>) emissions for a small industrial heater firing propane at 0.2 MMBtu/hr. All factors are taken from EPA AP-42, Section 1.4 (Gas- and Oil-Fired Boilers and Heaters) for a conventional (non-low-NO<sub>x</sub>) burner.

Step 1 – AP-42 Uncontrolled Emission Factors (lb pollutant per MMBtu fuel input)

- CO: 0.10 0.23 (typical 0.16)
- $NO_x$ : 0.03 0.11 (typical 0.04)
- VOC: 0.004 0.010 (typical 0.006)
- PM<sub>10</sub>: 0.004 0.010 (typical 0.007)

 $(PM_{2.5} \approx PM_{10} \text{ for propane combustion})$ 

Step 2 – Multiply by 0.2 MMBtu/hr

Pollutant	EF Range (lb/MMBtu)	Emission Rate Range (lb/hr)	Typical EF (lb/MMBtu)	Typical Rate (lb/hr)
СО	0.10 – 0.23	0.02 – 0.046	0.16	0.032
NO <sub>x</sub> (as NO <sub>2</sub> )	0.03 – 0.11	0.006 - 0.022	0.04	0.008
VOC	0.004 – 0.010	0.0008 – 0.0020	0.006	0.0012
$PM_{10}$	0.004 – 0.010	0.0008 – 0.0020	0.007	0.0014

- These factors assume a standard (uncontrolled) propane burner. If you have a low-NO<sub>x</sub> burner, the NO<sub>x</sub> EF may drop into the 0.01–0.05 lb/MMBtu range (≈ 0.002–0.010 lb/hr at 0.2 MMBtu/hr).
- 2.  $PM_{2.5}$  emissions from propane combustion are essentially the same as  $PM_{10}$ .

#### Attachment O

# Monitoring, Recordkeeping, Reporting and Testing Plans

## Pyrolysis Unit 1 and 2 - Natural Gas or Pyrolysis Gas Fired Low NOx Burners

The West Virginia Department of Environmental Protection (WVDEP) has a comprehensive set of regulations for air pollution sources, including plants operating with natural gas fired burners.

Applicable Regulations: Federal and State regulations like Title V, NSPS, NESHAP, and specific WVDEP rules such as 45CSR13 for minor sources, 45CSR30 for major sources, and 45CSR10 for sulfur oxides.

#### 1. Emissions Monitoring

Stack Testing/Performance Tests: On initial startup and annually, emissions testing will be completed to demonstrate compliance with emission limits for CO, NOx, and VOC.

Fuel Analysis: Operations will monitor pyrolysis gas for H2S, Cl, and CO content daily using gas detection tubes or other methods. Operations will log these readings in operating logs and note trends. Annually the data will be summarized and included in the report to site management.

## 3. Recordkeeping

Emissions Records: Clean Seas will maintain records of testing daily and annual testing data, including emissions data, stack test results, and calculations based on emission factors.

Operating Parameters: Records of daily operational parameters and trends, such as fuel usage, operating hours, and equipment settings will be maintained.

Maintenance Records: Records of maintenance and repairs performed on the burners and associated control equipment will be kept.

Compliance Records: Documentation of plant performance with respect to permitted limits and applicable regulations will be maintained at the plant site offices.

## 4. Reporting

Annual Emissions Inventory: A record of the annual emissions inventory will be reported to the WVDEP, detailing the monitoring of regulated pollutants emitted by the facility. This will

include Malfunction and Upset Reports that resulted in emissions exceeding permit limits. Compliance Reports: Clean Seas will submit periodic compliance reports as specified in the permit discussing how the facility performed with respect to permitted limits.

#### Flare 40 CFR 63.108

#### 1. Monitoring

Pilot Flame Monitoring: Operations will continuously monitor of the presence of the pilot flame(s) using a device like a thermocouple or infrared sensor which records data to the operations control system.

Visible Emissions: Clean Seas Operations will continuously monitor the flare for visible emissions exceeding 5 minutes in any two-hour period when material is routed to the flare. Operators in the control room will also monitor the flare with a camera.

#### 2. Recordkeeping

Records documenting pilot flame status, visible emissions observations, flow rates and operating parameters, flare vent gas upset sources, and periods when operating values are outside limits or when monitoring was not performed correctly will be maintained in operating logs.

#### 3. Reporting

An annual or more frequent if required Monitoring Report will be filed reporting excursions, missing readings, exceedances. Confirmed releases will be reported within 24 hours to the relevant agencies.

#### Tanks

The portable storage tanks (Baker Style) will be monitored by Clean Seas daily for leaks, overfilling and other upsets by the operators. The daily monitoring will include visual inspections, inventory control or other activities. Monitoring will inform the recordkeeping and reporting for the site's conformance with permitted activities.

The pyrolysis plants are designed to produce low vapor pressure pyrolysis oil. Clean Seas will use nitrogen blanketing and vent tanks to the flare for safe combustion of any vapors. Operations controls will continuously monitor purging of the tanks with nitrogen and record vapor flows to the flare.

## Recordkeeping

The facility will keep records of operation, maintenance, corrosion prevention, inspections (routine and periodic) and initial tightness testing. The site will maintain records of releases, containment, and follow-up actions.

#### Reporting

Release Reporting: Clean Seas will report releases above threshold quantities to the WVDEP appropriate authorities. Confirmed releases will be reported within guidelines to WVDEP authorities. Clean Seas will maintain Spill Prevention and Response Plans.

Certified Inspections: Required for ASTs.

Corrective Action: For confirmed releases, Clean Seas will follow AST rules, including immediate containment and hazard mitigation.

#### **Truck Loading Rack**

Requirements are primarily governed by West Virginia Legislative Rule 45CSR21, which addresses the control of VOC emissions.

#### 1. Emissions control and testing

The Clean Seas truck loading will be designed to contain vapors preventing any leakage to atmosphere. The loading design will control VOC emissions through the application of reasonably available control technology (RACT). Testing of the loading system will be completed before each truck loading to verify that the hoses, piping and equipment are properly aligned and in working condition. Initial and period testing will be used to demonstrate compliance with these emission limits.

## 2. Monitoring

Before loading or unloading each truck, operations and truck drivers will check for system integrity upon initial connection and at completion of the product loading. Control devices including VOC control devices (e.g., pressure, temperature, or flow rate) will be in place to maintain system integrity. Collection pans, curbing and other equipment will be used to catch any material when hoses or piping are disassembled.

#### 3. Recordkeeping

Maintain records of all testing and calculations performed to demonstrate compliance.

Clean Seas will keep records of maintenance and inspection activities related to the loading rack and control equipment. The facility will log operational data, including any deviations from normal operating conditions or malfunction events.

#### 4. Reporting

Clean Seas will maintain records of shipments, incidents, oil quality/properties and inventories. Deviations from permit requirements or malfunctions resulting in excess emissions will be logged and reported to the WVDEP, as specified in the facility's permit.

An emission Inventory will be prepared and submitted annually, detailing the amount of air pollutants emitted from the loading rack and other sources at the plant.

#### **Emergency Power Generator** 45CSR13

The site will install an emergency backup generator to enable safe shutdown of the plant for loss of electrical power supply to the facility. Emissions from this generator will be limited by using natural gas as a fuel and a catalytic converter on the exhaust.

#### Monitoring

The site will record the annual hours of operation including non-emergency usage such as maintenance checks and testing. The site will test run the generator once per week for approximately and hour.

Natural Gas Fuel Usage: Record the quantity of natural gas consumed by the generator.

Emission Limits: The manufacturer has performed testing on the generator and has reported the emissions of nitrogen oxides (NOx), carbon monoxide (CO), CO2, PE, sulfur dioxide (SO2), and volatile organic compounds (VOCs) based on natural gas fuel.

## Recordkeeping

Operating Logs: Clean Seas will maintain records of the dates, times, and duration of all emergency and non-emergency operations.

Fuel Purchase Records: The site will keep records of natural gas purchases to document fuel consumption.

Maintenance Records: Document all maintenance and repairs performed on the generator.

Manufacturer Specifications: Keep records of the generator's manufacturer's specifications and compliance demonstrations

## Reporting

Annual Emission Reports: Submit reports detailing the generator's emissions of regulated air pollutants, often using the DEP's emissions inventory system or required forms.

Compliance Certifications and Deviation Reports: Submit periodic certifications of compliance with the permit conditions. Report any deviations from permit conditions or regulations, such as exceeding operational hour limits or emission limits.

# Attachment P Public Notice

Class 1 Legal Advertisement
45 CSR 13.8.3 and 45 CSR 13.8.5

Example of Legal Advertisement for Details
Affidavit of Publication on Attachment P

# Clean-Seas West Virginia, Inc.

# W.V. Plant - Legal

#### Plant Location:

2700 E Dupont Ave

Belle WV 25015

#### Reference Coordinates:

• UTM – Easting – 440427.769

• UTM – Nothing – 1822380.411

• UTM Zone – 17n

• Longitude: 32.2081876

• Latitude: -81.5081475

Total Building Area: 62,100 sq ft

Plant from seal level EL 627.699 – 628.177 feet above sea level

Plant floor  $EL - 628 \pm .5$  ft

Applicant: Clean-Seas West Virginia, Inc.

Type of Permit: Minor Source – "Construction Permit"

Operations: Plastics Pyrolysis Plant

Startup Date: October 15, 2025

Type of Pollutant: Criteria Pollutant – Each Criteria Pollutant allowance by EPA and WV DAQ is 100 tons per year – See Emissions Table 9.4

A) Criteria Pollutant	Tons Per Year (Rounded)	
a. Particulate Matter	1	
b. CO2 – Carbon Dioxide	3500	
c. HCL	<.01	
d. SO2 – Sulfur Dioxide	.02	
e. NOX - Nitrogen Oxide	2	
f. HAPS (Total)	6	

#### B) Source and Contact – For more Information

Name: John Yonce, Clean-Seas

Address: 2700 E Dupont Ave, Ste 3B, Belle WV 25015

Tel: 304-220-2041

#### C) Written Comments:

- 1. All questions regarding this permit application should be directed to the DAQ at telephone number (304)-926-0499 Ext 1250.
- 2. Written comments should be sent to:

The West Virginia Department of Environmental Protection

Division of Air Quality (DAQ)

601 57th Street SE

Charleston, WV 25304

From 30 days from the date of publication of this notice.